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CONCEPT FOR ATTENUATION OF THE BACK
BLAST REGION OF A 105 mm RECOILLESS RIFLE

Hugo J. Nielsen

IIT Research Institute

Prepared for:

Watervliet Arsenal

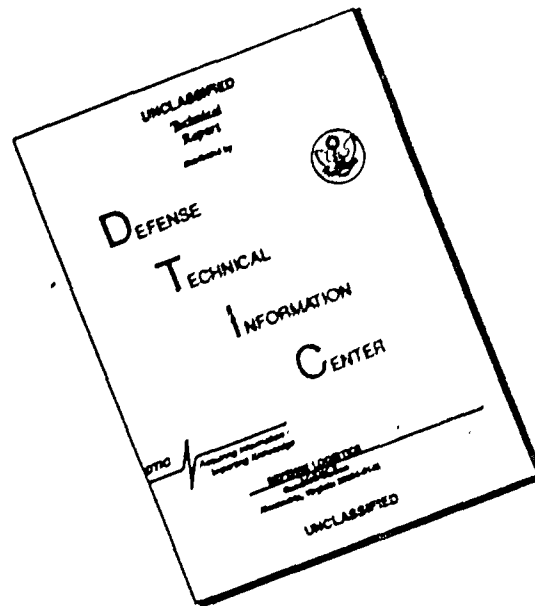
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REPORT DOCUMENTATION PAGE		READ INSTRUCTIONS BEFORE COMPLETING FORM
1. REPORT NUMBER WVT-CR-74026	2. GOVT ACCESSION NO.	3. RECIPIENT'S CATALOG NUMBER AD-786616
4. TITLE (and Subtitle) Concept for Attenuation of the Back Blast Region of a 105 mm Recoilless Rifle		5. TYPE OF REPORT & PERIOD COVERED
7. AUTHOR(s) Hugo J. Nielsen		6. PERFORMING ORG. REPORT NUMBER J6293 (Sep 1973)
9. PERFORMING ORGANIZATION NAME AND ADDRESS IIT Research Institute 10 West 35th St. Chicago, Illinois 60616		8. CONTRACT OR GRANT NUMBER(s) Contract No. DAAFO7-73-C-0155
11. CONTROLLING OFFICE NAME AND ADDRESS Benet Weapons Laboratory Watervliet Arsenal Watervliet, N.Y. 12189		10. PROGRAM ELEMENT, PROJECT, TASK AREA & WORK UNIT NUMBERS AMCMS No. 513F.12.05014.02 DA Project No. 1F163206D050 Proj No. RJ-2-50139-(01)-M7-M7
14. MONITORING AGENCY NAME & ADDRESS (if different from Controlling Office)		12. REPORT DATE July 1974
		13. NUMBER OF PAGES
		15. SECURITY CLASS. (of this report) UNCLASSIFIED
16. DISTRIBUTION STATEMENT (of this Report) Approved for release; distribution unlimited.		
17. DISTRIBUTION STATEMENT (of the abstract entered in Block 20, if different from Report)		
18. SUPPLEMENTARY NOTES		
19. KEY WORDS (Continue on reverse side if necessary and identify by block number) Recoilless Rifles Interior Ballistics Air Blast Fluid Dynamics Blast Attenuation Breech Blast Two-Phase Flow Davis Gun Represented by NATIONAL TECHNICAL INFORMATION SERVICE U.S. Department of Commerce Springfield, VA 22161		
20. ABSTRACT (Continue on reverse side if necessary and identify by block number) A concept for attenuating the back blast field of a recoilless rifle by the ejection of liquid or solid particles was investigated with respect to feasi- bility. The concept involves attaching a cylinder partially filled with liquid or solid particles to the nozzle. In this way the propellant gas is forced to expend some of its energy in driving the particles out of the cylinder and the duration of the flow of propellant gas into the blast field is altered. SEE REVERSE SIDE		

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ABSTRACT (Continued)

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The feasibility of the concept was investigated computationally. Computer programs were prepared to solve the gas dynamics of the blast field which included traveling particles. Computational procedures were used that are analogous to current single phase gas dynamics methods, but which are also based on the conservation relations for mass, momentum and energy in multiphase systems. The velocity and temperature of the gas and particles are allowed to be different in this computational procedure.

The results of the investigation, are that attenuation of the blast field is possible if the attached cylinder is long and the total weight of the expelled particles approaches the weight of the projectile. For shorter cylinders and smaller weights of particles, the blast field is not attenuated. Thus, the blast attenuation concept studied is feasible only in a rifle which is encumbered with an attachment which is so heavy the rifle is no longer a practical weapon.

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REGION OF A 105 MM RECOILLESS RIFLE

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WATERVLIET, N.Y. 12189**

JULY 1974

TECHNICAL REPORT

AMCMS No. 513F.12.0:014.02

DA Project No. 1F163206D050

Pron No. EJ-2-50139-(01)-M7-M7

Contract No. DAAF07-73-C-0155

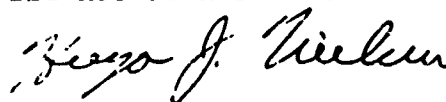
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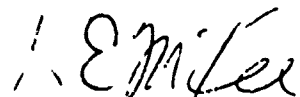
This is the final report on Contract DAAF07-73-C-0155 for Watervliet Arsenal, IIT Research Institute Project J6293. Charles C. Andrade was project monitor. A significant contribution to the effort described in this report was made by Arnold Wiedermann in the area of mechanisms that would influence the blast field and assistance in the programing effort.

Respectfully submitted,
IIT Research Institute



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1. INTRODUCTION

The army is currently investigating methods for arming helicopters with weapons of greater firepower. A major difficulty stems from the relatively weak helicopter structure which cannot sustain the recoil of most large caliber weapons. Although recoilless rifles obviate one problem, the blast field created by propellant gases discharged through the rifle nozzle creates other problems. Damaging peak overpressures of several pounds per square inch would be produced on some parts of the helicopter fuselage.

Constraints which arise from considerations of loading, firing, etc., prevent mounting the rifle so that the blast field does not affect the helicopter's structure. Moreover, severe weight penalties are involved in shielding the fuselage or employing ducts to carry away the nozzle blast gases. The net effect of these constraints is to make the feasibility of arming helicopters with recoilless rifles depend on finding a means for attenuating the intensity of the blast field.

A particular concept for attenuating the blast field was investigated. The concept involves attaching a short cylinder filled with water or solid particles to the rifle nozzle to delay the emergence of propellant gas. The flowing propellant gas would be slowed by driving the particles* out of the cylinder, thereby reducing the blast pressure, if the expelled liquid or solid does not give up its acquired momentum to the atmosphere too rapidly after it emerges from the cylinder.

The approach taken in this investigation is to develop a computational method and program for describing the blast field produced by the particles expelled from the cylinder. This is accomplished by extending the numerical methods presently used for solving unsteady compressible single component flows to a multiphase flow where the velocity and temperature of the particles can be different from that of the gas in which they are suspended.

*The word "particles" as used herein refers to solid or liquid particles.

2. BLAST ATTENUATION

a. Basic Mechanism

The blast field behind a recoilless rifle depends mainly upon two factors, the total energy of the propellant gas flowing through the nozzle and the duration of the flow. Since the comparative importance of these factors varies with the distance from the nozzle, it is desirable to have an assessment of the distances in which one or the other has a predominant influence.

The distribution of pressure, density, energy or velocity in the blast field can be regarded as a system of traveling waves in which the local wave speed is the speed of sound. As the propellant gas flows into the blast field and raises the temperature by the effect of compression or by the convection of gases of higher temperature, the wave speed increases. A consequence of this is that a profile of pressure versus time that formerly rose gradually to the peak pressure in the vicinity of the nozzle, changes so that it rises more rapidly at greater distances. As one considers increasing distances from the nozzle the pressure profile eventually steepens to form a shock wave. The process takes place as illustrated in Figs. 1a and 1b. For distances large enough for the profile to steepen up to a shock wave the pressure is independent of the duration of the nozzle flow and only depends on the total energy of the gas and the distance from the nozzle. If the shock pressure were still strong compared to the ambient pressure at these distances it would approach the Taylor's result for a point source explosion (Ref. 1),

$$p \propto E_t / R^3 \quad (1)$$

-
1. Taylor, G., "The Formation of a Blast Wave by a Very Intense Explosion," Vol. 201.

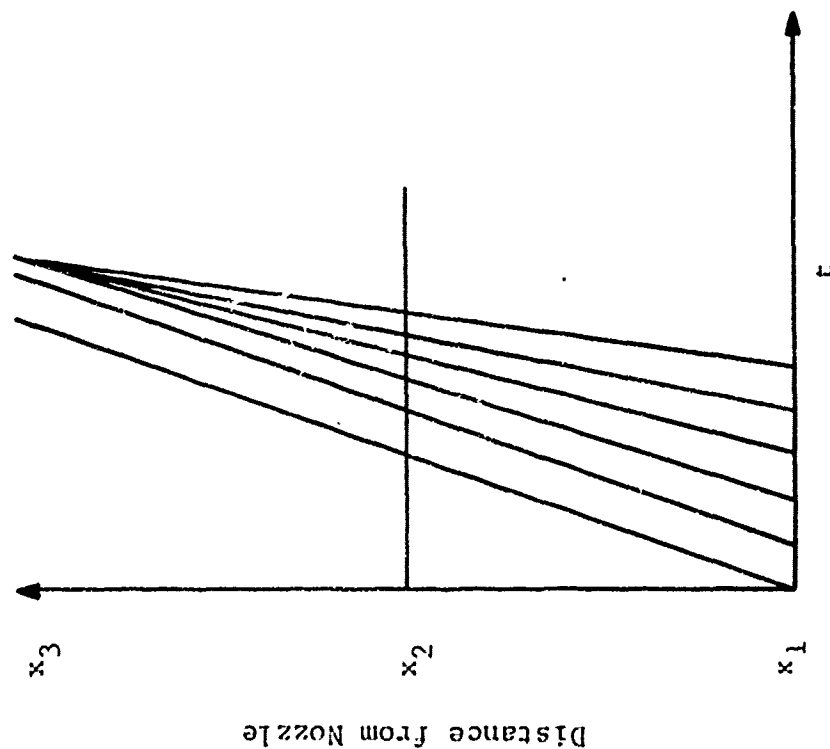


Figure 1a. DISTANCE OF WAVE PROPAGATION

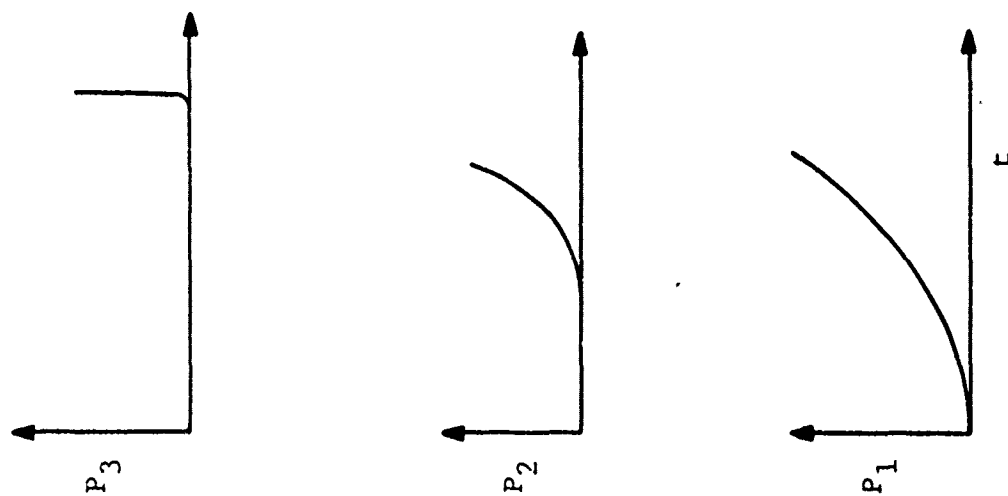


Figure 1b. PRESSURE PROFILE AT VARIOUS DISTANCES FROM NOZZLE

where

E_t = total energy released by explosion
or in propellant gases

p = pressure

R = realistic distance from source

Although Taylor's result may not be useful for a quantitative estimate of the blast pressure in the problem of concern, the indicated linear dependence of the pressure on the total gas energy is probably a good guide.

These preliminary considerations of the propagation of the blast wave show that for positions in the blast field beyond the distance where a shock wave forms, the only means for attenuating blast intensity is to reduce the total energy in the propellant gas. At lesser distances, nozzle flow duration is a factor and prolonging it would result in reduced peak pressure. An approximation of the distance required for the formation of the shock wave can be made as follows. The temperature of the propellant gas increases the speed of sound two to three times over that which exists in ambient air. The peak chamber pressure is reached about 6 msec after ignition. Equating the travel distances for waves emitted at the initial and peak pressure conditions and assuming that the waves at the peak condition travel at a speed three times greater than the others, yields a distance of 10 ft.

The area of interest on the helicopter extends from about 3 to 10 ft from the fuselage. For much of this area it is apparent that both of the factors discussed will influence the blast pressure, but at the extremity the peak pressure is determined by the total energy in the propellant gases.

b. Approaches for Implementing the Blast Attenuating Mechanism

Two recoilless rifle configurations were considered in which particles are expelled. Each epitomizes a different blast attenuation mechanism: (1) reduction of total energy, and (2) prolongation of flow duration.

(1) Davis Gas

A rifle based on this principle would consist of a straight tube in which particles are expelled from one end and the projectile from the other. Since the momentum of the particles must equal that of the projectile to fulfill the requirements for cancellation of recoil, the tube length required is large unless the weight of the particles is much larger than that of the projectile. For particles of weight equal to the projectile, the tube length would be twice that of a conventional rifle and, therefore, impractical. The blast pressure is reduced because the gas does not escape from the rifle freely until the particles are expelled from the tube. An estimate of the energy removed from the propellant gas by accelerating the projectile and particles may be obtained by assuming that the expansion is isentropic,

$$\frac{e_2}{e_1} = (\text{volume ratio})^{\gamma-1} = 0.66 \quad (2)$$

where

- e_1 = initial internal energy
- e_2 = internal energy when propellant gas emerges
- γ = ratio of specific heat, 1.21 for propellant
gas volume ratio = 1/7, chamber-to-chamber
plus barrel volume

About one-third of the energy in the propellant gas is removed and the approximate effect on the blast field is proportional to the value given for the ratio of the emergent to the initial internal energy.

This concept provides a means for reducing the blast intensity and shows that it is feasible to attenuate the blast pressure by expelling particles. The question remaining is, do the expelled particles release their acquired momentum to the air after exiting? If the particles remain as a coherent mass, they would not; if they expand rapidly, the drag forces acting on the particles would cause

them to transmit their momentum to the air again and produce a blast field. This problem is dealt with by means of the two-dimensional blast field code discussed in the following section. A listing of one- and two-dimensional codes is provided in Appendices A and B.

(2) Short Cylinder Concept

This concept was developed in an attempt to achieve blast attenuation without the excessive length of the Davis gun. The cylinder from which particles are expelled is shorter and a nozzle is used between the cylinder and rifle chamber to permit the chamber pressure to build up properly. With the shorter cylinder, the amount of energy that can be removed from the propellant gas is less than with the Davis Gas concept. To have a significant reduction in the intensity of the blast field, the effect of flow duration has to be exploited. In this study, the particles are not compacted and the propellant gas is permitted to leak through void spaces, thus prolonging the flow period. Since the particles are not attached to the cylinder and do not transmit an axial load to it, the recoilless properties of the rifle are not affected significantly by the cylinder.

3. MATHEMATICAL MODELING

The physical problem to be modeled involves the motion of liquid droplets or solid particles through a gas in which strong compressible effects take place that include the formation of shock waves. Because the temperature and velocity of the particles are not usually the same as of the gas at the same location, various interactions take place between the gas and the suspended

particles. The effects of drag and heat transfer cause momentum and energy to be transferred between the gas and the particles. The motion and temperature of the gas therefore, are different than in an analogous flow case without particles.

A numerical method is developed for the solution of this problem that is patterned after the same techniques used for the numerical solution of single component flows. Conservation relations for the mass, momentum and energy are developed for the gas and particle phases and these relations are then expressed in finite difference form for solution by numerical methods. Approaches to the development of the conservation relations and some solution for particular flow cases are summarized by Soo (Ref. 2) and Marble (Ref. 3).

a. Conservation Relations

The conservation relations are developed for an elemental cell as indicated in Fig. 2. Particle sizes and mean separation distances are assumed to be small relative to the size of the cell. This limits the applicability of the method to problems in which the mean particle separation distance is small relative to the system size and the scale of the phenomena of interest.

(1) Mass Conservation

Equating the accumulation of gas or particles to the net flux of gas or particles into the cell and the contributions due to evaporation and other effects, gives the following expressions for the gaseous and particle phases:

-
2. Soo, S. L., Fluid Dynamics of Multiphase System, Blaudell Publishing Co., (1967).
 3. Marble, F. E., "Dynamics of Dusty Gases," Annual Rev. Fluid Mech., Vol. 2, (1970).

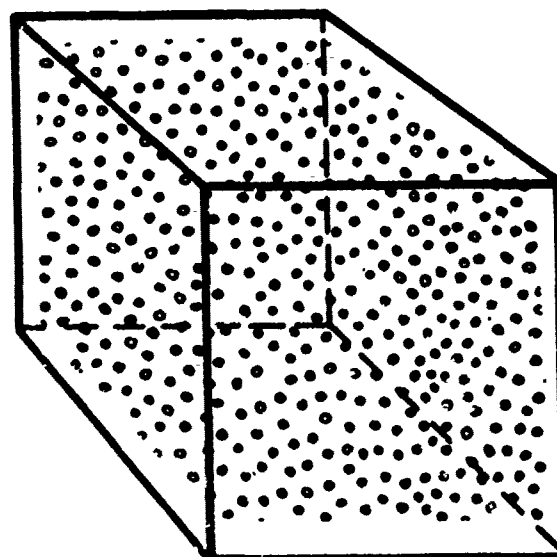


Figure 2 ELEMENTAL CELL.

$$\frac{\partial c_g}{\partial t} = - \nabla \cdot \vec{u}_g c_g + N W_e + W_{pb} \quad (3)$$

$$\frac{\partial c_d}{\partial t} = - \nabla \cdot \vec{u}_d c_d - N W_e \quad (4)$$

$$\frac{\partial N}{\partial t} = - \nabla \cdot \vec{u}_d N \quad (5)$$

where

c_g = concentration of gas

c_d = concentration of matter present as particles

N = number of particles per unit volume

t = time

\vec{u}_d = velocity of particles

\vec{u}_g = velocity of gas

W_e = mass loss of a single particle by vaporization

W_{pb} = mass addition by propellant burning

(2) Momentum Conservation

When one considers the motion of a single particle the governing equation is obtained by equating the Lagrangian acceleration to the drag force and the pressure difference across the particle.

$$m \frac{D\vec{u}_d}{Dt} = - \vec{D} - V \nabla p \quad (6)$$

where

\vec{D} = drag force vector

m = mass of the particle

p = pressure

V = volume of the particle

For the purpose of the computational method to be developed, a Eulerian expression (i.e., at a fixed point for the derivative), is required and can be obtained if the number of particles within the cell indicated in Fig. 2 is large enough so that the mean velocity is reasonably well defined and can be assumed to be continuous.

$$m \frac{\partial \vec{u}_d}{\partial \tau} = -m \vec{u}_d \cdot \nabla \vec{u}_d - \vec{D} - V \nabla p \quad (7)$$

Multiplying through by the number of particles and using Eq. (4) gives the following for the momentum of the particle phase.

$$\frac{\partial c_d \vec{u}_d}{\partial \tau} = -\nabla \cdot c_d \vec{u}_d; \vec{u}_d - ND - \frac{c_d}{\rho_d} \nabla p \quad (8)$$

where ρ_d is the density of the material of which the particles are composed.

Although the dyadic notation used ($\nabla \cdot c u; u$) is inconvenient, it permits the development of a conservative computational scheme, i.e., one in which the accumulation of momentum in the computational grid is exactly consistent with the fluxes of momentum over the grid boundaries. The alternative and more common expression for acceleration ($\vec{u} \cdot \nabla \vec{u}$), does not permit this.

The momentum equation for the gas phase may be obtained by subtracting the equation for the particle momentum derived here from the equations for total momentum of both the gas and the particles. However, the experience obtained with various different computation procedures with this problem, showed that a more stable program is obtained if the computational procedure is based on the equations for the total momentum of both the gas and particles and the momentum of the particles alone rather than on the equations for the momentum of the gas and particle phases.

Equating the accumulation of the momentum to the fluxes across the cell boundaries and the effects of pressure, gives the following expression for the total momentum of both phases,

$$\frac{\partial}{\partial t} (c_g \vec{u}_g + c_d \vec{u}_d) = - \nabla \cdot (c_g \vec{u}_g; \vec{u}_g + c_d \vec{u}_d; \vec{u}_d) - \nabla p \quad (9)$$

Terms relating to particle drag do not appear in this equation since they control only the transfer of momentum between the gas and particle phases and thus do not add to or subtract from the momentum sum.

(3) Energy Conservation

Considering again a single particle, the following equation is obtained for the temperature by equating the rate of change of stored sensible heat to the losses by convection and evaporative cooling.

$$m c_{pd} \frac{DT_d}{Dt} = - (Q_c + Q_e) \quad (10)$$

where

c_{pd} = specific heat of the particle

Q_c = cooling rate of particle by convection

Q_e = cooling rate of particle by evaporation

An Eulerian representation for the rate of temperature change can be obtained when the number of particles within the cell is large enough to permit a reasonable definition of a mean particle temperature.

$$c_{pd} \frac{\partial c_d T_d}{\partial t} + \nabla \cdot c_d \vec{u}_d T_d = - N(Q_c + Q_e) \quad (11)$$

An expression for the total energy in both phases is obtained by equating the rate of accumulation of energy to the fluxes and the work done by pressure effects at the cell boundaries.

$$\begin{aligned}
& \frac{\partial}{\partial t} \left(c_g \left(e_g + \frac{1}{2} \vec{u}_g \cdot \vec{u}_g \right) + c_d \left(c_{pd} T_d + \frac{1}{2} \vec{u}_d \cdot \vec{u}_d \right) \right) \\
& = - \nabla \cdot \vec{u}_g \left(c_g \left(e_g + \frac{1}{2} \vec{u}_g \cdot \vec{u}_g \right) + VFp \right) \\
& \quad - \nabla \cdot \vec{u}_d \left(c_d (c T_d + \frac{1}{2} \vec{u}_d \cdot \vec{u}_d) + (1 - VF)p \right) \quad (12)
\end{aligned}$$

where

e_g = internal energy of the gas phase
 VF = void fraction

As in the case of the momentum equation, the computation scheme is more stable if the computations are based on the total energy and the energy in the particle stream. The gas phase energy is then obtained by calculating the difference in these quantities rather than by calculating the gas energy from an equation for the energy of the gas phase.

b. Subsidiary Relations

To obtain solutions for the above set of equations, it is necessary to connect the concentration, pressure and density with an equation of state, to evaluate the drag forces and particle heat transfer rates that transfer momentum and energy between the gas and particle phases. A propellant burning law is also required to predict the rate at which mass and energy is added to the propellant gases.

Equation of State

Tabulated values for the thermodynamic properties of the propellant gas from 23 different military propellants are given in Ref. 4. For computational purposes a polynomial representation was used to fit the equation of state data. The following nine term polynomial was fitted by least squares to the data for M8 propellant with a maximum discrepancy of only 0.3 of 1 percent:

4. Baer, P. G. and Bryson, K. R., Tables of Computed Thermodynamics Properties of Military Gun Propellants, BNL Memo. Rept. No. 1338 (Mar. 1961).

$$pR = \sum_{i=1}^3 \sum_{j=0}^2 A_{ij} \rho_g^i e_g^j \quad (13)$$

where

ρ_g = density

e_g = internal energy, including energy of formation as defined for e in Ref. 4

Numerical values for the coefficients A_{ij} are given in Appendix A in the subroutine entitled EQSTAT of the one-dimensional code.

The gas density to be used in this equation of state is determined from the amount of gas existing in a unit volume and the void fraction.

$$VF = 1 - \frac{c_d}{\rho d} \quad (14)$$

$$\rho_g = c_g / V \quad (15)$$

• Drag Forces

Drag forces acting on the drops are calculated from the drag coefficient and the dynamic pressure as follows:

$$D = C_d \frac{\pi}{4} a^2 \rho_g \frac{|\vec{u}_d - \vec{u}_g|}{2} (\vec{u}_d - \vec{u}_g) \quad (16)$$

where

a = particle diameter

C_d = drag coefficient

ρ_g = gas density

Absolute values of the velocity difference are used in the manner shown to preserve the proper sign and direction of the drag force irrespective of the sign of the velocity difference.

4. Baer, P. G. and Bryson, K. R., Tables of Computed Thermodynamics Properties of Military Gun Propellants, BRL Memo. Rept. No. 1338 (Mar. 1961).

Coefficients of drag C_d are obtained from the particle Reynolds number Re as shown, Ref. 5

$$C_d = \frac{24}{Re} \quad Re < 2.05 \quad (17)$$

$$C_d = \frac{18}{Re} 0.6 \quad 2.05 < Re < 486 \quad (18)$$

$$C_d = 0.44 \quad 486 < Re \quad (19)$$

where

$$Re = \frac{\rho_g a |\vec{u}_d - \vec{u}_g|}{\mu_g}$$

μ_g = gas viscosity

• Heat Exchange

The rate at which heat is transferred from the gas to the particulate phase is obtained from correlations for the heat transfer coefficient on a single particle (Ref. 6),

$$\frac{ha}{k_g} = 2 + 0.34 Re^{0.6} P_r^{1/3} \quad (20)$$

where

h = heat transfer coefficient

k_g = thermal conductivity of the gas

P_r = Prandtl number of the gas

The heat transfer rate, Q , is given by

$$Q = \pi a^2 h (T_g - T_d) \quad (21)$$

5. Perry, J. H., Chemical Engineering Handbook, McGraw-Hill Publishing Co. (1950).

6. McAdams, Heat Transmission, McGraw-Hill Publishing Co. (1954).

where

T_g = the gas temperature.

• Propellant Burning Law

The rate at which gas and energy is added to the propellant gas will be computed from surface regression rate of the burning propellant. Watervliet Arsenal provided the following correlation for the propellant to be considered.

$$R = 0.00186 p^{0.83} \quad (22)$$

where p is the pressure in pounds per square inch and R is the regression rate of the propellant surface in inches per second.

c. Computational Procedure

For the purpose of presenting the numerical method by which solutions to the preceding equation may be obtained, it is useful to use a more compact notation. Each of the differential Eqs. (3), (4), (5), (8), (9), (11) and (12) can be expressed in the following form.

$$\frac{\partial r \alpha_n}{\partial t} + \frac{\partial r(u \alpha_n + \epsilon_n)}{\partial r} + r \frac{\partial \gamma_n}{\partial r} + \frac{\partial r(w \alpha_n + \epsilon_n)}{\partial z} = r \xi_n \quad (23)$$

where r is the radial distance from the axis and z is the distance along the axis. Each of the variables α to ξ are defined in Table I. The velocity components, u and w , are of the phase considered.

The numerical procedure is based on a finite difference form for each of the equations represented by Eq. 23. Conceptually, the field of interest is divided into discrete cells and the finite difference equations describe the rate of accumulation of mass, number of particles, momentum, energy, etc. in terms of the fluxes of these quantities across the cell boundaries and the other quantities appearing in Eq. 23. In the particular grid system used in this study, velocity is defined at the cell boundaries

Table I DEFINITION OF TERMS IN EQUATION

Conservation of	α	β	γ	δ	ξ
Gas	c_g	0	0	0	$NW_e + W_{pg}$
Particle Mass	c_d	0	0	0	$-NW_e$
Number of Particles	N	0	0	0	0
Radial Momentum of Particles	$c_d u_d$	0	0	0	$-ND_r - \frac{c_d}{\rho_d} \frac{\partial p}{\partial r}$
Radial Momentum of Gas and Particles	$c_g u_g + c_d u_d$	0	0	0	0
Axial Momentum of Particles	$c_d w_d$	0	0	0	$-ND_z - \frac{c_d}{\rho_d} \frac{\partial p}{\partial z}$
Axial Momentum of Gas and Particles	$c_g w_g + c_d w_d$	0	0	0	0
Energy of Particles	$c_{pd} c_d T_d$	0	0	0	$-N(Q_c + Q_e)$
Energy of Gas and Particles	$c_g(e + \frac{1}{2} u_g \cdot u_g) + c_d(c_{pd} T_d + \frac{1}{2} u_d \cdot u_d)$	$VF \cdot p \cdot u_g$	0	$VF \cdot p \cdot w_g$	0
		$+(1-VF) \cdot p \cdot u_d$		$+(1-VF) \cdot p \cdot w_d$	

and particle number, concentration, pressure energy and temperature are defined at the cell centers as indicated in Fig. 3. The fluxes across the cell boundaries are computed in accordance with the donor cell concept described by Gentry and Martin (Ref. 7). That is, the flux of particles for example, is calculated from the particle density in the cell which donates the particles.

Because velocity, in the computational procedure used here, is defined at the cell boundaries, computations for the momentum of the gas and of the particles are based on special cells displaced one half the distance between the grid lines so that it is centered over the points where the velocity is defined. The momentum, pu , is thus based on the velocity at the special cell centers and an interpolated value for the density at that point. Similarly, the kinetic energy at the center of the cells where internal energy is defined is based on interpolated values for the kinetic energy.

Our experience with this computational procedure is that spurious negative values for the internal energy and pressure are obtained less frequently than with the more usual procedure in which the velocity is calculated for the same positions as the density and energy.

For the study of the blast field behind the weapon, the method would be implemented in a two-dimensional grid as shown in Fig. 4. The grid spacing increases with distance from the nozzle to accommodate a large region without an excessive number of grid points. Two computer programs were prepared for solving the blast field problem: (1) a one-dimensional program which describes the interior ballistics of the rifle and the flow from the cylinder; (2) a two-dimensional program which uses the flow from the cylinder as input and calculates the blast field.

-
7. Gentry, R. A.; Martin, R. E.; and Daly, B. J., "An Eulerian Differencing Method for Unsteady Compressible Flow Problems," Computational Phys., Vol. 1, pp 87-118 (1966).

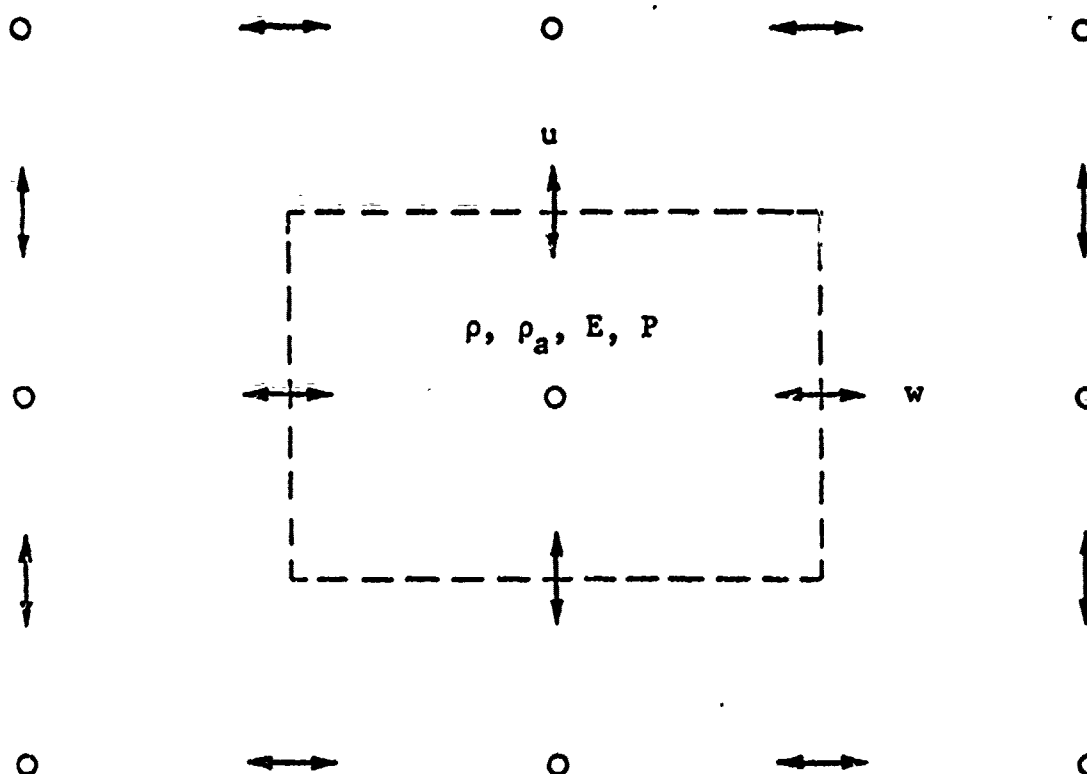


Figure 3 ELEMENT SPATIAL DISTRIBUTION WITH INTERLEAVING OF VELOCITY POINTS BETWEEN POINTS AT WHICH DENSITY, ENERGY, PRESSURE AND COMPOSITION ARE CALCULATED

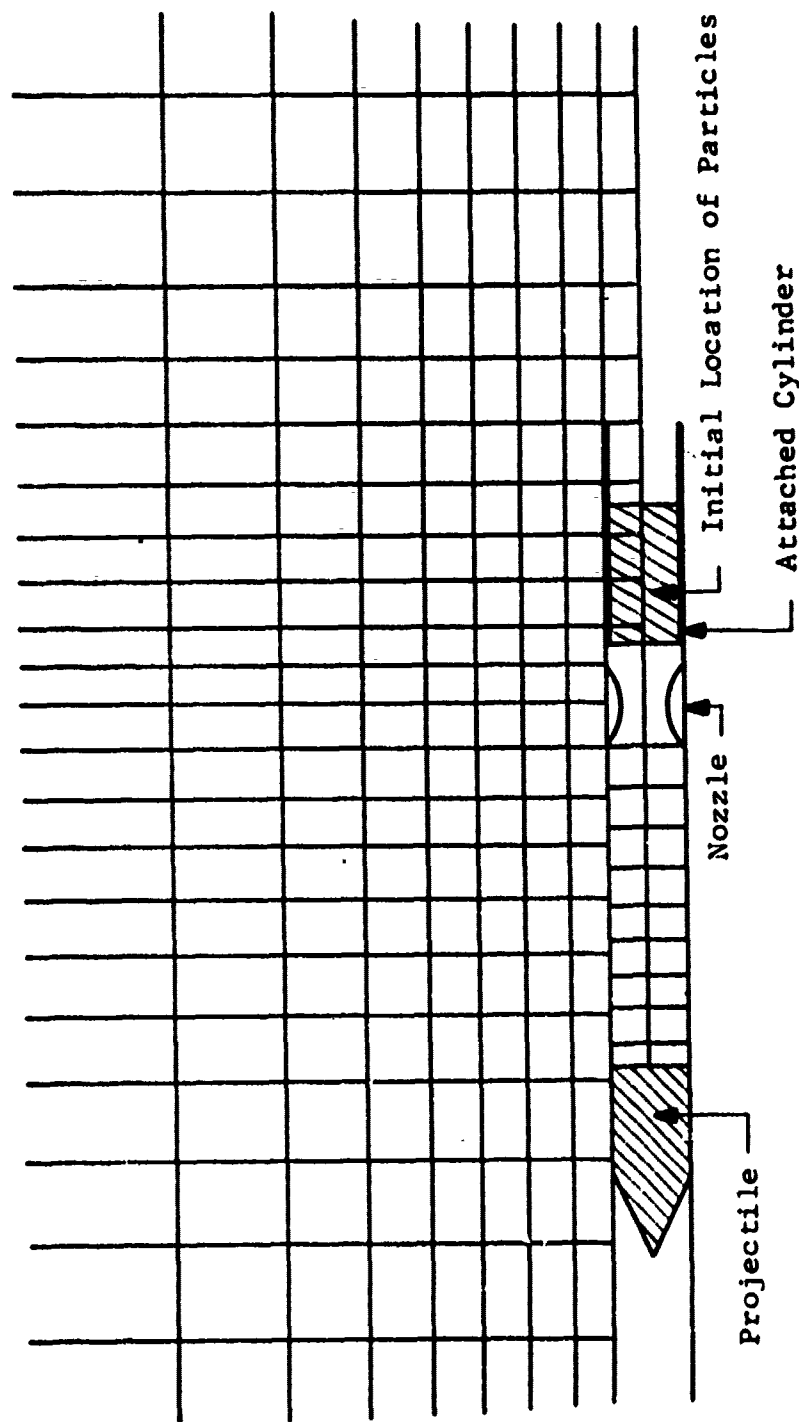


Figure 4 RECOILLESS RIFLE AND DISTRIBUTION OF NODES IN FINITE DIFFERENCE GRID

4. RESULTS

The interior ballistics and nozzle blast field were calculated for the conditions defined by the following values:

charge	8.1 lb
web	0.061 in.
bore	105 mm
barrel length	140 in.
chamber volume	200 in.
cylinder diameter	7.4 in.
cylinder length	24 in.
throat diameter (effective)	3.26 in.

Results for three different conditions in the attached cylinder are presented:

- no water in the cylinder
- 5 lb of water with a drop size of 5 mm
- 5 lb of water with a drop size of 1 mm

Results obtained with the one-dimensional model which furnished the inputs for the two-dimensional model are given in the following figures. Chamber pressures are given in Figs. 5-7.

These were obtained by calculating the average value of the pressures at nodes in the chamber region of the gun. A value of approximately 8000 lb was obtained for the peak chamber pressure in each case. The peak pressure is shown to increase slightly when water is used in the cylinder and when the drop size is diminished. This is due to the resistance to the flow or propellant gas developed by the water drops which diminish the leak rate of the rifle. The abrupt drop in chamber pressure that occurs at about 15 msec, coincides with the burnout of propellant. Values obtained for the projectile travel and velocity while in the barrel are shown in Figs. 8-10.

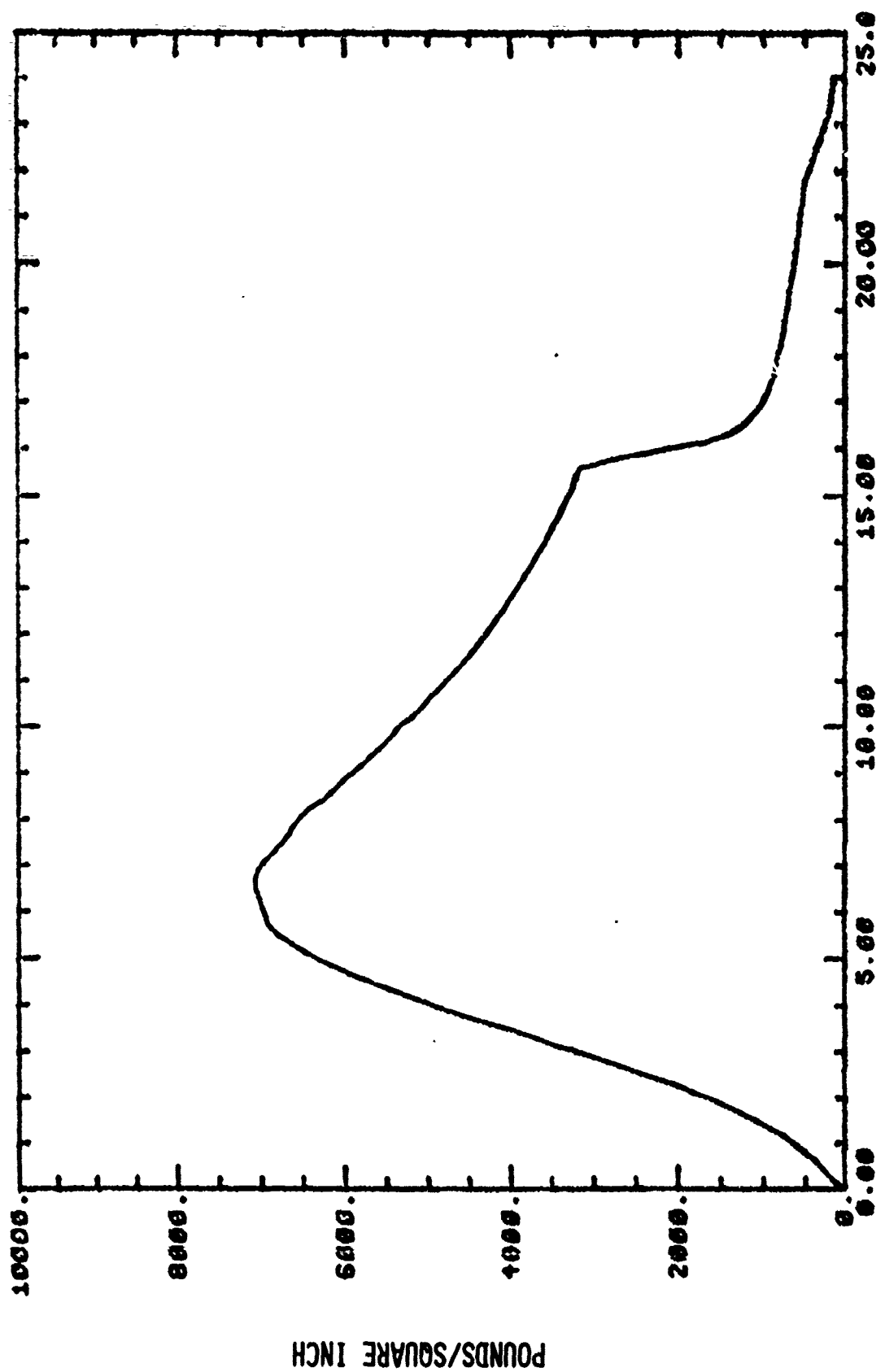


Figure 5 CHAMBER PRESSURE; NO WATER

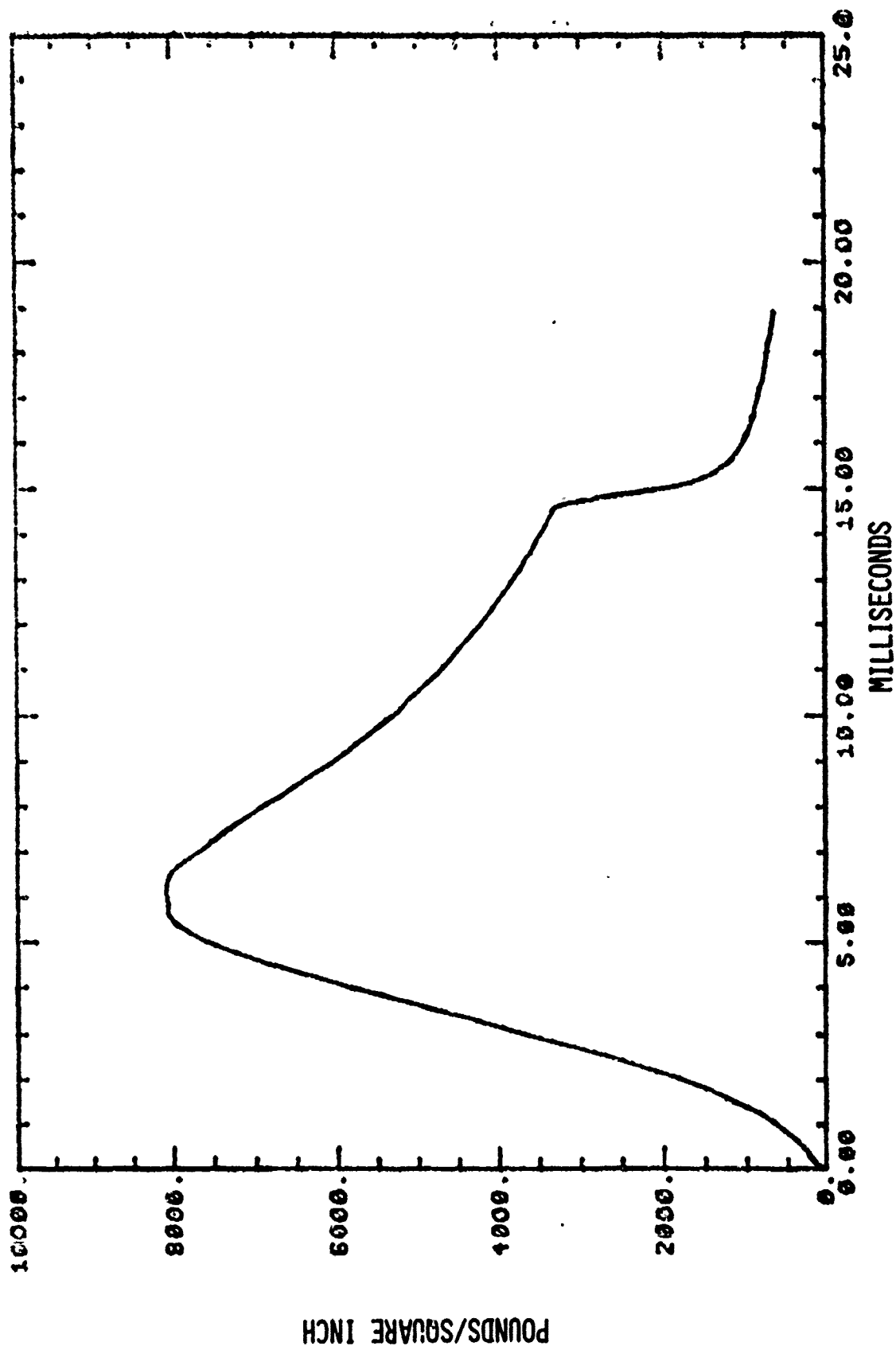


Figure 6 CHAMBER PRESSURE; 5 LB WATER, 5 MM DROP SIZE

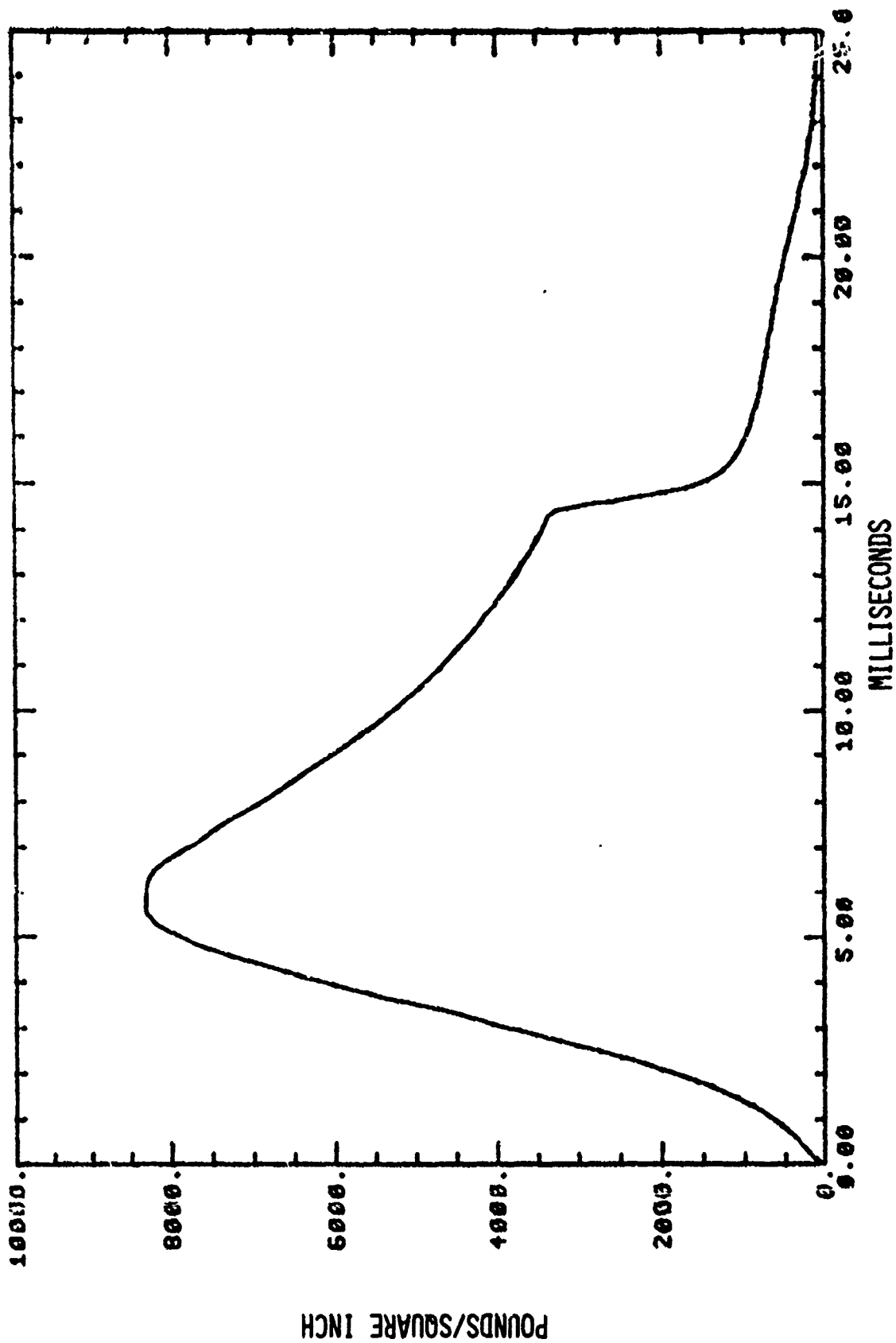


Figure 7 CHAMBER PRESSURE, 5 LB WATER, 1 MM DROP SIZE

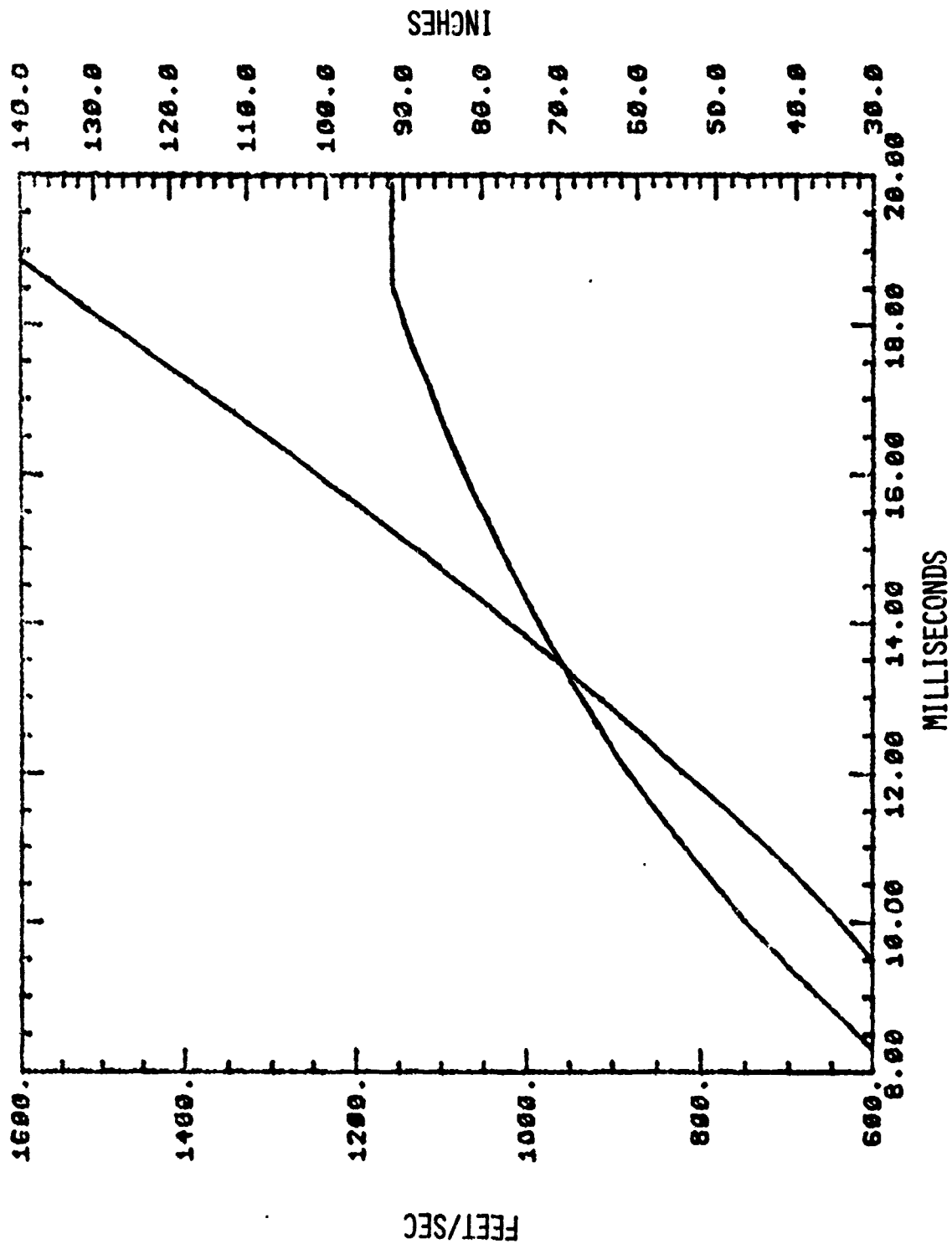


Figure 8 PROJECTILE VELOCITY AND TRAVEL DISTANCE, NO WATER

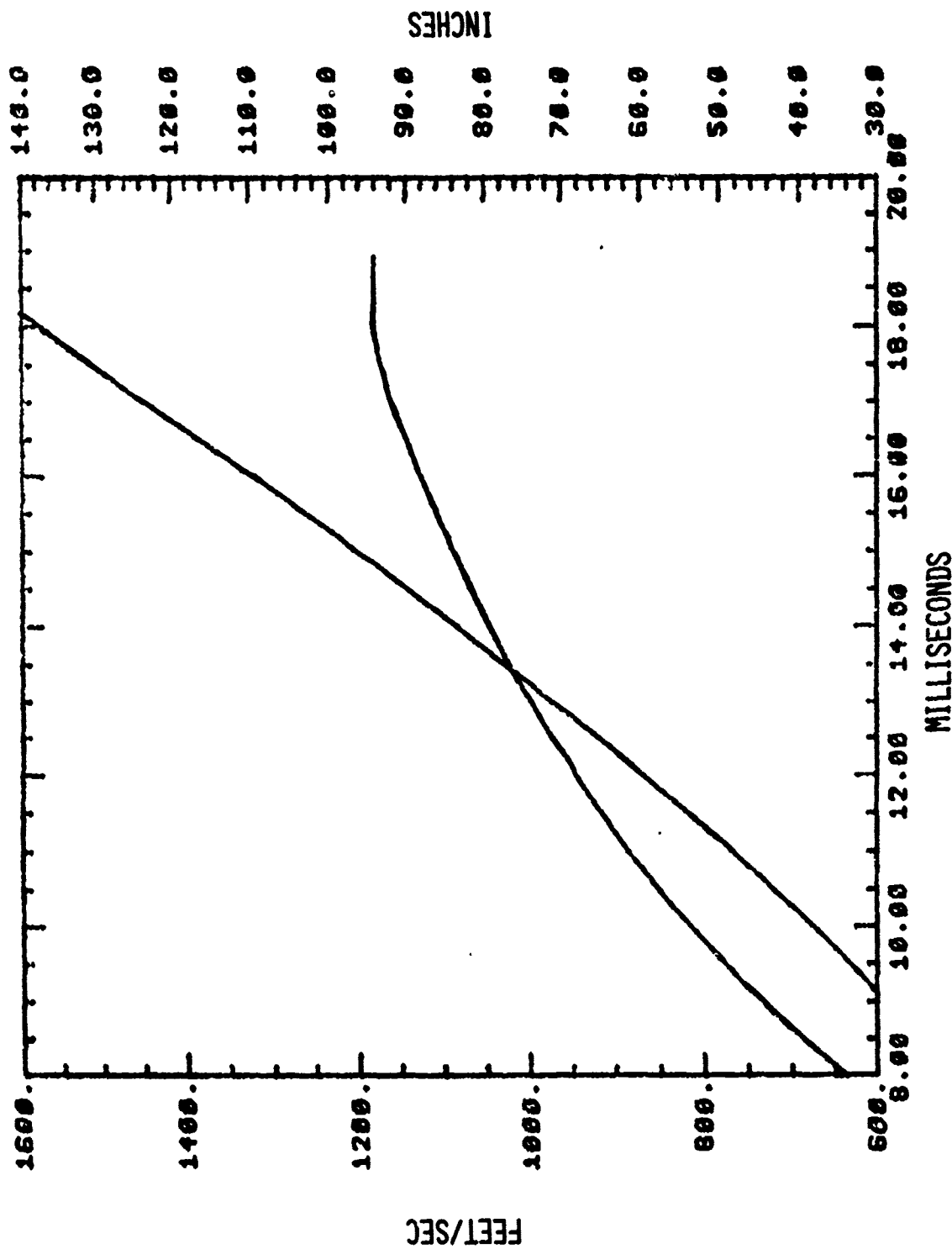


Figure 9 PROJECTILE VELOCITY AND TRAVEL DISTANCE, 5 LB WATER, 5 MM Drop Size

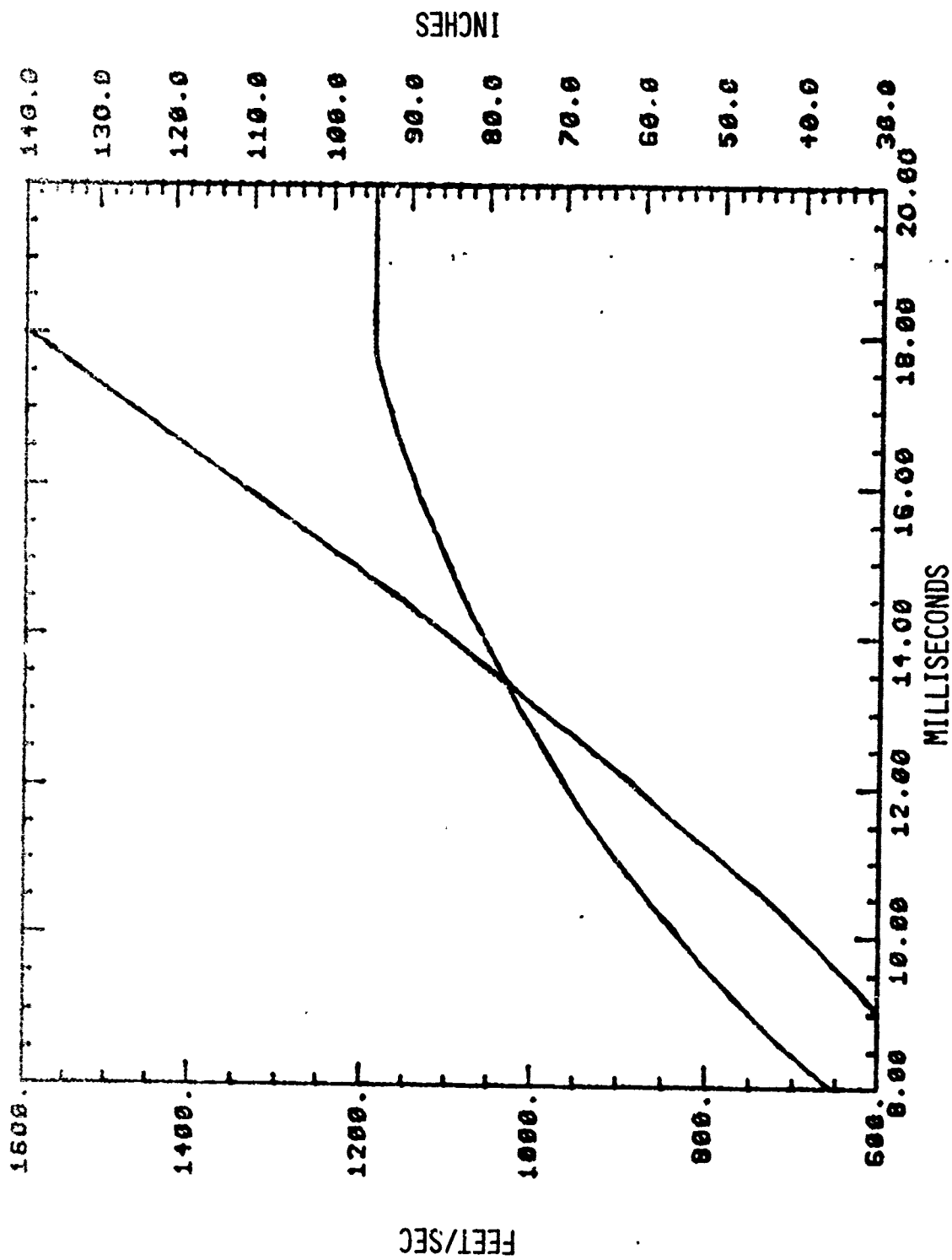


Figure 10 PROJECTILE VELOCITY AND TRAVEL DISTANCE, 5 LB WATER,
1 MM DROP SIZE

The output of the one-dimensional program was used as an input condition for the two-dimensional program. Early time examples of the spatial pressure distribution are shown in Figs. 11-12. The flow out of the attached cylinder is directed to the right and the cylinder exit is located on the horizontal axis in the center of the smallest contour. As one would expect, the pressure profile is elongated in the direction of flow. For the purpose of evaluating the effect on the blast pressure of water in the cylinder attached to the rifle, the pressure was listed for selected points for each case. The location of these points A-F is indicated in Fig. 13, and the pressure pulse profiles in Figs. 14-16. These pressure pulse profiles show that the peak pressure increases as water is added to the cylinder and the drop size is diminished.

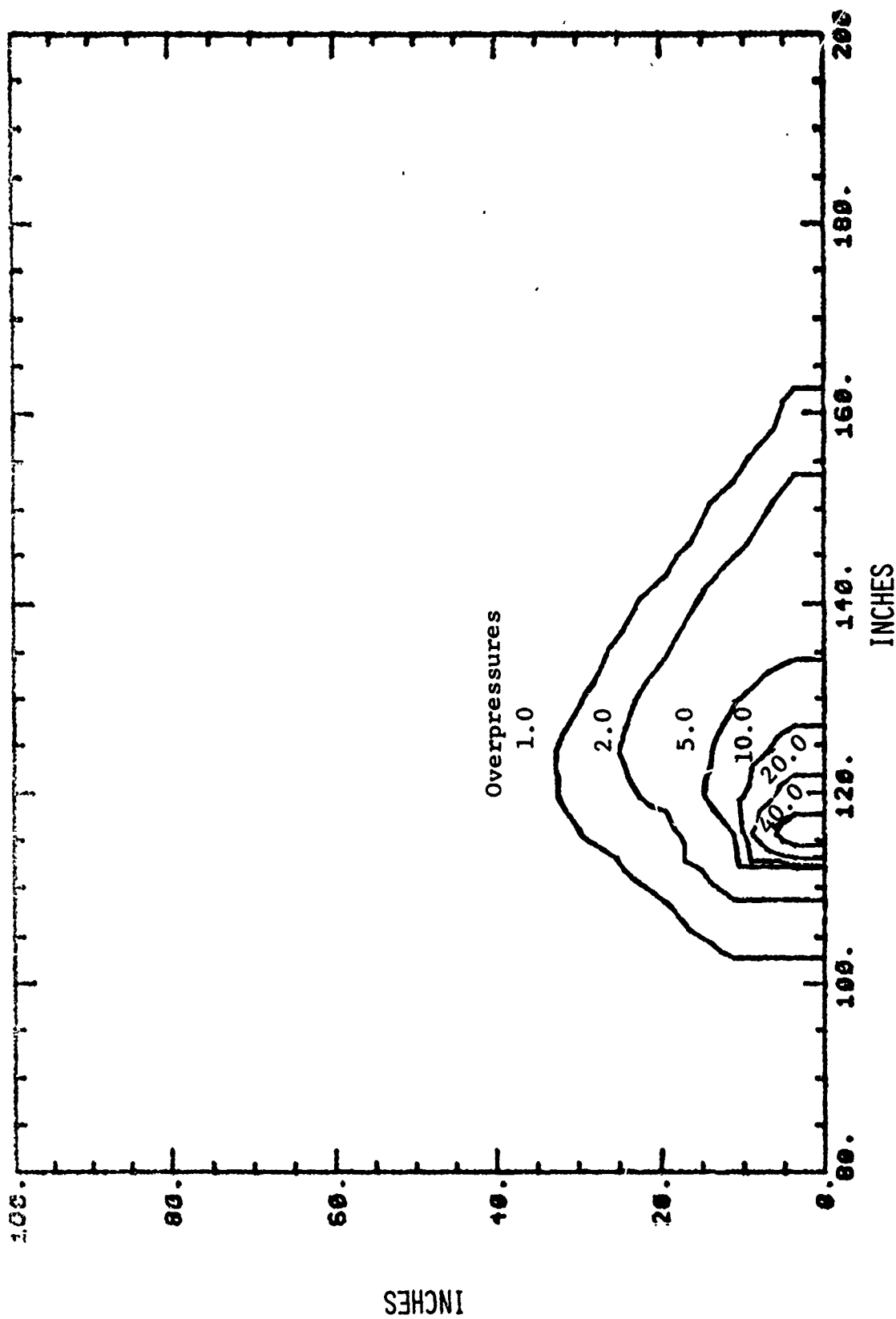


Figure 11 PRESSURE PROFILE CONTOURS, 3.5MSEC AFTER IGNITION, 5 LB WATER
1 MM DROP SIZE

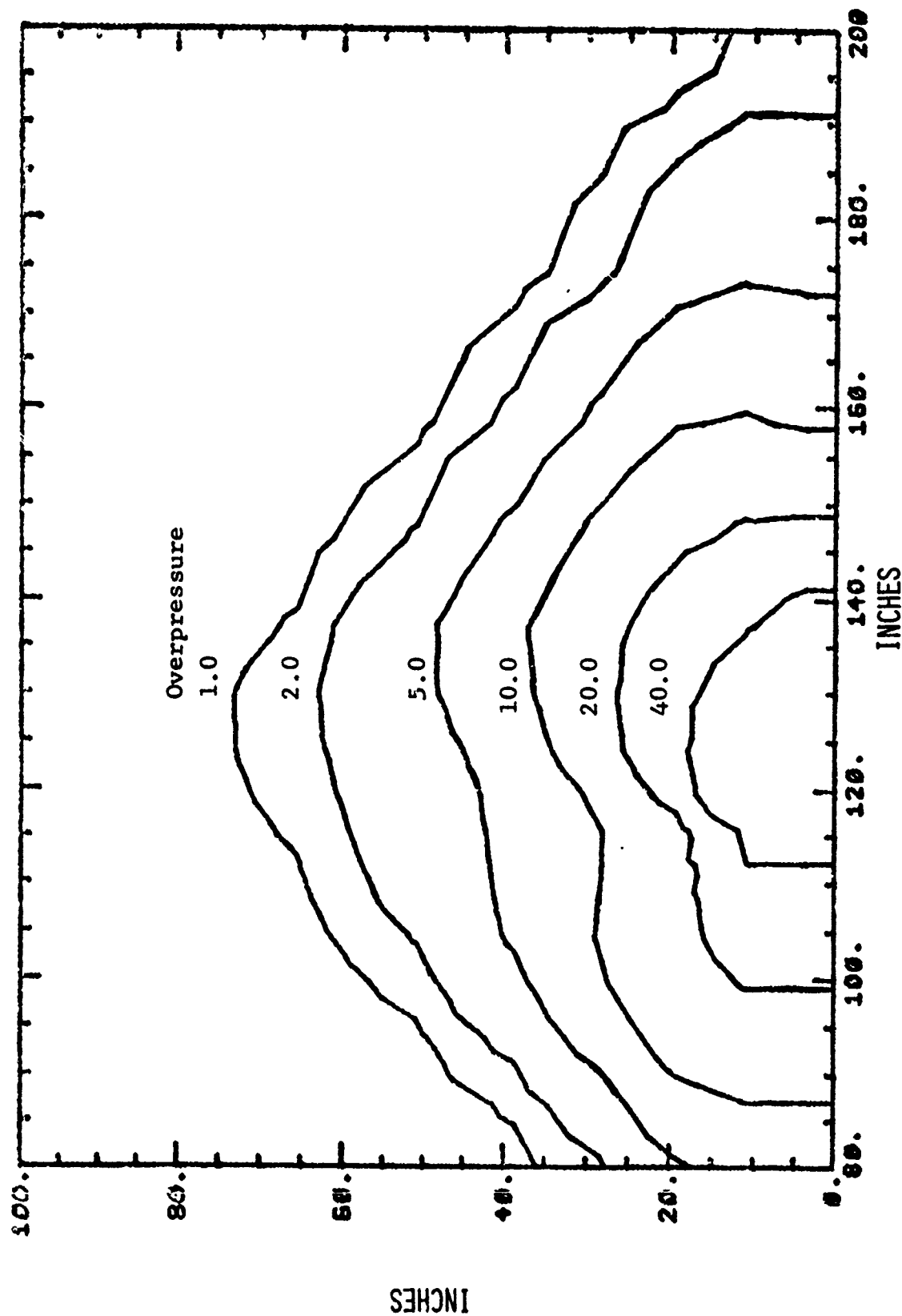


Figure 12 PRESSURE PROFILE CONTOURS, 5.7 MSEC AFTER IGNITION, 5 LB WATER, 1 MM DROP SIZE

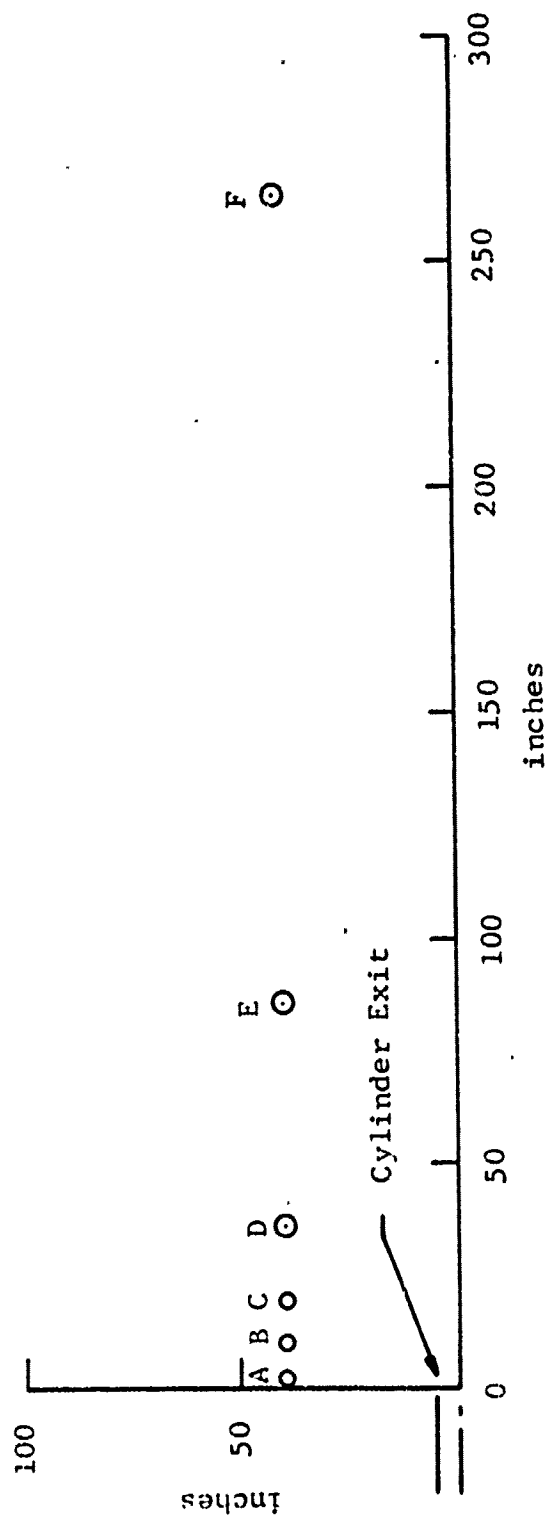


Figure 13 LOCATION OF POINTS IN BLAST FIELD FOR WHICH PRESSURE IS PLOTTED
AS A FUNCTION OF TIME

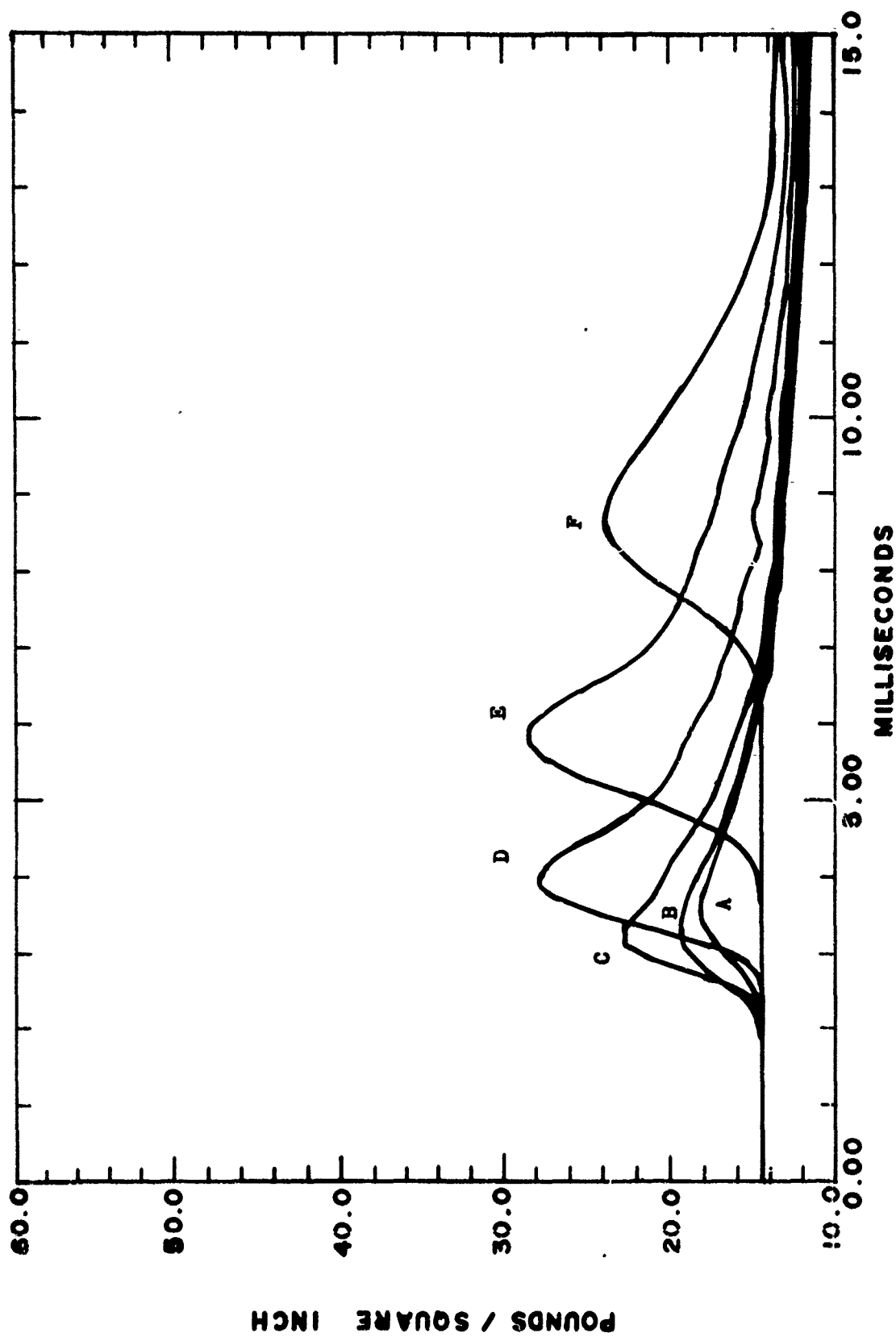


Figure 14. PRESSURE (STATIC PLUS DYNAMIC) VS TIME WITH NO WATER IN THE CYLINDER

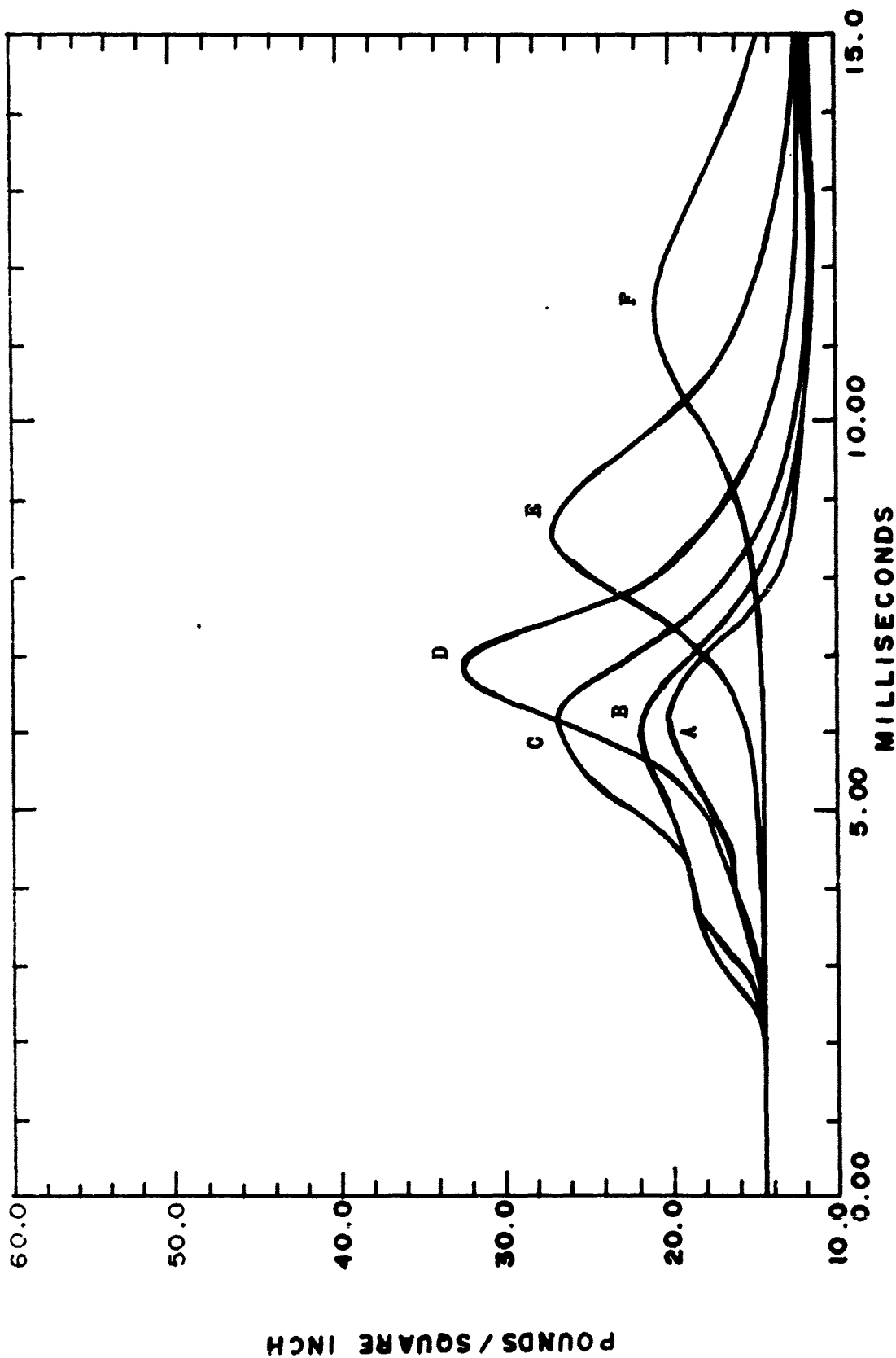


Figure 15 PRESSURE (STATIC PLUS DYNAMIC) VS TIME WITH 5 LB OF WATER IN THE CYLINDER, ASSUMED DROP SIZE - 5 M

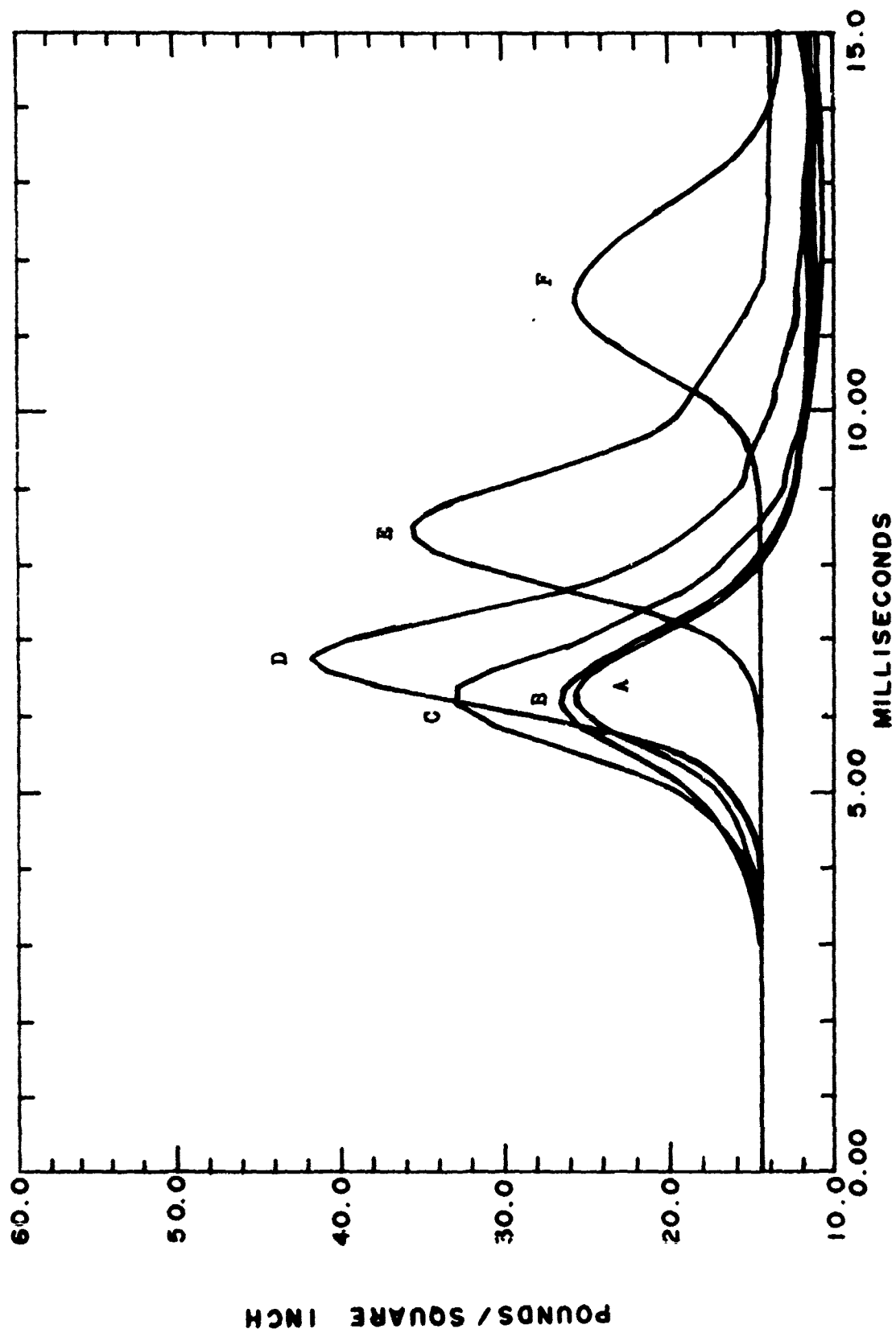


Figure 16 PRESSURE (STATIC PLUS DYNAMIC) VS TIME WITH 5 LB OF WATER IN THE CYLINDER, "ROP SIZE, 1 MM

5. SUMMARY OF RESULTS AND CONCLUSIONS

Contrary to the reasons advanced for expecting blast attenuation, the results obtained show that the peak pressure is increased rather than reduced by expelling water. The duration of the pulse is shorter, however, so that the total blast load represented in the pulse may be somewhat reduced. The most probable explanation involves the effect of flow duration and perhaps also the ability of the particles to transfer momentum to the blast field after expulsion from the cylinder.

In the study of the short cylinder concept it was thought that an optimum particle size might exist that would prolong flow duration, thereby reducing the peak blast pressure. It appears, however, that particles of suitable size, on the order of 1 mm, also have a drag-to-weight ratio so large that the momentum absorbed from the propellant gas in the cylinder is given back to the air when the particles emerge. The remaining hope for reducing the blast pressure with a concept involving particle expulsion is to use considerably more water so as to absorb more energy from the propellant gas, or to exploit other phenomena not investigated in this study, such as quenching the gas by the cooling effect of droplet vaporization.

REFERENCES

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6. McAdams, Heat Transmission, McGraw-Hill Publishing Co. (1954).
7. Gentry, R. A.; Martin, R. E.; and Daly, B. J., "An Eulerian Differencing Method for Unsteady Compressible Flow Problems," Computational Phys., Vol. 1, pp 87-118 (1966).

APPENDIX A
ONE-DIMENSIONAL GAS PARTICLE FLOW

MA	NO01	MA	NO02	MA	NO03	MA	NO04	MA	NO05	MA	NO06	MA	NO07	MA	NO08	MA	NO09	MA	NO10	MA	NO11	MA	NO12	MA	NO13	MA	NO14	MA	NO15	MA	NO16	MA	NO17	MA	NO18	MA	NO19	MA	NO20	MA	NO21	MA	NO22	MA	NO23	MA	NO24	MA	NO25	MA	NO26	MA	NO27	MA	NO28	MA	NO29	MA	NO30	MA	NO31	MA	NO32	MA	NO33	MA	NO34	MA	NO35	MA	NO36	MA	NO37	MA	NO38	MA	NO39
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DIMENSION Y(NRKD),DY(NRKD),AE(NRKD),RE(NRKD),AEF(7)
COMMON / NRK / NRK
COMMON / ALL / IM,K,KP,KM,IPL1,IP-2,KST,KKST,IMW,KS,KK,KKO,
2 VFS,NFE,APS,PEJ,PRJ,IPQ,XB,ZMAX,Z3,IR,VHL(NDC),VHR(NDC),
3 FL,RWD,P,VISC,VFIN,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJW,CHAML,
4 WIDTH,CPP,EL,FORCE,DSCPSI,SR,DYDT,A,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(NDC,7),CS(NDC),EG(NDC),FV(NDC),TP(NDC),FM(NDC),UG(NDC),
6 UP(NDC),A(NDC),AE(NDC),V(NDC),VS(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PR(NDC),DP(NDC),DG(NDC),GF(NDC,7),G(NDC,7),Q(NDC),Z(NDC),ZB(NDC)
K,TGA(NDC),GCA(NDC),GEA(NDC),VFA(NDC),FMV(NDC)
COMMON / MD / KS,S,KSWM,KS'Y
COMMON / VC / NZ,Z,(7),ZWC(7),IZW(7),ZW(7),LEX
CONTINUE
1 READ (5,101) IM,K,KP,KM,KST,KKST,KS,S,KSWM,KSWM
101 FORMAT (8I10/I10)
2 WRITE (6,102) IM,K,KP,K,KST,KKST,KS,S,KSWM,KS,M
102 FORMAT (1I1,4X,2I1X,1H3,I5,1H3,I5,
3X,2H4)
2

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

3      5X,2-KP      ,1H,16,
4      5X,2-MCM     ,1H,16,
5      5X,3-KST      ,1H,16,
6      5X,4-KKST     ,1H,16,
7      5X,4-KSWS     ,1H,16,
8      5X,4-KSWH     ,1H,16,
9      5X,4-KSWH     ,1H,16,
      IF (IM) 10,4,10
4 STOP
1- CONTINUE
      READ (5,110) IR,ZR,ZMAX,ZPL1,ZPL2
110 FORMAT (110,4F10.5)
      READ (5,113) DP0,FL,ER,RHOP,CPP,VISCG,VFMIN,PDF,FJ,CMAX,PV1,PV2,
2 PV3
113 FORMAT (7F10.5,E10.5 / 5F10.5)
      WRITE (6,114) DP0,FL,ER,RHOP,CPP,VISCG,VFMIN,PDF,FJ,CMAX,PV1,PV2,
2 PV3
114 FORMAT (1H0,9X,3HDP0
      9X,2HFL
      9X,2HER
      9X,4HRHOP
      9X,3HCPP
      9X,5HVISCG
      9X,5HVFMIN
      9X,3HPDF
      9X,2HFI
      9X,4HCYAX
      9X,3HVP1
      9X,3HVP2
      9X,3HVP3
      READ (5,105) CHARG,PROJW,W20,WIDTH,SL,BORE,VCHAMB,CNA1,CNA2,
2 R,DTM,DEXC,ENL,GNWT
105 FORMAT (8F10.5 / 6F10.5)
      WRITE (6,106) CHARG,PROJW,W20,WIDTH,SL,BORE,VCHAMB,CNA1,CNA2,
2 R,DTM,DEXC,ENL,GNWT
106 FORMAT (1H0, 9X,6HCHARGE ,1H,1PE14,6, 7H POUNDS
      ,10X,5HPROJW ,1H, E14,6, 7H POUNDS
      ,10X,4HW20 ,1H, E14,6, 7H POUNDS
      ,10X,5WIDTH ,1H, E14,6, 7H INCHES

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5 10X,2-3L      1H2,      E14,6, 7H INCHES
6 10X,4-3ORE    1H2,      E14,6, 3H MY
7 10X,6-VCHAMB 1H2,      E14,5,13H CUBIC INCHES
8 10X,4-CHVA1   1H2,      E14,6, 8H DEGREES
9 10X,4-CHVA2   1H2,      E14,5, 8H DEGREES
A 10X,2-CHV     1H2,      E14,6, 7H INCHES
B 10X,3-CHV     1H2,      E14,6, 7H INCHES
C 10X,4-CHV     1H2,      E14,6, 7H INCHES
D 10X,3-CHV     1H2,      E14,6, 7H INCHES
E 10X,4-CHV     1H2,      E14,5, 7H POUNDS

      KK2=-1
      KK2=-1
      IRK=7*IM+5
      CALL CALXC (CVA1,CVA2,RN,DTM,DEXC,3L,BORE,VCHAMB,ENL,XC,XBS)
      WRITE (6,108) (1,XC(I),I=1,9)
      ID= FORNAT (1H / (1H 10X,2H1=,12,3X,6HXC(1)=,1PE14,6))
      CALL ZSPACE
      CALL IOFZB(ZPL1,2,54,IPL1)

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

CALL IOFZB(ZPL2*2.54,IPL2)
IP-1=IPL1-1
CALL IOFZ (-ENL*2.54,IEX)
IEX=IEX+1
WRITE (6,111) IR,ZR,ZMAX,ZPL1,ZPL2,IPL1,IPL2,IEX
111 FORMAT (1H0,5X,3H1R=,16.5X,3HZR=,1PE12.5,5X,5HZMAX=,E12.5,5X,
2 5HZPL1=,E12.5,5X,5HZPL2=,E12.5, / 1H,5X,5HZPL1=,E12.5,
3 5HZPL2=,E12.5,4H1EX=,16)
WRITE (6,112) (I,Z(I),ZB(I),A(I),A9(I),V(I),VB(I),I=1,IM)
112 FORMAT (1H1,5X,1H1,10X,1HZ,16X,2HZB,17X,1HA,18X,2HAB,17X,1HV,
1 1HX,2HVB / 1H,16.1PE19.6,5E19.6)
READ (5,112) VZW,(ZV(I),I=1,7)
112 FORMAT (1H0,7F10.5)
DO 5 I=1,NZ
ZZ=2.54*(XC(3)-ZW(I))
ZXC(I)=ZZ
CALL IOFZ (ZZ,II)
5 IZ(I)=II
WRITE (6,113) (I,IZ(I),ZV(I),ZXC(I),I=1,NZ)
113 FORMAT (1H0,14X,1H1,7X,3HZV,8X,2HZZ,12X,3HZXC /
2 (1H,10X,2I10.1PE14.5,E14.5)
DSCPSI=453.59*980.616/(2.54**2)
CCPCIN=2.54**3
AP=2.0*CHARG*453.59/(1.6*WIDTH*(2.54**3))
AC=0.25*3.141593*((BORE/25.4)**2)
ZZ=0.5*(XC(3)+XC(4))*2.54
CALL IOFZB(ZZ,NFS)
CALL IOFZB(2.54*XC(7),NFE)
NPS=NFE
NFE=NFE+1
CHAML=VCHAM*(2.54**3)/(0.25*3.141593*(0.1*BORE)**2)
ZZ=Z(NPS)+CHAML*2.54*4.0
CALL IOFZ (ZZ,NPE)
WRITE (6,109) NFS,Z(NFS),NFE,Z(NFE),VPS,Z(NPS),NPE,Z(NPE)
109 FORMAT (1H0, 9X,4HNFS=,16.5X,1PE14.6,
2 10X,4HNFE=,16.5X, E14.6/
3 10X,4HNPS=,16.5X, E14.6,
4 10X,4HNPE=,16.5X, E14.6)
F**=(3.141593/6.0)*RNOPE*(CPO/10)**3)

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CL=RHOP*(1.0-VFMIN)
FLLEN=WH20*453.59/(CL*0.25*3.141593*(DEXC*2.54)**2)
ZL=2.54*XC(4)-FLEN
CALL IOFZ(2.54*XC(4),I2)
CALL IOFZ(ZL,I1)
I1=I1-1
I2=I2-1
VOLP=(ZB(I2)-ZB(I1-1))*0.25*3.141593*((DEXC*2.54)**2)
CL=WH20*453.59/VOLP
CL=AMAX1(CL,1.3E-10)
FVPA=CL/FX1
VF=1.0-CL/RHOP
CGG=VF*0.0010294
IF (KST-1) 7,2,7
  2 Y(1)=CHARG
  3 Y(1)=0.0
  FVPA1=FVPA*1.3E-3
  
```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

FNP11=AMAX1(FNP11,1.0E-10/FMN)
ZP=CHAML+2.54*(4.0+XC(7))
CALL IOFZ (ZP,IPRJ)
VV=AB(IPRJ)*(ZP-Z3(IPRJ-1))
IMV=IPRJ
IPO=IMV
KSI=1
DO 11 I=1,14
  IF (I-IPRJ) 15,14,15
14 VV=VV
  GO TO 20
15 VV=V(I)
20 CONTINUE
  F(I,1)=0.0010694*VV
  F(I,3)=FNP11*VV
  F(I,5)=FMV*FNP11*VV
  F(I,4)=293.0*F(I,5)
  F(I,2)=F(I,1)*(-1.145E3)+F(I,4)
  F(I,6)=0.0
  F(I,7)=0.0
11 DO 12 I=11,12
  F(I,1)=CGG*V(I)
  F(I,3)=FNP11*V(I)
  F(I,5)=FNP11*V(I)
  F(I,4)=F(I,5)*293.0
  F(I,2)=F(I,1)*(-1.145E3)+F(I,4)
  DT=0.0001
7 CONTINUE
  EZ=ER*0.01
  DO 9 I=1,5
  RE(I)=ER
  AE(1)=EZ*CHRG
  AE(2)=EZ*2000.0
  AE(3)=EZ*140.0
  AE(4)=EZ*1000.0
  AE(5)=AE(4)
  AEF(1)=EZ*0.1
  AEF(2)=AEF(1)*1000.0
  AEF(3)=EZ*FNP1

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AEF(5)=EZ*FM*FNP
AEF(4)=AEF(5)*503.0
AEF(6)=AEF(1)*40000.0
AEF(7)=AEF(5)*40000.0
L=5
DO 6 I=1,14
CC 6 K=1,7
L=L+1
RE(L)=ER
AE(L)=AEF(K)*V(I)
V(L)=F(I,K)
REALD 6
REALD 9
REALD 10
REALD 11
IF (KST-2) 17,16,17
16 CONTINUE
CC 13 LL=1,1000

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

18 READ (9) KK,T,DT,IPRJ,IMW,KS,(Y(I),I=1,IRK)
19 READ (10) K9
20 IF (KK-KKST) 18,19,19
21 CONTINUE
22 DO 2 LL=1,10000
23 READ (8) KK1
24 READ (11) KK3
25 IF (KK1-KK) 8,13,13
26 CONTINUE
27 CONTINUE
28 KK=KK-1
29 IPC=IPRJ
30 CONTINUE
31 EXTERNAL DERIV,CTRL
32 CALL RK2 (DERIV,CTRL,Y,DY,AE,PE,T,DT,IRK,2,DE6)
33 RE*IND 8
34 RE*IND 9
35 RE*IND 10
36 RE*IND 11
37 GO TO 1
38 END

```

MAIN2290
 MAIN2300
 MAIN2310
 MAIN2320
 MAIN2330
 MAIN2340
 MAIN2350
 MAIN2360
 MAIN2370
 MAIN2380
 MAIN2390
 MAIN2400
 MAIN2410
 MAIN2420
 MAIN2430
 MAIN2440
 MAIN2450
 MAIN2460
 MAIN2470
 MAIN2480
 MAIN2490
 MAIN2500

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE DERIV(Y,DY,T)
Y(1)= UNBURNT PROPELLANT POUNDS
Y(2)= PROJECTILE VELOCITY FT/SEC
Y(3)= TRAVEL INCHES
Y(4)= IMPULSE POUNDS X SEC
Y(5)= IMPULSE X TIME POUND X SEC XX 2
PARAMETER NRK=200
DIMENSION Y(1:NRK),DY(NRK)
COMMON /ALL/ IM,K,KP,KM,IP,L2,KST,KKST,IMW,KS,KK,KKO,
2 NFS,NFS,NFS,NPE,IPRJ,IPQ,XSB,ZMAX,ZR,IR,VHL(NDC),VHR(NDC),
3 FL,RHCP,VISC,VFWIN,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJW,CHAML,
4 WIDTH,CPP,BL,FORCE,DSCPSI,BR,DYDT,A,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(NDC),CG(NDC),EG(NDC),FM(NDC),TP(NDC),FN(NDC),UG(NDC),
6 UP(NDC),A(NDC),AB(NDC),V(NDC),VB(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PD(NDC),OP(NDC),DG(NDC),DF(NDC,7),G(NDC,7),Q(NDC),Z(NDC),ZB(NDC),
8 TGA(NDC),GEA(NDC),GEA(NDC),VFA(NDC),FMV(NDC)
DATA C/0.01/
L=5
DO 12 I=1,IM4
DO 12 K=1,7
L=L+1
12 F(I,K)=Y(L)
ZPROJ=Y(3)
VPROJ=Y(2)
CALL DERIV(Y(1))
L=5
DO 13 I=1,IM4
DO 13 K=1,7
L=L+1
13 DY(L)=DF(I,K)
DY(1)=DYDT
IF(Y(3)+4.0-AL) 9,9,8
8 DY(2)=0.0
GO TO 10
9 DY(2)=PG(IPRJ)*AC*32.1724/(PROJW*DSCPSI)
10 DY(3)=Y(2)*12.0
FORCE=0.0
DO 11 I=1,NFS,NFS

```

DER10010
 DER10020
 DER10030
 DER10040
 DER10050
 DER10060
 DER10070
 DER10080
 DER10090
 DER10100
 DER10110
 DER10120
 DER10130
 DER10140
 DER10150
 DER10160
 DER10170
 DER10180
 DER10190
 DER10200
 DER10210
 DER10220
 DER10230
 DER10240
 DER10250
 DER10260
 DER10270
 DER10280
 DER10290
 DER10300
 DER10310
 DER10320
 DER10330
 DER10340
 DER10350
 DER10360
 DER10370
 DER10380
 DER10390

```
17 FORCE=FORCE+PG(I)*(AB(I-1)-AB(I))  
   FORCE=FORCE/(380,616+453,59)  
   DY(4)=FORCE  
   DY(5)=Y(4)  
   RETURN  
   END
```

```
DER10400  
DER10410  
DER10420  
DER10430  
DER10440  
DER10450
```

DER10010
DER10020
DER10030
DER10040
DER10050
DER10060
DER10070
DER10080
DER10090
DER10100
DER10110
DER10120
DER10130
DER10140
DER10150
DER10160
DER10170
DER10180
DER10190
DER10200
DER10210
DER10220
DER10230
DER10240
DER10250
DER10260
DER10270
DER10280
DER10290
DER10300
DER10310
DER10320
DER10330
DER10340
DER10350
DER10360
DER10370
DER10380
DER10390

F(1,1)	=	MASS OF GAS
F(1,2)	=	TOTAL ENERGY, BOTH PHASES
F(1,3)	=	NUMBER OF PARTICLES
F(1,4)	=	SENSIBLE HEAT IN PARTICLE PHASE
F(1,5)	=	MASS OF PARTICLES
F(1,6)	=	TOTAL MOMENTUM, BOTH PHASES
F(1,7)	=	MOMENTUM OF PARTICLE PHASE
G(1,1)	=	FLUX OF GAS
G(1,2)	=	FLUX OF TOTAL ENERGY
G(1,3)	=	FLUX OF PARTICLES
G(1,4)	=	FLUX OF PARTICLE SENSIBLE HEAT
G(1,5)	=	FLUX OF PARTICLE MASS
G(1,6)	=	FLUX OF TOTAL MOMENTUM
G(1,7)	=	FLUX OF PARTICLE MOMENTUM

```

PARAMETER NDC=200
DIMENSION EKGA(NDC),EKPA(NDC)
COMMON /ALL/ IM,K,KP,KM,IPL1,IPL2,KST,KKST,IMW,KS,KK,KK0,
2 NKS,NFE,NPS,NPE,IPRJ,IPO,XBB,ZMAX,Z1,IR,VHL(NDC),VHR(NDC),
3 FL,RWOP,VISCG,VF,IN,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJM,CHAML,
4 WIDTH,CPP,BL,FORCE,DSCPSI,BR,DYDT,A,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(NDC,7),CG(NDC),EG(NDC),FN(NDC),FM(NDC),UG(NDC),
6 UP(NDC),A(NDC),AB(NDC),V(NDC),VE(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PC(NDC),DP(NDC),CG(NDC),DF(NDC,7),G(NDC,7),G(NDC),Z(NDC),ZB(NDC),
8 TCAL(NDC),SCAL(NDC),GEA(NDC),VEA(NDC),FHV(NDC)

```

COPY / NO / KS-5, KSH, KS-7

DATA ENTRY-13

14. P13194+1

THE

GO TO (29.30) K53

$$\int_0^1 \int_0^1 (x+y) \, dx \, dy = \frac{1}{2}$$

07-0041187-47) • (P#41) EVZAA/VVz

3-11-68

COPIES

$x=1,5$

$$F(1, K) = (2, G \circ F(2, K) / V(2) - F(3, K) / V(3)) \circ V(1)$$
$$F(Y, \lambda, \kappa) = F(Y, \kappa) \circ V(M+I)/V(M)$$

February 2003

DER10400
DER10410
DER10420
DER10430
DER10440
DER10450
DER10460
DER10470
DER10480
DER10490
DER10500
DER10510
DER10520
DER10530
DER10540
DER10550
DER10560
DER10570

```

CG(I)=F(I,1)/V(I)
FN(I)=ANAX1(FMN,F(I,3))/V(I)
FNV(I)=ANAX1(FMN,F(I,5))/V(I)
FM(I)=FMV(I)/FN(I)
2 CONTINUE
GO TO (41,32),KSW
41 CG(IPRJ)=F(IPRJ,1)/VV
FN(IPRJ)=ANAX1(FMN,F(IPRJ,3))/VV
FMV(IPRJ)=ANAX1(FMN,F(IPRJ,5))/VV
32 CONTINUE
DO 3 I=2,IM
  CG=(VM2(I)*CG(I)+VHL(I+1)*CG(I+1))/VB(I)
  FMB=(VM2(I)*FNV(I)+VHL(I+1)*FNV(I+1))/VB(I)
  GO TO (42,33),KSDS
42 CONTINUE
UP(I)=F(I,7)/(FMB*VB(I))
UG(I)=(F(I,6)-F(I,7))/(CGB*VB(I))
GO TO 3

```

```

33 CONTINUE
  UP(I)=F(I,6)/((CG5+FM6)*VB(I))
  UG(I)=UP(I)
3 CONTINUE
  UG(I)=(2.0*UG(2)*AS(2)-UG(3)*AS(3))/AB(1)
  UP(I)=(2.0*UP(2)*AS(2)-UP(3)*AS(3))/AB(1)
  GO TO (4,3),K54
4 UG(IPRJ)=33.45*VP+QJ
  UP(IPRJ)=33.45*VP+QJ
5 UG(IM+1)=JG(IM)*AB(IM)/AB(IM+1)
  UP(IM+1)=UP(IM)*AB(IM)/AB(IM+1)
4 CONTINUE
  DO 7 I=2,I*NP1
    EKS=(VH(I))*UG(I)*2+VHL(I)*UG(I-1)*2)/(2.0*V(I))
    EKP=(VH(I))*UP(I)*2+VHL(I)*UP(I-1)*2)/(2.0*V(I))
    EKSA(I)=EKG
    EKPA(I)=EKP
  GO TO (35,34),K544
35 CONTINUE
  EG(I)=(F(I,2)-F(I,4)-F(I,5)*EK2/FJ)/=(I,1)-EKG/FJ
  TP(I)=F(I,4)/(F(I,5)*CFF)
  CALL TOEAR (EG(I),RHOG(I),TGA(I))
  GO TO 7
36 CONTINUE
  SF(I,2)=(F(I,1)*EKG+F(I,5)*EK2)/FJ
  VF=1.0-FMV(I)/RHOG
  RHOG=CG(I)/VF
  F1=3.627725E3+RHOG*(1.041936E3-RHOG*1.501111E3)
  F2=1.635622+RHOG*(2.115013-RHOG*1.648174)
  F3=-0.107984E-2+RHOG*(-0.686307E-3+RHOG*0.422347E-2)
  W1=F1*F(I,5)*CFF-S
  W2=F2*F(I,5)*CFF+F(I,1)
  W3=F3*F(I,5)*CFF
  IF (F(I,5)-1.0E-4*F(I,1))23,24,24
23 CONTINUE
  ET=-1000.0
  ET=ET-(W1+ET*(W2+ET*(W3+ET*(W4+ET*(W5+ET*(W6+ET*(W7+ET*(W8+ET*(W9+ET*(W10+ET*(W11+ET*(W12+ET*(W13+ET*(W14+ET*(W15+ET*(W16+ET*(W17+ET*(W18+ET*(W19+ET*(W20+ET*(W21+ET*(W22+ET*(W23+ET*(W24+ET*(W25+ET*(W26+ET*(W27+ET*(W28+ET*(W29+ET*(W30+ET*(W31+ET*(W32+ET*(W33+ET*(W34+ET*(W35+ET*(W36+ET*(W37+ET*(W38+ET*(W39+ET*(W40+ET*(W41+ET*(W42+ET*(W43+ET*(W44+ET*(W45+ET*(W46+ET*(W47+ET*(W48+ET*(W49+ET*(W50+ET*(W51+ET*(W52+ET*(W53+ET*(W54+ET*(W55+ET*(W56+ET*(W57+ET*(W58+ET*(W59+ET*(W60+ET*(W61+ET*(W62+ET*(W63+ET*(W64+ET*(W65+ET*(W66+ET*(W67+ET*(W68+ET*(W69+ET*(W70+ET*(W71+ET*(W72+ET*(W73+ET*(W74+ET*(W75+ET*(W76+ET*(W77+ET*(W78+ET*(W79+ET*(W80+ET*(W81+ET*(W82+ET*(W83+ET*(W84+ET*(W85+ET*(W86+ET*(W87+ET*(W88+ET*(W89+ET*(W90+ET*(W91+ET*(W92+ET*(W93+ET*(W94+ET*(W95+ET*(W96+ET*(W97+ET*(W98+ET*(W99+ET*(W100+ET*(W101+ET*(W102+ET*(W103+ET*(W104+ET*(W105+ET*(W106+ET*(W107+ET*(W108+ET*(W109+ET*(W110+ET*(W111+ET*(W112+ET*(W113+ET*(W114+ET*(W115+ET*(W116+ET*(W117+ET*(W118+ET*(W119+ET*(W120+ET*(W121+ET*(W122+ET*(W123+ET*(W124+ET*(W125+ET*(W126+ET*(W127+ET*(W128+ET*(W129+ET*(W130+ET*(W131+ET*(W132+ET*(W133+ET*(W134+ET*(W135+ET*(W136+ET*(W137+ET*(W138+ET*(W139+ET*(W140+ET*(W141+ET*(W142+ET*(W143+ET*(W144+ET*(W145+ET*(W146+ET*(W147+ET*(W148+ET*(W149+ET*(W150+ET*(W151+ET*(W152+ET*(W153+ET*(W154+ET*(W155+ET*(W156+ET*(W157+ET*(W158+ET*(W159+ET*(W160+ET*(W161+ET*(W162+ET*(W163+ET*(W164+ET*(W165+ET*(W166+ET*(W167+ET*(W168+ET*(W169+ET*(W170+ET*(W171+ET*(W172+ET*(W173+ET*(W174+ET*(W175+ET*(W176+ET*(W177+ET*(W178+ET*(W179+ET*(W180+ET*(W181+ET*(W182+ET*(W183+ET*(W184+ET*(W185+ET*(W186+ET*(W187+ET*(W188+ET*(W189+ET*(W190+ET*(W191+ET*(W192+ET*(W193+ET*(W194+ET*(W195+ET*(W196+ET*(W197+ET*(W198+ET*(W199+ET*(W200+ET*(W201+ET*(W202+ET*(W203+ET*(W204+ET*(W205+ET*(W206+ET*(W207+ET*(W208+ET*(W209+ET*(W210+ET*(W211+ET*(W212+ET*(W213+ET*(W214+ET*(W215+ET*(W216+ET*(W217+ET*(W218+ET*(W219+ET*(W220+ET*(W221+ET*(W222+ET*(W223+ET*(W224+ET*(W225+ET*(W226+ET*(W227+ET*(W228+ET*(W229+ET*(W230+ET*(W231+ET*(W232+ET*(W233+ET*(W234+ET*(W235+ET*(W236+ET*(W237+ET*(W238+ET*(W239+ET*(W240+ET*(W241+ET*(W242+ET*(W243+ET*(W244+ET*(W245+ET*(W246+ET*(W247+ET*(W248+ET*(W249+ET*(W250+ET*(W251+ET*(W252+ET*(W253+ET*(W254+ET*(W255+ET*(W256+ET*(W257+ET*(W258+ET*(W259+ET*(W260+ET*(W261+ET*(W262+ET*(W263+ET*(W264+ET*(W265+ET*(W266+ET*(W267+ET*(W268+ET*(W269+ET*(W270+ET*(W271+ET*(W272+ET*(W273+ET*(W274+ET*(W275+ET*(W276+ET*(W277+ET*(W278+ET*(W279+ET*(W280+ET*(W281+ET*(W282+ET*(W283+ET*(W284+ET*(W285+ET*(W286+ET*(W287+ET*(W288+ET*(W289+ET*(W290+ET*(W291+ET*(W292+ET*(W293+ET*(W294+ET*(W295+ET*(W296+ET*(W297+ET*(W298+ET*(W299+ET*(W300+ET*(W301+ET*(W302+ET*(W303+ET*(W304+ET*(W305+ET*(W306+ET*(W307+ET*(W308+ET*(W309+ET*(W310+ET*(W311+ET*(W312+ET*(W313+ET*(W314+ET*(W315+ET*(W316+ET*(W317+ET*(W318+ET*(W319+ET*(W320+ET*(W321+ET*(W322+ET*(W323+ET*(W324+ET*(W325+ET*(W326+ET*(W327+ET*(W328+ET*(W329+ET*(W330+ET*(W331+ET*(W332+ET*(W333+ET*(W334+ET*(W335+ET*(W336+ET*(W337+ET*(W338+ET*(W339+ET*(W340+ET*(W341+ET*(W342+ET*(W343+ET*(W344+ET*(W345+ET*(W346+ET*(W347+ET*(W348+ET*(W349+ET*(W350+ET*(W351+ET*(W352+ET*(W353+ET*(W354+ET*(W355+ET*(W356+ET*(W357+ET*(W358+ET*(W359+ET*(W360+ET*(W361+ET*(W362+ET*(W363+ET*(W364+ET*(W365+ET*(W366+ET*(W367+ET*(W368+ET*(W369+ET*(W370+ET*(W371+ET*(W372+ET*(W373+ET*(W374+ET*(W375+ET*(W376+ET*(W377+ET*(W378+ET*(W379+ET*(W380+ET*(W381+ET*(W382+ET*(W383+ET*(W384+ET*(W385+ET*(W386+ET*(W387+ET*(W388+ET*(W389+ET*(W390+ET*(W391+ET*(W392+ET*(W393+ET*(W394+ET*(W395+ET*(W396+ET*(W397+ET*(W398+ET*(W399+ET*(W400+ET*(W401+ET*(W402+ET*(W403+ET*(W404+ET*(W405+ET*(W406+ET*(W407+ET*(W408+ET*(W409+ET*(W410+ET*(W411+ET*(W412+ET*(W413+ET*(W414+ET*(W415+ET*(W416+ET*(W417+ET*(W418+ET*(W419+ET*(W420+ET*(W421+ET*(W422+ET*(W423+ET*(W424+ET*(W425+ET*(W426+ET*(W427+ET*(W428+ET*(W429+ET*(W430+ET*(W431+ET*(W432+ET*(W433+ET*(W434+ET*(W435+ET*(W436+ET*(W437+ET*(W438+ET*(W439+ET*(W440+ET*(W441+ET*(W442+ET*(W443+ET*(W444+ET*(W445+ET*(W446+ET*(W447+ET*(W448+ET*(W449+ET*(W450+ET*(W451+ET*(W452+ET*(W453+ET*(W454+ET*(W455+ET*(W456+ET*(W457+ET*(W458+ET*(W459+ET*(W460+ET*(W461+ET*(W462+ET*(W463+ET*(W464+ET*(W465+ET*(W466+ET*(W467+ET*(W468+ET*(W469+ET*(W470+ET*(W471+ET*(W472+ET*(W473+ET*(W474+ET*(W475+ET*(W476+ET*(W477+ET*(W478+ET*(W479+ET*(W480+ET*(W481+ET*(W482+ET*(W483+ET*(W484+ET*(W485+ET*(W486+ET*(W487+ET*(W488+ET*(W489+ET*(W490+ET*(W491+ET*(W492+ET*(W493+ET*(W494+ET*(W495+ET*(W496+ET*(W497+ET*(W498+ET*(W499+ET*(W500+ET*(W501+ET*(W502+ET*(W503+ET*(W504+ET*(W505+ET*(W506+ET*(W507+ET*(W508
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A-15

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DER10970
DER10980
DER10990
DER11000
DER11010
DER11020
DER11030
DER11040
DER11050
DER11060
DER11070
DER11080
DER11090
DER11100
DER11110
DER11120
DER11130
DER11140

```

GO TO 902
C FLAG EG(I)=(SQRT(W2*W2-4.0*W1*W3)-W2)/(2.0*W3)
C      24 WTST=X2*W2-4.0*W1*W3
      WTST1=MAX1(WTST,C,0)
      EG(I)=(SQRT(WTST1-W2)/(2.0*W3)
      IF (WTST) 901,902,902
901 WRITE (6,A01) I,S,RHO,WTST,W1,W2,W3,F1,F2,F3
A01 FORMAT (1H,5X,12HDER1 WARNING,5X,2-I=,15,5X,2HS=.1PE12,5,5X,
2 4-HO=.E12,5,5X,3HWTST=.E12,5 / 1H,5X,3HW1=.E12,5,5X,3HW2=.
3 E12,5,5X,3HW3=.E12,5,5X,3HF1=.E12,5,5X,3HF2=.E12,5,5X,
4 3-F3=.E12,5)
902 CONTINUE
      CALL TOEAR (EG(I),RHO,TP(I))
      TGA(I)=TP(I)
7 CONTINUE
      EG(1)=2.0*EG(2)-EG(3)
      TP(1)=2.0*TP(2)-TP(3)

```


ONE DIMENSIONAL GAS PARTICLE FLOW

```

DO 11 I=1,IM*PI
VF=1.0-FMV(I)/RHOP
VFA(I)=VF
RHOG(I)=CG(I)/VF
CALL EGSTAT(EG(I),RHOG(I),PSI)
PC(I)=PSI*DSICPSI
IF(VF-VFMIN)9,5,9
5 PC(I)=0.0
GO TO 10
9 VF=AMAX1(VF,1.0E-10)
VR=VF/VFMIN
PC(I)=POF*(1.0/(VR*VR)+2.0*VR-3.0)
10 DF3=6.0*FM(I)/(RHP*3.141593)
11 DP(I)=ROTC(DP3,3)
DO 12 I=2,IM
DU=-(UG(I)*AB(I)-UG(I-1)*AB(I-1))/A(I)
DU=AMAX1(DU,3.0)
O(I)=FL*CG(I)*DU*(DU+50000.0)
DU=-(UP(I)*AB(I)-UP(I-1)*AB(I-1))/A(I)
DU=AMAX1(DU,3.0)
PC(I)=FL*DU*(DU+50000.0)+PD(I)
12 CONTINUE
PC(I)=0.0
3(I)=0.0
DO 13 I=2,IM
P1=PG(I+1)+G(I+1)+FMV(I+1)*PD(I+1)
P2=PG(I)+G(I)+FMV(I)*PD(I)
DF(I,6)=(P1-P2)*AB(I)
GO TO (36,28),KSW
36 CONTINUE
DU=UP(I)-UG(I)
RHOG=3.5*(R-UG(I+1)+RHOG(I))
DFB=0.5*(DP(I)+DP(I+1))
RE=DPB+RHJGB*ABS(DU)/VISCG
DG(I)=0.125*3.141593*CORE*VISCG*DPB*DU
FNB=0.5*(FN(I+1)+FN(I))
FMVB=0.5*(FMV(I+1)+FMV(I))
DF(I,7)=-AB(I)*(FMV(I+1)*PD(I+1)-FMV(I)*PD(I))

```

DER11150
 DER11160
 DER11170
 DER11180
 DER11190
 DER11200
 DER11210
 DER11220
 DER11230
 DER11240
 DER11250
 DER11260
 DER11270
 DER11280
 DER11290
 DER11300
 DER11310
 DER11320
 DER11330
 DER11340
 DER11350
 DER11360
 DER11370
 DER11380
 DER11390
 DER11400
 DER11410
 DER11420
 DER11430
 DER11440
 DER11450
 DER11460
 DER11470
 DER11480
 DER11490
 DER11500
 DER11510
 DER11520
 DER11530

```

2 -(PG(I+1)-PG(I))*AB(I)*FMVB/R40=
DF(I,7)=DF(I,7)+FVB*DG(I)*VB(I)
GC TO 13
29 CONTINUE
13 DF(I,7)=C.C
13 CONTINUE
GC 14 I=1,IMXF1
IM1=I-1
IM2=MAX0(IM1,1)
UB=C.5*(UP(I)+UP(IM1))
CALL LOFU(UB,L)
G(I,7)=A(I)*FV(I)*(UP(IM1+L)**2)
G(I,6)=G(I,7)
UB=C.5*(UG(I)+UG(IM1))
CALL LOFU(UB,L)
G(I,6)=G(I,6)+A(I)*CG(I)*UG(IM1+L)**2
CALL LOFU(UP(I),L)
IL=I+L

```

```

DER11540
DER11550
DER11560
DER11570
DER11580
DER11590
DER11600
DER11610
DER11620
DER11630
DER11640
DER11650
DER11660
DER11670
UER11680
UER11690
DER11700
DER11710

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ONE DIMENSIONAL GAS PARTICLE FLOW

```

IL=MINO(I*PI,IL)
ILM1=IL-1
ILM1=MAXO(ILM1,1)
G(I,3)=AB(I)*UP(I)*FN(IL)
G(I,5)=AB(I)*JP(I)*FMV(IL)
G(I,4)=AB(I)*JP(I)*FMV(IL)*CPP*TP(IL)
G(I,2)=G(I,4)
2  +4G(I)*UP(I)*FMV(IL)*(EKP*(IL)+2G(IL)+(PG(IL)+G(IL))/RHOP)/FJ
CALL LOFU (UG(I),L)
IL=I+L
IL=MINO(I*PI,IL)
ILM1=IL-1
ILM1=MAXO(ILM1,1)
G(I,1)=AB(I)*UG(I)*CG(IL)
G(I,2)=G(I,2)+AB(I)*UG(I)*(YFA(IL)*(2G(IL)+3(IL))/FJ
2  +CG(IL)*(EG(IL)+EKG(IL)/FJ)
14 CONTINUE
PR=0.0
20 51 I=VPS,NPE
51 PR=PB+PG(I)
PB=PB/FLOAT(NPE-NPS+1)
PB=PB/DSCPSI
PC=MAX1(200.0,PS)
RR=0.00186*(PC**0.83)
DYDT=-AP*RR*1.6*CCPCIN/453.59
EE=YONE/CHARG
IF (ABS(EE)-1.0E-5) 201,202,202
201 DYDT=0.0
GO TO 204
202 IF (ABS(EE)-0.01) 203,204,204
203 DYDT=DYDT*EE/0.01
204 CONTINUE
DWDI=-DYDT*453.59/(A(NPE)*(23(NPE)-23(NPS-1)))
DO 18 I=2,IMW
GO TO (48,44),KSW
48 IF(I-IPRJ) 44,43,44
43 VVV=VV
GO TO 45
44 VVV=V(I)

```

DER11720
 DER11730
 DER11740
 DER11750
 DER11760
 DER11770
 DER11780
 DER11790
 DER11800
 DER11810
 DER11820
 DER11830
 DER11840
 DER11850
 DER11860
 DER11870
 DER11880
 DER11890
 DER11900
 DER11910
 DER11920
 DER11930
 DER11940
 DER11950
 DER11960
 DER11970
 DER11980
 DER11990
 DER12000
 DER12010
 DER12020
 DER12030
 DER12040
 DER12050
 DER12060
 DER12070
 DER12080
 DER12090
 DER12100

```

45 CONTINUE
   DF(I,1)=-G(I,1)-G(I-1,1)
   IF(I-NPS)17,15,15
   15 IF(I-NPE)16,16,17
   16 DF(I,1)=DF(I,1)+D*DT*VVV
   17 DF(I,2)=-G(I,2)-G(I-1,2)
   DF(I,3)=-G(I,3)-G(I-1,3)
   DF(I,4)=-G(I,4)-G(I-1,4)
   DF(I,5)=-G(I,5)-G(I-1,5)
   DF(I,6)=DF(I,6)-(G(I+1,6)-G(I,6))
   DF(I,7)=DF(I,7)-(G(I+1,7)-G(I,7))
   GO TO (37,46),KSW+1
37 CONTINUE
   DU=0.5*(UP(I)-UG(I)+UP(I-1)-UG(I-1))
   RE=DP(I)*RHOG(I)*ABS(DU)/VISC
   REP6=RODT(RE,5)
   REP6=REP6*REP6*REP6
   FNU=2.0+0.34*.89*REP6

```

```

DER12110
DER12120
DER12130
DER12140
DER12150
DER12160
DER12170
DER12180
DER12190
DER12200
DER12210
DER12220
DER12230
DER12240
DER12250
DER12260
DER12270
DER12280

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

H=FNU*0.25*VISCG/(0.7*DP(I))
TG=TGA(I)
TPT=TP(I)
QC=(TPT-TG)*H*(DP(I)**2)*3.141593
GO TO (38,39),KSWX
38 CONTINUE
GK=FNU*VISCG/(PG(I)*DP(I)*0.7)
PVL=PV1-PV2/(TP(I)-273.0+PV3)
PVL=AMIN1(PVL,30.0)
PV=EXP(PVL*2.302585)
C FLAG
C
PV=AMIN1(PV,760.0)
PV=14.7*(PV/760.0)*DSCPSI
DMDDT=3.141593*GK*(DP(I)**2)*(PV-0.19*PG(I))
DMDDT=AMAX1(DMDDT,0.0)
GO TO 40
39 DMDDT=0.0
40 CONTINUE
DF(I,1)=DF(I,1)+DMDDT*F(I,3)
GE=DMDDT*560.0
QF(I,4)=QF(I,4)-(DMDDT*TP(I)*CAP+QC+3E)*F(I,3)
DF(I,5)=DF(I,5)-DMDDT*F(I,3)
GO TO 47
46 QC=0.0
GE=0.0
DF(I,4)=0.0
47 CONTINUE
QCA(I)=QC
GEA(I)=GE
18 CONTINUE
GEA(I)=0.0
GEA(IMWP1)=GEA(IM4)
DO 22 I=2,IMW
GO TO (26,27),KSWX
25 DF(I,7)=DF(I,7)-(GEA(I)*FN(I)*VWR(I)+GEA(I+1)*FN(I+1)*VWL(I+1))
2 *UP(I)/560.0
GO TO 22
27 DF(I,7)=0.0
22 CONTINUE

```

DER12680
DER12690
DER12700
DER12710
DER12720
DER12730
DER12740
DER12750
DER12760

00 21 K=1.7
21 DF(1,K)=0.0
GO TO (19,20),KSW
19 I=IPRJ
DF(1,6)=0.0
DF(1,7)=0.0
20 CONTINUE
RETURN
END

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE CNTRL (Y,DY,DT,T,NTRY)
PARAMETER NDC=200
PARAMETER NRKC=1800
DIMENSION Y(NRKC),DY(NRKC)
COMMON /ALL/ IM,K,KP,KM,IPL1,IPL2,KST,KKST,IMW,KSW,KK,KKO,
2 NPS,NFE,NPS,NPE,IPRJ,IPO,XBB,ZMAX,ZR,IR,VHL(NDC),VHR(NDC),
3 FL,RHDP,VISC,VF1IN,PVF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJW,CHAML,
4 WIDTH,CPP,6L,FORCE,DSCPSI,BR,DYDT,A3,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(NDC,7),CG(NDC),EG(NDC),FV(NDC),TP(NDC),FY(NDC),UG(NDC),
6 UP(NDC),A(NDC),AB(NDC),V(NDC),V3(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PC(NDC),OP(NDC),OG(NDC),DF(NDC,7),G(NDC,7),G(NDC),Z(NDC),ZB(NDC)
8 ,TGA(NDC),GCA(NDC),DEA(NDC),VFA(NDC),FMA(NDC)
COMMON /NRKC/ NRK
COMMON /MC/ NZA,ZA(7),ZWC(7),IZW(7),ZW(7),IEX
IF (ZPROJ+4.0-BL) 1,1,5
1 KSW=1
ZP=CHAML+2.54*(ZPROJ+4.0+XC(7))
CALL IOFZ (ZP,IPRJ)
IMX=IPRJ
NRK=5+7*IPRJ
IF (IPRJ-IPO)18,6,2
2 CONTINUE
DDC=ZP-ZB(IPRJ-2)
VR=(ZP-ZB(IPRJ-1))/DCD
VRC=V(IPO)/(DDC*AS(IPC))
DO 3 K=1,5
F(IPRJ,K)=VR*F(IPO,K)
3 F(IPJ,K)=VRC*F(IPJ,K)
UG(IPC)=UG(IPJ-1)*(VPROJ*30,43-UG(IPJ-1))*(ZB(IPO)-ZB(IPJ-1))/
2 (ZP-ZB(IPJ-1))
UF(IPO)=UP(IPJ-1)*(VPROJ*30,43-UP(IPJ-1))*(ZB(IPO)-ZB(IPJ-1))/
2 (ZP-ZB(IPJ-1))
F(IPJ,7)=UP(IPO)*F(IPJ,5)
F(IPJ,6)=F(IPJ,7)+UG(IPJ)*F(IPJ,1)
L=5
DO 4 I=1,IMW
DO 4 K=1,7
L=L+1
4 Y(L)=F(I,K)

```

CNTR0010
 CNTR0020
 CNTR0030
 CNTR0040
 CNTR0050
 CNTR0060
 CNTR0070
 CNTR0080
 CNTR0090
 CNTR0100
 CNTR0110
 CNTR0120
 CNTR0130
 CNTR0140
 CNTR0150
 CNTR0160
 CNTR0170
 CNTR0180
 CNTR0190
 CNTR0200
 CNTR0210
 CNTR0220
 CNTR0230
 CNTR0240
 CNTR0250
 CNTR0260
 CNTR0270
 CNTR0280
 CNTR0290
 CNTR0300
 CNTR0310
 CNTR0320
 CNTR0330
 CNTR0340
 CNTR0350
 CNTR0360
 CNTR0370
 CNTR0380
 CNTR0390

```

17 CONTINUE
18 CALL DERIV (Y,OY,T)
19 IPO=IPRJ
20 GO TO 6
21 KS=2
22 IM=IM-1
23 NRK=5+7*IM
24 IF (IM-IPO) 13,14,13
13 CONTINUE
25 F(IP0,7)=UP(IP0)+F(IP0,5)
26 F(IP0,6)=F(IP0,7)+UG(IP0)+CG(IP0)
27 IPO=IM
28 GO TO 14
14 CONTINUE
29 KK=KK+1
30 KK0=KK0+1
31 IF (KK0-KK) 8,7,7
32 NTRY=2
33 GO TO 9

```

```

CNTR0400
CNTR0410
CNTR0420
CNTR0430
CNTR0440
CNTR0450
CNTR0460
CNTR0470
CNTR0480
CNTR0490
CNTR0500
CNTR0510
CNTR0520
CNTR0530
CNTR0540
CNTR0550
CNTR0560
CNTR0570

```


ONE DIMENSIONAL GAS PARTICLE FLOW

```

8 NTRY=1
9 WRITE (6,101) KK,T,DT,IMW,ZP,Z (IMW)
101 FORMAT (1H,5X,34KK=,16,5X,2HT=,1PE12.5,5X,3HDT=,E12.5,5X,
2 4HIMW=,16,5X,3HZP=,E12.5,5X,7HZ(IMW)=,E12.5)
DO 16 I=1,NZ
11=12*(I)
12=11+1
ZZ=7*CC(I)
P1=PG(I1)+0.5*RHOG(I1)*(UG(I1)**2)
P2=PG(I2)+0.5*RHOG(I2)*(UG(I2)**2)
PSAVE=P1+(ZZ-Z(I1))*(P2-P1)/(Z(I2)-Z(I1))
PU(I)=PSAVE/DSCPSI
16 CONTINUE
WRITE (6,109) (I,PU(I),I=1,NZW)
109 FORMAT (1H,2X,5(34PW(I,2H)=,1PE12.5,4X,))
IF ((KK/5)*5-KK) 20,19,20
19 CONTINUE
WRITE (8) KK,T,(PW(I),I=1,NZW),PB,V=ROJ,ZPROJ,Y(4),Y(5)
WRITE (11) KK,T,PG(1EX),CG(1EX),JG(1EX),UP(1EX),FMV(1EX)
20 CONTINUE
IF ((KKQ/KK)*KW-KKQ) 11,10,11
10 IM*PI=IM*PI+1
IKK=5+7*IM
WRITE (9) KK,T,DT,IPRJ,IMW,KSW,(Y(I),I=1,IRK)
WRITE (13) KK,(PG(I),FMV(I),UG(I),UP(I),Z(I),ZB(I),I=1,IM)
IF ((KKQ/KP)*KP-KKQ) 15,12,15
11 CONTINUE
WRITE (6,102) KKQ,KK,T,DT,PB,DYDT,FORCE,Y(1),Y(4),Y(5),ZPROJ,VPROJ
102 FORMAT (1H,5X,44KKQ=,16,5X,34KK=,16,5X,2HT=,1PE12.5,5X,3HDT=,
3 E12.5,5X,3HPC=,E12.5,5X,3HDYDT=,E12.5, / 1H,5X,6HFORCE=,E12.5,
4 5X,20HUNBURVED PROPELLANT=,E12.5,
5 E12.5,5X,6HIMPULSE=,E12.5,12HIMPULSE*SEC=,E12.5,5X,5HZPRJ=,
WRITE (6,103) (I,UG(I),UP(I),PG(I),G(I),PD(I),CG(I),VFA(I),
2 RHOG(I),I=1,IMWP1)
103 FORMAT (1H,7X,1H,4X,2HUG,12X,2HUP,12X,2HPC,12X,1HG,13X,2HPD,
2 12X,2HCG,12X,3HVF=,11X,4HRHOG / 1H,18,1PE14,6,7E14,6))
WRITE (6,104) (I,EG(I),TGA(I),TP(I),FN(I),OP(I),DG(I),GCA(I),
2 GEA(I),I=1,IMWP1)

```


ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE EXSTAT (E,RHO,P)
F1= 1.6663384E 05+RHO*( 2.3860914E 05+RHO* 1.8121513E 05)
F2= 8.804000E 01+RHO*( 2.099948E 02+RHO*-1.7081190E 01)
F3=-3.9913083E-02+RHO*(-6.3478293E-03+RHO*-1.0366801E-01)
P=RHO*(F1+E*(F2+E*F3))
RETURN
END

```

EGST00010
EGST00020
EGST00030
EGST00040
EGST00050
EGST00060
EGST00070

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE TOEAR (E,RHO,T)
F1=3.607725E3+RHO*(1.041906E3-RHO*1.501111E3)
F2=1.655822+RHO*(2.115013-RHO*1.948174)
F3=-0.107984E-2+RHO*(-0.686307E-3+RHO*0.422347E-2)
T=F1+E*(F2+E*F3)
RETURN
END

```

TOEAG0010
TOEAG0020
TOEAG0030
TOEAG0040
TOEAG0050
TOEAG0060
TOEAG0070

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE LOFU (U,L)
IF (U) 2,1,1
1 L=0
RETURN
2 L=1
RETURN
END

```

LOFU00010
LOFU00020
LOFU00030
LOFU00040
LOFU00050
LOFU00060
LOFU00070

ONE DIMENSIONAL GAS PARTICLE FLOW

```

C
C
C
C
C
C
SUBROUTINE RK2 (DERIV,CNTRL,Y,DY,A,R,T,DT,N,DTM)
SECOND ORDER RUNGE KUTTA
NTRY IS ASSIGNED ONE OF THE VALUES LISTED BELOW IN CNTRL
NTRY = 1 CONTINUE INTEGRATION
NTRY = 2 RETURN FROM RUNGE KUTTA
NTRY = 3 REPEAT STEP WITH NEW DT GIVEN IN CNTRL
NTRY = 4 CONTINUE INTEGRATION WITH FIXED STEP
PARAMETER NRKC=1800
DIMENSION Y(NRKC),DY(NRKC),A(NRKC),R(NRKC),YST(NRKC),DYST(NRKC)
COMMON / NRKC/ NRK
EXTERNAL DERIV,CNTRL
THR10=10,*(1.0/3.0)
GAM=3.5
BETA=0.5/GAM
ALPHA=1.0-BETA
CALL DERIV (Y,DY,T)
CALL CNTRL(Y,DY,DT,T,NTRY)
4 TST=1
N=NRK
DO 5 I=1,N
YST(I)=Y(I)
5 DYST(I)=DY(I)
6 IF (DT) 8,7,8
7 WRITE (6,101)
101 FORMAT (10,20X,17HSTEP SIZE = ZERO, )
RETURN
8 T=1T+GAM*DT
DO 9 I=1,N
9 Y(I)=YST(I)+GAM*DT*DYST(I)
CALL DERIV (Y,DY,T)
T=1T+DT
DO 10 I=1,N
10 Y(I)=YST(I)+DT*(ALPHA*DYST(I)+BETA*DY(I))
CALL DERIV (Y,DY,T)
EOCM=0.0
DO 13 I=1,N
13 E=Y(I)-(YST(I)+0.5*DT*(DYST(I)+DY(I)))
C=A(I)+R(I)*ABS(Y(I))
IF (C) 12,11,12

```

RK2 0010
 RK2 0020
 RK2 0030
 RK2 0040
 RK2 0050
 RK2 0060
 RK2 0070
 RK2 0080
 RK2 0090
 RK2 0100
 RK2 0110
 RK2 0120
 RK2 0130
 RK2 0140
 RK2 0150
 RK2 0160
 RK2 0170
 RK2 0180
 RK2 0190
 RK2 0200
 RK2 0210
 RK2 0220
 RK2 0230
 RK2 0240
 RK2 0250
 RK2 0260
 RK2 0270
 RK2 0280
 RK2 0290
 RK2 0300
 RK2 0310
 RK2 0320
 RK2 0330
 RK2 0340
 RK2 0350
 RK2 0360
 RK2 0370
 RK2 0380
 RK2 0390

```

11 WRITE (6,132) I
102 FORMAT (1H0, 20X, 27H(1)+R(1)+ABS(Y(1))=0 AT 1s , 16)
      RETURN
12 EOC=ABS(E/C)
   C EOCY=MAX1(EOC,EOCY)
      IF(EOC-EOCY) 13,13,201
201 EOCY=EOC
      LS=1
13 CONTINUE
   IS=(LS+1)/7
   KS=LS-5-7*(IS-1)
      IF (EOC-1.0) 17,17,14
14 CONTINUE
      WRITE (6,131) EOC,LS,KS,IS
331 FORMAT (1H ,10X,5-EOC=,1PE12,5,5X,3-LS=,16,5X,3HKS=,16,5X,
2 3-LS=,16)
      CALL DUMPE
   C T=TS
      T=TS

```

```

RK2 0400
RK2 0410
RK2 0420
RK2 0430
RK2 0440
RK2 0450
RK2 0460
RK2 0470
RK2 0480
RK2 0490
RK2 0500
RK2 0510
RK2 0520
RK2 0530
RK2 0540
RK2 0550
RK2 0560
RK2 0570

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

DO 15 I=1,N
Y(I)=YST(I)
15 CY(I)=CYST(I)
DO 16 J=1,10
EOCM=EOCM/10.0
DT=DT/THR10
IF (EOCM-1.0) 6,6,16
16 CONTINUE
GO TO 6
17 CALL CNTRL (Y,DY,DT,I,NTRY)
GO TO (21,18,19,4),NTRY
18 RETURN
19 T=TSI
DO 20 I=1,N
Y(I)=YST(I)
20 CY(I)=CYST(I)
GO TO 6
21 IF (EOCM-0.3) 23,23,22
22 DT=DT/THR10
WRITE (6,301) EOCM,LS,KS,IS
GO TO 4
23 IF (ECCM-C,03) 25,4,4
25 DT=DT/THR10
IF (ABS(DT)-ABS(DTM)) 4,4,24
24 DT=ABS(DTM)*DT/APS(DT)
GO TO 4
END

```

```

RK2 0580
RK2 0590
RK2 0600
RK2 0610
RK2 0620
RK2 0630
RK2 0640
RK2 0650
RK2 0660
RK2 0670
RK2 0680
RK2 0690
RK2 0700
RK2 0710
RK2 0720
RK2 0730
RK2 0740
RK2 0750
RK2 0760
RK2 0770
RK2 0780
RK2 0790
RK2 0800
RK2 0810
RK2 0820
RK2 0830
RK2 0840

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE CALXC(CNA1,CNA2,RV,DT,DEXC,BL,D,VCHAMB,ENL,XC,XBB)
DIMENSION XC(9)
XC(1)=-1.0E+37
XC(3)=-ENL
XC(4)=0.0
TCNA1=TAN(3.141593*CNA1/180.0)
SCNA1=TCNA1/SQRT(1.0+TCNA1**2)
CCNA1=COS(3.141593*CNA1/180.0)
IF (ENL-1.0E-10) 16,16,17
14 ANG=CNA1
GO TO 18
17 ANG=0.0
18 SANG=SIN(3.141593*ANG/180.0)
RC=24.0
RCC=RC*(SQRT(2.0)-1.0)/(SQRT(2.0)-SANG-SQRT(1.0-SANG**2))
XC(2)=-ENL+RCC*(SANG-1.0/SQRT(2.0))
RXC2=0.5*DEXC+RCC*(SQRT(1.0-SANG**2)-1.0/SQRT(2.0))
DI=0.25*4
XC(5)=0.5*(DEXC-DTH)/TCNA1
XC(6)=XC(5)+12.0
XBB=0.5*(XC(6)+XC(5))
XC(7)=XC(6)+0.5*(DI-DTH)/TCNA1
CWL=4.0*VCHAMB/(3.141593*DI*DI)
XC(8)=XC(7)+CWL*BL
XC(9)=1.0E37
X1=XC(1)
X2=XC(2)
K=1
4=100.0
RETURN
ENTRY RADIUS(XC,R)
X=XCH/2.54
IF (X-X1) 4,3,3
3 IF (X-X2) 7,7,4
4 DO 5 I=1,9
J=I
IF (XC(I)-X) 5,5,6
5 CONTINUE
6 K=J-1

```

CALX0400
CALX0410
CALX0420
CALX0430
CALX0440
CALX0450
CALX0460
CALX0470
CALX0480
CALX0490
CALX0500
CALX0510
CALX0520
CALX0530
CALX0540
CALX0550
CALX0560
CALX0570

CALXG580
CALXC590
CALX0600
CALX0610
CALX0620
CALX0630

```

X1=XC(J-1)
X2=XC(J)
7  CONTINUE
17 GO TO (19,8,9,10,11,12,13,14),4
17 R=XC2-X+XC(2)
GO TO 15
8 Z=X-XC(3)
R=CC*SQRT(1.3-5A*5**2)+0.5*DEXC-SQRT(WCC**2-(Z-RCC*SANG)**2)
GO TO 15
9 R=0.5*CEXC
GO TO 15
11 R=0.5*JEXC-X*TCNA1
GO TO 15
11 R=0.5*QTH
GO TO 15
12 R=0.5*CI+(X-XC(7))*TCNA1
GO TO 15
13 R=0.5*CI

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

GO TO 15
14 R=0.5*CI+SQRT ((X-XC(8))*2+A*A)-A
15 CONTINUE
R=R*2.54
RETURN
END

```


ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE ZSPACE
PARAMETER NCC=200
DIMENSION ZS(202)
COMMON /ALL/ IM,K,KP,KM,IPL1,IPL2,KST,KKT,IMW,KS,KK,KKO,
2 NFS,NFE,NPS,NPE,IPIJ,IPO,XB8,ZMAX,Z3,IR,VHL(NDC),VHR(NDC),
3 FL,RHOP,VISC,VFMIN,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJW,CHAML,
4 WIDTH,CPP,BL,FORCE,DSCPSI,GR,DYDT,A,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(NDC,7),CG(NDC),EG(NDC),FN(NDC),TP(NDC),FM(NDC),UG(NDC),
6 UF(NDC),A(NDC),AB(NDC),V(NDC),V3(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PE(NDC),DP(NDC),DG(NDC),DF(NDC,7),G(NDC,7),Q(NDC),Z(NDC),ZB(NDC),
8 TGA(NDC),GCA(NDC),GEA(NDC),VFA(NDC),FMV(NDC),
IM3=IM+1
ZMAXC=ZMAX*2.54
ZRC=ZR*2.54
CALL UNEGR (IM3,IM,K,KP,KM,IPL1,IPL2,KST,KKT,IMW,KS,KK,KKO,
J=IM3
I=0
DO 8 L=1,1000
J=J-1
IF (J) 2,1,2
1 J=-2
2 JA=IABS(J)
ZST=ZS(JA)
IF (J) 4,5,3
3 ZL=XB8*2.54-ZST
GO TO 5
4 ZL=XB8*2.54+ZST
5 IF ((L/2)*2-L) 6,7,6
6 I=I+1
Z(I)=ZL
GO TO 8
7 ZB(I)=ZL
IF (I-IM) 8,10,10
8 CONTINUE
10 CONTINUE
R2C=0.0
DO 9 I=1,IM
CALL RADIUS (Z(I),R)
CALL RADIUS (ZB(I),R2)

```

```

A(I)=3.141593*R*R
AR(I)=3.141593*R2*R2
IM1=MAXC(I-1,1)
VHR(I)=3.141593*(Z(I)-Z(IM1))*(R2+R2+R2+R2)/3.0
VHL(I)=3.141593*(Z(I)-Z(IM1))*(R2+R2+R2+R2)/3.0
R2J=R2
9 CONTINUE
VHL(1)=VHR(1)
VHR(14)=VHL(14)
VHL(14+1)=VHR(14)
DO 11 I=1,14
V(I)=VHL(I)+VHR(I)
V2(I)=VHR(I)+VHL(I+1)
11 RETURN
END

```

```

ZSPA0400
ZSPA0410
ZSPA0420
ZSPA0430
ZSPA0440
ZSPA0450
ZSPA0460
ZSPA0470
ZSPA0480
ZSPA0490
ZSPA0500
ZSPA0510
ZSPA0520
ZSPA0530
ZSPA0540

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE IOFZ(ZZ,II)
PARAMETER NDC=200
COMMON /ALL/ IM,K,,KP,KM,IPL1,IPL2,KST,KKST,IMW,KS,J,KK,KKD,
2 NPS,VFE,NPS,NPE,IPRJ,IPO,XBS,ZMAX,Z3,IR,VHL(NDC),VHR(NDC),
3 FL,RHCP,VISCG,VF1IN,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJX,CHAML,
4 WIDTH,CPP,BL,FORCE,DSCHSI,BR,DYDT,AP,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(NDC,7),CG(NDC),EG(NDC),FN(NDC),TP(NDC),FM(NDC),UG(NDC),
6 UP(NDC),A(NDC),AB(NDC),V(NDC),V3(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PT(NDC),DP(NDC),DG(NDC),DF(NDC,7),G(NDC,7),G(NDC),Z(NDC),ZH(NDC),
8 ,TGA(NDC),GC1(NDC),GEA(NDC),VFA(NDC),FMV(NDC)
DATA LLL / 1 /
GO TO (1,2),LLL
1 Z1=Z(1)
  Z2=Z(2)
  IO=1
  LLL=2
2 IF (ZZ-Z1) 5,3,3
3 IF (ZZ-Z2) 4,6,6
4 II=10
  RETURN
5 IS=1
  GO TO 7
6 IS=10
7 DO 8 I=IS,IM
  JS=I
  IF (ZZ-Z(II)) 10,9,3
8 CONTINUE
9 II=J
  GO TO 11
10 II=J-1
11 IO=II
  Z1=Z(IO)
  Z2=Z(IO+1)
  RETURN
  END

```

IOFZ0010
 IOFZ0020
 IOFZ0030
 IOFZ0040
 IOFZ0050
 IOFZ0060
 IOFZ0070
 IOFZ0080
 IOFZ0090
 IOFZ0100
 IOFZ0110
 IOFZ0120
 IOFZ0130
 IOFZ0140
 IOFZ0150
 IOFZ0160
 IOFZ0170
 IOFZ0180
 IOFZ0190
 IOFZ0200
 IOFZ0210
 IOFZ0220
 IOFZ0230
 IOFZ0240
 IOFZ0250
 IOFZ0260
 IOFZ0270
 IOFZ0280
 IOFZ0290
 IOFZ0300
 IOFZ0310
 IOFZ0320
 IOFZ0330
 IOFZ0340
 IOFZ0350

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE IOFZB(ZZ,II)
PARAMETER NDC=200
COMMON /ALL/ IM,K,KP,KM,IPL1,IPL2,KST,KKST,IMW,KSW,KK,KKQ,
2 NFS,NFE,NFS,NPE,IPRJ,IPQ,XBB,ZMAX,Z3,IR,VHL(NDC),VHR(NDC),
3 FL,RHGP,VISCG,VFIN,PDF,FJ,CMAX,PV1,PV2,PV3,CHARG,PROJW,CHAML,
4 WIDTH,CPP,EL,FORCE,DSCPSI,BR,DYDT,A,CCPCIN,AC,VPROJ,ZPROJ,PB,
5 F(NDC,7),CG(NDC),EG(NDC),FN(NDC),TP(NDC),FM(NDC),UG(NDC),
6 UF(NDC),A(NDC),AB(NDC),V(NDC),VE(NDC),XC(9),RHOG(NDC),PG(NDC),
7 PC(NDC),DP(NDC),CG(NDC),DF(NDC,7),G(NDC,7),G(NDC,7),G(NDC),ZB(NDC),
8 ,TGA(NDC),GC1(NDC),GEA(NDC),VFA(NDC),FMV(NDC)
DATA LLL / 1 /
GO TO (1,2),LLL
1 Z1=ZB(1)
Z2=ZB(2)
IO=1
LLL=2
2 IF (ZZ-Z1) 5,3,3
3 IF (ZZ-Z2) 4,6,6
4 II=10
RETURN
5 IS=1
GO TO 7
6 IS=10
7 DO 8 I=IS,IM
J=I
IF (ZZ-ZB(I)) 10,9,8
8 CONTINUE
9 II=J
GO TO 11
10 II=J-1
11 IO=II
Z1=ZB(IO)
Z2=ZB(IO+1)
RETURN
END

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE UNEQR(IM, RM, IR, RR, R)
  DIMENSION R(222)
  FIR=FLOAT(IR)
  FIM=FLOAT(IM)
  B=1.0
  DO 1 K=1,5
    EX=EXP(-B*(FIR-FIR-2.0))+(1.0-EX)*(-2.0*B*(FIR-1.0))*RM/RR
    B=ALOG(EX)/(FIR-FIR)
    WRITE (6,101) K,B,IM,IR,RR,R
101  FORMAT (10,3X,2H K=,15,3X,2H B=,1PE14,6,3X,3H IM=,15,3X,
2 3H IR=,15,3X,3H RM=,E14,6,3X,3H RR=,E14,6)
1  CONTINUE
  DO 2 K=6,25
    F1=RM*SINH(B*(FIR-1.0))
    F2=RR*SINH(B*(FIM-1.0))
    DO F1-F2
    C1=RM*(FIR-1.0)*COSH(B*(FIR-1.0))-RR*(FIM-1.0)*COSH(B*(FIM-1.0))
    C2=F1*(FIR-1.0)*2-F2*(FIM-1.0)*2
    D1=SGL(CLOG(1.000-DBLE(C0)*DBLE(D2)/DBLE(D1)**2)*DBLE(D1)/
2 DBLE(C2))
    B=B+DB
  WRITE (6,102) K,C1,C2
102  FORMAT (10,3X,2H K=,15,3X,3H C1=,1PE14,6,3X,2H C2=,E14,6)
  IF (ABS(DB)-1.0E-7)3,3.2
2  CONTINUE
3  A=RR/SINH(3*(FIR-1.0))
  DO 4 I=1,IM
    R(I)=A*SINH(B*FLOAT(I-1))
4  RETURN
  END

```

UNEQ00010
 UNEQ00020
 UNEQ00030
 UNEQ00040
 UNEQ00050
 UNEQ00060
 UNEQ00070
 UNEQ00080
 UNEQ00090
 UNEQ00100
 UNEQ00110
 UNEQ00120
 UNEQ00130
 UNEQ00140
 UNEQ00150
 UNEQ00160
 UNEQ00170
 UNEQ00180
 UNEQ00190
 UNEQ00200
 UNEQ00210
 UNEQ00220
 UNEQ00230
 UNEQ00240
 UNEQ00250
 UNEQ00260
 UNEQ00270
 UNEQ00280
 UNEQ00290
 UNEQ00300

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE PLOTS (X,Y1,Y2,Y3,M,I1,I2,ND,K1,K2,K3,XMIN,XMAX,
2 YMIN,YMAX)
PURPOSE - TO PLOT A GRAPH WITH ONE INDEPENDENT VARIABLE AND UP
TO 9 DEPENDENT VARIABLES. THE INDEPENDENT VARIABLE IS PLOTTED ON A
HORIZONTAL AXIS, THE DEPENDENT ONES ON A VERTICAL AXIS. WIDTH
IS 100 PRINT POSITIONS, HEIGHT IS 50.
PARAMETER USAGE.
N      NUMBER OF OBSERVATIONS
M      NUMBER OF VARIABLES (INDEPENDENT + DEPENDENT)
XMAX,XMIN,YMAX,YMIN MAXIMUM AND MINIMUM VALUES OF THE INDEPENDENT
AND DEPENDENT VARIABLES TO BE USED IN THE PLOT.
IF XMAX = XMIN, THE PROGRAM CALCULATES ITS OWN MAXIMUM AND MINIMUM
FOR THE INDEPENDENT VARIABLE. SIMILARLY FOR YMAX = YMIN
KPS PLOTTING SYMBOL ARRAY, KPS(L) SYMBOL FOR LTH VARIABLE. AA(I,L)
REQUIRED SUBROUTINES SCAL
DIMENSION X(N),Y1(ND),Y2(ND),Y3(ND),A(800),KPS(4)
DATA KPS/1H=1/
N=12-11+1
M=4+1
KPS(1)=K0
KPS(2)=K1
KPS(3)=K2
KPS(4)=K3
DO 1 I=1,N
J=I+11-1
L2=I+1
L3=I+2+N
L4=I+3+N
A(I)=X(J)
A(L2)=Y1(J)
A(L3)=Y2(J)
A(L4)=Y3(J)
XMAX=XMAX
XMIN=XMIN
YMAX=YMAX
YMIN=YMIN
EXTERNAL BLANK
RETURN

```

CCCCCCCCCCCCCCCC

CALL PLOT (G,A,N,V,UFUNC,BLANK,XLAX,XLIN,YLAX,YLIN,KPS)
RETURN
END

PLOT0400
PLOT0410
PLOT0420

ONE DIMENSIONAL GAS PARTICLE FLOW

SUBROUTINE BLANK (X,Y)
Y=0.0
RETURN
END

BLAN0010
BLAN0020
BLAN0030
BLAN0040

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE PLOT (NO,A,N,N,NFUNG,FUNC,XLAX,XLIN,VLAX,YLIN,KFS)
PURPOSE - TO PLOT A GRAPH WITH ONE INDEPENDENT VARIABLE AND UP
TO 9 DEPENDENT VARIABLES, WITH THE ADDITIONAL ABILITY TO PLOT A
CALCULATED CURVE. THE INDEPENDENT VARIABLE IS PLOTTED ON A
HORIZONTAL AXIS, THE DEPENDENT ONES ON A VERTICAL AXIS. WIDTH
IS 100 PRINT POSITIONS, HEIGHT IS 50, EVERY POINT OF EACH
DEPENDENT VARIABLE IS INDICATED BY A NUMBER (1-9), WHILE THE
CALCULATED POINTS ARE DENOTED BY ASTERISKS.
PARAMETER USAGE:
NC      A FIXED POINT NUMBER, UP TO 3 DIGITS, PRINTED AS THE
        CHART NUMBER
A      A VECTOR WHOSE FIRST N POSITIONS CONTAIN THE INDEPENDENT
        VARIABLE, AND WHOSE NEXT N SETS OF N POSITIONS CONTAIN
        THE DEPENDENT VARIABLES
N      NUMBER OF OBSERVATIONS
NFUNG  NUMBER OF VARIABLES (INDEPENDENT + DEPENDENT)
        NFUNG GREATER THAN ZERO IF A CALCULATED CURVE IS TO BE
        PRINTED
FUNC  SUBROUTINE TO GENERATE CALCULATED CURVE, IF ONE WANTED.
        ELSE IS A DUMMY. PROGRAM CALLING PLOT MUST HAVE AN
        'EXTERNAL FUNC', SUBROUTINE CALLED BY CALL FUNC (X,Y),
        WHERE X IS GIVEN TO SUBROUTINE AND Y RETURNED. THE
        XLAX,XLIN,VLAX,YLIN MAXIMUM AND MINIMUM VALUES OF THE
        INDEPENDENT AND DEPENDENT VARIABLES TO BE USED IN THE
        PLOT IF XLAX = XLIN, THE PROGRAM CALCULATES ITS OWN
        MAXIMUM AND MINIMUM FOR THE INDEPENDENT VARIABLE.
        SIMILARLY FOR VLAX = YLIN
REQUIRED SUBROUTINES, FUNC (IF USED), AND SCAL,
KFS(1)= PLOTTING SYMBOL FOR FUNCTION
KFS(2)= PLOTTING SYMBOL FOR DATA IN FIRST ARRAY,
KFS(3)= PLOTTING SYMBOL FOR DATA IN SECOND ARRAY ETC.
CALC IS 1 LARGER THAN NEEDED IN CASE XLIN + 100*XSCL
SHOULD BE LARGER THAN XMAX, THIS PREVENTS SLOPOVER INTO
NEXT LOCATION. LOOK AROUND CARD #950 TO SEE WHAT I MEAN,
CALC IS WHERE CALCULATED FUNCTION GOES.
DATA KFS/1H
EQUIVALENCE (IOUT(1),XPH(1))
1 FORMAT(1H1.6X,7H CHART ,13)
113 FORMAT (1H ,12X,2-- ,131A1.1H--)

```

CC

PLOT0400
PLOT0410
PLOT0420
PLOT0430
PLOT0440
PLOT0450
PLOT0460
PLOT0470
PLOT0480
PLOT0490
PLOT0500
PLOT0510
PLOT0520
PLOT0530
PLOT0540
PLOT0550
PLOT0560
PLOT0570

```

2  FORMAT (1H ,1PE12.3,2H+ ,101A1.1H+,E12.3)
7  FORMAT (1H ,14X,1E10H+,..... ,1H+)
8  FORMAT(1H,5X,1PE10.3,10E10,3)
9  PRINT CHART NO.
10 WRITE (6,1) NO
11 ICOUNT = 4
12 IF NO EXTREMES OF X GIVEN, FIND THEM
13 DIMENSION IOUT(101),XPR(11),A(500),CALC(102),KPS(4)
14 IF (XMAX - XMIN) 20,10,20
15 XMIN = A(1)
16 XMAX = XMIN
17 DO 15 J = 1,N
18 IF (A(J) - XMIN) 11,12,12
19 IF (A(J) - XMAX) 15,15,14
20 XMIN = A(J)
21 GO TO 15
22 XMAX = A(J)
23 CONTINUE

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

20  GO TO 202
    XMAX=XLAX
    XMIN=XLIN
    CALCULATE MAX SCALE SIZE
    200 XSCALE=(XMAX-XMIN)/100.
    XSCALE=MAX(XSCALE,1.0E-20)
    ROUTINE TO CALCULATE EXACT SCALE SIZE AND END POINTS
    CALL SCAL (XSCALE,XMAX,XMIN)
    IF NO EXTREMES OF Y GIVEN, FIND THEM
    IF (YLLX - YLIN) 110,112,110
    112 L = N + 1
    YMIN = ALL
    YMAX = YMIN
    LL = M+M
    DO 40 J = L,LL
    IF (A(J)-YMIN) 25,26,26
    24 IF (A(J)-YMAX) 40,40,30
    28 YMIN=A(J)
    30 YMAX=A(J)
    40 CONTINUE
    GO TO 201
    YMAX=VLAX
    YMIN=VLIN
    GET SCALE SIZE AND END POINTS
    201 YSCALE = (YMAX - YMIN) / 50.
    YSCALE=MAX(1,YSCALE,1.0E-20)
    CALL SCAL (YSCALE,YMAX,YMIN)
    PRINT TOP SCALE
    XPR(1) = YMIN
    DO 200 JP=1,10
    XPR(JP+1) = XPR(JP) + XSCALE * 10,
    TO MAKE SURE THAT ZERO REALLY PRINTS AS ZERO, NOT A SMALL NUMBER
    CAUSED BY ROUNDING ERRORS.
    IF (ABS(XPR(JP+1) - .5 * XSCALE)) 240,240,200
    240 XPR(JP+1) = 0.
    200 CONTINUE
    WRITE (6,6) (XPR(JP),JP=1,11)
    WRITE (6,7)

```

PLOT0580
 PLOT0590
 PLOT0600
 PLOT0610
 PLOT0620
 PLOT0630
 PLOT0640
 PLOT0650
 PLOT0660
 PLOT0670
 PLOT0680
 PLOT0690
 PLOT0700
 PLOT0710
 PLOT0720
 PLOT0730
 PLOT0740
 PLOT0750
 PLOT0760
 PLOT0770
 PLOT0780
 PLOT0790
 PLOT0800
 PLOT0810
 PLOT0820
 PLOT0830
 PLOT0840
 PLOT0850
 PLOT0860
 PLOT0870
 PLOT0880
 PLOT0890
 PLOT0900
 PLOT0910
 PLOT0920
 PLOT0930
 PLOT0940
 PLOT0950
 PLOT0960

PLOT10970
PLOT10980
PLOT10990
PLOT11000
PLOT11010
PLOT11020
PLOT11030
PLOT11040
PLOT11050
PLOT11060
PLOT11070
PLOT11080
PLOT11090
PLOT11100
PLOT11110
PLOT11120
PLOT11130
PLOT11140

```

C      IF CALCULATED CURVE WANTED GET VALUES BETWEEN XMIN AND XMAX
      IF (NFUNC) 213,214,215
      IF F = XMIN
      IF F = 1
      213 CALL FUNC(F,C,LC(UP))
      IF (F = XMAX) 212,213,215
      212 F = F + 1
      IF F = JB + 1
      GO TO 213
      210 CONTINUE
      PRINT PRINT AT MAXIMUM Y
      YPR = YMIN
      CLEAR PRINT LINE
      210 GO 55 UP = 1.101
      IF (OUT(UP) = 0)
      IF CALCULATED CURVE WANTED SET UP POINTS
      IF (NFUNC) 214,215,216
      IF F = XMIN

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

C      SCAN ALL VALUES OF Y FOR X BETWEEN XMIN AND XMAX
      JP = 1
      IS POINT WITHIN HALF A SCALE OF PRINT POSITION
      220 IF (ABS(YPR-CALC(JP)) - .5 * YSCAL) 216,217,218
      C      IF EXACTLY BETWEEN PRINT POSITIONS ONLY PRINT IT ONCE
      217 IF (YPR - CALC(JP)) 218,216,216
      C      BELIEVE IT OR NOT THIS IS AN ASTERISK (NUMBER TOO LARGE TO WRITE
      C      AS ONE NUMBER)
      216 IOUT(JP) = KPS(1)
      215 IF (F - XMAX) 219,214,214
      214 JP = JP + 1
      F = F + XSCAL
      GO TO 220
      RUN DOWN EACH SET OF DEPENDENT VARIABLES
      IF NO POINTS WANTED
      214 IF (N) 70,70,300
      300 DO 221 J = 2,N
      DO 222 L = 1,N
      C      CALCULATE SUBSCRIPT FOR A
      LL = (J - 1) * N + L
      IS IT WITHIN HALF A SCALE OF PRINT POSITION
      IF (ABS(YPR - A(LL)) - .5 * YSCAL) 223,224,225
      C      IF EXACTLY HALFWAY BETWEEN, PRINT ONLY ONCE
      224 IF (YPR - A(LL)) 225,223,223
      C      FIND HORIZONTAL POSITION
      223 FJF = (A(LL) - X*1.) / XSCAL + 1.5
      JP=IF1X(FJP)
      IF OFF GRAPH, FORGET IT
      IF (JP - 1) 225,226,226
      226 IF (JP - 101) 227,227,225
      C      THIS GIVES 1,2,3 ETC. FOR J=2,3,4 ETC
      227 IOUT(JP) = KPS(J)
      225 CONTINUE
      222 CONTINUE
      221 CONTINUE
      70 ICOUNT = ICOUNT + 1
      C      PRINT VALUE ON VERTICAL AXIS EVERY FIVE POSITIONS
      IF (ICOUNT - 5) 120,119,120
      120 WRITE (6,118) (IOUT(JP),JP=1,101)

```

PLOT1150
 PLOT1160
 PLOT1170
 PLOT1180
 PLOT1190
 PLOT1200
 PLOT1210
 PLOT1220
 PLOT1230
 PLOT1240
 PLOT1250
 PLOT1260
 PLOT1270
 PLOT1280
 PLOT1290
 PLOT1300
 PLOT1310
 PLOT1320
 PLOT1330
 PLOT1340
 PLOT1350
 PLOT1360
 PLOT1370
 PLOT1380
 PLOT1390
 PLOT1400
 PLOT1410
 PLOT1420
 PLOT1430
 PLOT1440
 PLOT1450
 PLOT1460
 PLOT1470
 PLOT1480
 PLOT1490
 PLOT1500
 PLOT1510
 PLOT1520
 PLOT1530

```

C      GO TO 80
      MAKE ZERO PRINT AS ZERO, NOT SMALL NUMBER
      119 IF (ABS(YPR) - .5 * YSCAL) 232,232,233
      232 F = 0
      233 GO TO 234
      234 F = YPR
      235 WRITE (6,2) F, (IOUT(JP),JP=1,101),F
      ICOUNT = 0
      IF REACHED YMIN, STOP
      83 IF (YPR - YMIN) 86,86,45
      C      ELSE DECREMENT Y
      45 YPR = YPR - YSCAL
      GO TO 235
      85 WRITE (6,7)
      C      PRINT BOTTOM SCALE
      XPR(1) = XMIN
      DO 90 JP = 1,10
      XPR(JP+1) = XPR(JP) + XSCAL * 10.

```

```

PLOT1540
PLOT1550
PLOT1560
PLOT1570
PLOT1580
PLOT1590
PLOT1600
PLOT1610
PLOT1620
PLOT1630
PLOT1640
PLOT1650
PLOT1660
PLOT1670
PLOT1680
PLOT1690
PLOT1700
PLOT1710

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

      IF (ABS(XPR(JP+1) - .5 * XSCAL)) 231,231,90
      231 XPR(JP+1) = 0.
      90 CONTINUE
      WRITE (6,8) (XPR(JP),JP=1,11)
      RETURN
      END

```

```

PLOT1720
PLOT1730
PLOT1740
PLOT1750
PLOT1760
PLOT1770

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE SCAL (XSCAL,XMAX,XMIN)
PURPOSE. GIVEN R1A SCALE AND END POINTS, GET ROUNDED VALUES,
F=ALOG10(XSCAL*1.000001)
FIND NEXT LOWEST POWER OF 10.
IF (F) 1,2,2
IF NEGATIVE, STOP FORTHAN FROM ROUNDING UP
1 JP=-INT(-(F-1.0))
GO TO 20
2 JP=INT(F)
FIND VALUE JUST LARGER THAN 10JP YSCAL, OF FORM 1,2,2.5,2,OR 10
TIMES 10 TO AN INTEGRAL POWER
20 F=10.**JP
4 IF (F-XSCAL) 3,4,4
3 F=F+F
IF (F-XSCAL) 5,4,4
5 F=1.25*F
IF (F-XSCAL) 7,4,4
7 F=F+F
IF (F-XSCAL) 30,4,4
30 F=F+F
GO TO 6
SET EQUAL TO SCALE
4 XSCAL=F
IF (ABS(XMAX/XSCAL)-1.0E9) 8,11,11
8 JP=INT(XMAX/XSCAL)
TAKE END POINTS INTEGRAL MULTIPLES OF SCALE
12 F=XSCAL*FLOAT(JP)
IF (F-XMAX) 13,11,11
10 JP=JP+1
GO TO 12
11 XMAX=F
IF (ABS(XMIN/XSCAL)-1.0E9) 9,14,14
9 JP=INT(XMIN/XSCAL)
13 F=XSCAL*FLOAT(JP)
IF (F-XMIN) 14,14,15
15 JP=JP-1
GO TO 13
XMIN=F
14 RETURN
END

```

SCAL0010
 SCAL0020
 SCAL0030
 SCAL0040
 SCAL0050
 SCAL0060
 SCAL0070
 SCAL0080
 SCAL0090
 SCAL0100
 SCAL0110
 SCAL0120
 SCAL0130
 SCAL0140
 SCAL0150
 SCAL0160
 SCAL0170
 SCAL0180
 SCAL0190
 SCAL0200
 SCAL0210
 SCAL0220
 SCAL0230
 SCAL0240
 SCAL0250
 SCAL0260
 SCAL0270
 SCAL0280
 SCAL0290
 SCAL0300
 SCAL0310
 SCAL0320
 SCAL0330
 SCAL0340
 SCAL0350
 SCAL0360
 SCAL0370
 SCAL0380
 SCAL0390
 SCAL0400

ONE DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE DUMPE
PARAMETER NDC=200
COMMON /ALL/ IN,K,KP,KY,IPL1,IPL2,KST,KKT,IM,KSW,KK,KKQ,
2 NPS,NFE,NFS,NPE,IPO,XBA,ZBA,IR,VHL(NDC),VHR(NDC),
3 EL,RHCP,VISCO,VEMIN,PDE,FU,CMA,FV1,FV2,FV3,CHARG,PROJ,CHAML,
4 WIST,CP,EL,FORCE,DSCPSI,BR,DYDT,AP,CCPCIV,AC,VPROJ,ZPROJ,PR,
5 F(NDC,7),GG(NDC),GG(NDC),FN(NDC),TP(NDC),FV(NDC),UG(NDC),
6 UP(NDC),Z(NDC),Z(NDC),V(NDC),V(NDC),XC(9),RHOG(NDC),PG(NDC),
7 P(NDC),PP(NDC),PP(NDC),DE(NDC,7),G(NDC,7),G(NDC),Z(NDC),Z(NDC),
8 ,VSA(NDC),Z(NDC),Z(NDC),VFA(NDC),FNV(NDC)
IMWP1=IMW+1
WRITE(6,171)
100 FORMAT(140,7// 2IX,10HPROM DUMPE )
WRITE(6,172) (I, 6(1),6P(1),23(1),23(1),6G(1),VFA(1),
2 RHOG(1),131,IMWP1)
101 FORMAT(140,7X,IM, 4X,24UG,12X,24UP,12X,24PS,12X,14G,13X,24PD,
2 12X,24MS,12X,34V, 11X,4444G5 / (1M, 18,1PE14,4,7E14.6))
WRITE(6,174) (1,E14(1),15A(1),1P(1),FN(1),6P(1),6G(1),6CA(1),
2 24E(1),131,IMWP1)
104 FORMAT(140,7X,IM, 4X,24EG,12X,34TSA,11X,24HP,12X,24FN,12X,24DP,
2 12X,24MS,12X,34V, 11X,343E1 / (1M, 18,1PE14,6,7E14.6))
WRITE(6,105) (1,M(1),FNV(1),131,IMWP1)
105 FORMAT(140,7X,IM, 4X,24EF,12X,34FMV / (1M, 18,1PE14,6,E14.6))
WRITE(6,106) (K,K=1,7),(1,6 F(1,K),K=1,7),131,IMWP1)
106 FORMAT(140,7X,IM, 4X,34 F(1, 11,14) , 6(7X,54 F(1, 11,14) ) /
2 (1M, 18,1PE14,6,6E14.6))
WRITE(6,107) (K,K=1,7),(1,6 G(1,K),K=1,7),131,IMWP1)
107 FORMAT(140,7X,IM, 4X,34G F(1, 11,14) , 6(7X,54G F(1, 11,14) ) /
2 (1M, 18,1PE14,6,6E14.6))
WRITE(6,108) (K,K=1,7),(1,6 G(1,K),K=1,7),131,IMWP1)
108 FORMAT(140,7X,IM, 4X,34 G(1, 11,14) , 6(7X,54 G(1, 11,14) ) /
2 (1M, 18,1PE14,6,6E14.6))
RETURN
END

```

DUMP0010
 DUMP0020
 DUMP0030
 DUMP0040
 DUMP0050
 DUMP0060
 DUMP0070
 DUMP0080
 DUMP0090
 DUMP0100
 DUMP0110
 DUMP0120
 DUMP0130
 DUMP0140
 DUMP0150
 DUMP0160
 DUMP0170
 DUMP0180
 DUMP0190
 DUMP0200
 DUMP0210
 DUMP0220
 DUMP0230
 DUMP0240
 DUMP0250
 DUMP0260
 DUMP0270
 DUMP0280
 DUMP0290
 DUMP0300
 DUMP0310
 DUMP0320
 DUMP0330
 DUMP0340

POW 0400
 POW 0410
 POW 0420
 POW 0430
 POW 0440
 POW 0450
 POW 0460
 POW 0470
 POW 0480
 POW 0490
 POW 0500

GO TO 15
 10 X2=X*X
 X4=X2*X2
 X8=X4*X4
 XP=X3*X2
 15 GO TO (16,17),KS
 16 PC=X1.0/XP
 RETURN
 17 PO=X*XP
 RETURN
 END

ONE DIMENSIONAL GAS PARTICLE FLOW

```

FUNCTION ROOT (X,K)
ROOT=KTH ROOT OF X
K MUST SATISFY ,GE. 0 ,AND, .LE. 10
DATA L / 1 / , F / 0.9 /
DIMENSION A(13),C(11,10)
GO TO (1,5),L
1 DO 4 M=1,10
  FY=FLOAT(M)
  A( )=(0.75)**(1./FY)
  C(1,M)=1./C
  DO 3 J=1,10
    FJ=FLOAT(J)
    C(J+1,M)=2./C*(FJ/F)
  3 CONTINUE
  L=L+2
  5 IF (K) 6,7,8
  6 ROOT=0.0
  7 ROOT=1.0
  8 IF (K-1) 11,9,10
  9 ROOT=X
  10 IF (X) 11,11,12
  11 ROOT=0.0
  12 RETURN
  13 V1=FLD(C,9,X)
  14 J=FLD(9,27,X)
  15 FLD(9,27,F)=J
  16 E=F-0.75
  17 U=E*4./3./0
  18 FK=FLCAT(K)
  19 S=A(K)*(2./J*FK+(FK+1./J)*U)/(2./J*FK+(FK-1./J)*U)
  20 N=N+1-129
  21 N=(N+100*K)/K-100
  22 NRES=N-K*M
  23 FLD(C,9,S)=N+128
  24 Y=C(NR+1,K)*S
  25 IF (K-10) 14,14,15

```

C C

ROOT0010
 ROOT0020
 ROOT0030
 ROOT0040
 ROOT0050
 ROOT0060
 ROOT0070
 ROOT0080
 ROOT0090
 ROOT0100
 ROOT0110
 ROOT0120
 ROOT0130
 ROOT0140
 ROOT0150
 ROOT0160
 ROOT0170
 ROOT0180
 ROOT0190
 ROOT0200
 ROOT0210
 ROOT0220
 ROOT0230
 ROOT0240
 ROOT0250
 ROOT0260
 ROOT0270
 ROOT0280
 ROOT0290
 ROOT0300
 ROOT0310
 ROOT0320
 ROOT0330
 ROOT0340
 ROOT0350
 ROOT0360
 ROOT0370
 ROOT0380
 ROOT0390

```

15 ROOT=0.0
   RETURN
14 Y5=Y
   DO 33 LL=1,10
   GO TO (21,22,23,24,25,26,27,28,29,30),K
21 P=X
   GO TO 31
22 P=(Y*Y+X)/(2.0*Y)
   GO TO 31
23 Y2=Y*Y
   P=(2.0*Y2*Y+X)/(3.0*Y2)
   GO TO 31
24 Y2=Y*Y
   Y4=Y2*Y2
   P=(3.0*Y4+X)/(4.0*Y2*Y)
   GO TO 31
25 Y2=Y*Y
   Y4=Y2*Y2

```

```

ROOT0430
ROOT0410
ROOT0420
ROOT0430
ROOT0440
ROOT0450
ROOT0460
ROOT0470
ROOT0480
ROOT0490
ROOT0500
ROOT0510
ROOT0520
ROOT0530
ROOT0540
ROOT0550
ROOT0560
ROOT0570

```

ONE DIMENSIONAL GAS PARTICLE FLOW

```

P=(4.0*Y4*Y+X)/(5.0*Y4)
GO TO 31
26 Y2=Y*Y
Y4=Y2*Y2
P=(5.0*Y4*Y2+X)/(6.0*Y4*Y)
GO TO 31
27 Y2=Y*Y
Y4=Y2*Y2
Y6=Y4*Y2
P=(6.0*Y6*Y+X)/(7.0*Y4)
GO TO 31
28 Y2=Y*Y
Y4=Y2*Y2
P=(7.0*Y4*Y4+X)/(5.0*Y4*Y2*Y)
GO TO 31
29 Y2=Y*Y
Y4=Y2*Y2
Y8=Y4*Y4
P=(8.0*Y6*Y+X)/(9.0*Y8)
GO TO 31
30 Y2=Y*Y
Y4=Y2*Y2
Y8=Y4*Y4
P=(9.0*Y8*Y2+X)/(10.0*Y8*Y)
31 IF (ABS(1.0-Y/P)-1.0E-5)34,34,32
32 Y=P
33 CONTINUE
34 ROOT=P
RETURN
END
ROOT0580
ROOT0590
ROOT0600
ROOT0610
ROOT0620
ROOT0630
ROOT0640
ROOT0650
ROOT0660
ROOT0670
ROOT0680
ROOT0690
ROOT0700
ROOT0710
ROOT0720
ROOT0730
ROOT0740
ROOT0750
ROOT0760
ROOT0770
ROOT0780
ROOT0790
ROOT0800
ROOT0810
ROOT0820
ROOT0830
ROOT0840
ROOT0850
ROOT0860
ROOT0870

```

APPENDIX B
TWO-DIMENSIONAL GAS PARTICLE FLOW

```

C MAIN PROGRAM FOR 2-PHASE/2-D AXIAL SYMMETRY FLOW MODEL - NOZZLE BLAST
PARAMETER ID=25, JD=15, LD=400, NRKC=2625
DIMENSION Y(NRKC), AE(NRKC), RE(NRKC), REF(7), AEF(7), FMV(LD)
DIMENSION ZP(LD)
COMMON/VC/VJW(L,N), JW(8), PW(R)
COMMON/ALL/F(ID,J,D), DF(ID,J,D,7), IS, IA, IB, IM, JA, JB, JM, IT,
1EJ, VCLP, W, AEF, VFLMAX, PA, VFLRG, KW, KK, KKO, KM, PIN, IRK, RHOP,
2 T(LC), P(V,LC), CIND(LD), WINDG(LD), NIND(LD),
3Z(ID), ZZ(ID), DELZ(ID), DELZZ(ID), R(J,D), RR(JD), DELR(JD), DELRR(JD),
4AZ(J), AZD(JD), AR(ID,J,D), ARN(ID,J,D), ARD(ID,J,D), V(ID,J,D), VZ(ID,J,D),
5VR(ID,J,D), C(ID,J,D), CZ(ID,J,D), CR(ID,J,D), CD(ID,J,D), WC(ID,J,D),
6WGR(ID,J,D), WGD(ID,J,D), UG(ID,J,D), UGN(ID,J,D), UGD(ID,J,D), WP(ID,J,D),
7WPR(ID,J,D), WPD(ID,J,D), UFZ(ID,J,D), N(ID,J,D), NZ(ID,J,D), NR(ID,J,D),
8E(ID,J,D), E1(ID,J,D), P(ID,J,D), OR(ID,J,D), PO(ID,J,D), DR(ID,J,D),
9NZ(ID,J,D), LWR(ID,J,D), KUP(ID,J,D), LWG(ID,J,D), KUG(ID,J,D), GZ(ID,J,D)
A, NINDP(LD)
REAL N, VIND, V, R, NZ
1000 READ (5,1002) II, IP, JM, KW, KM, KST, KKST, KMID
1002 FORMAT (5,1004) RG, PATH, DATH, FJ, RHOP, DIAP, VFLMAX, PA, V, FL, ER
1004 FORMAT (F10.5/2=10.5)
C PRELIMINARY CALCULATIONS
PRELVP = 5238*(DIAP**3)
VN = VOLP*H3P
APF = .172*(DIAP**2)
AEF(1)=RG*VFLMAX/VOLP
AEF(2)=ER*1.0E5
AEF(3)=AEF(2)
AEF(4)=ER*1.002
AEF(5)=AEF(4)*1.0E5
AEF(6)=AEF(5)
AEF(7)=ER*0.002*200.0
DO 36 I=1,7
36 REF(I)=ER
REWIND 8
REWIND 9
REWIND 11
DO 37 LUL=2,LD
37 LUL=LL

```

```

      READ (11) K1, T1(LLL), PIND(LLL), CIND(LLL), WINDG(LLL), WINDP(LLL);
      2 FMV(LLL)
      IF (K1-410) 37,38,38
      37 CONTINUE
      38 CONTINUE
      REWIND 11
      DO 39 LLL=2,LS
        WINDG(LLL)=WINDG(LLL)
        WINDP(LLL)=WINDP(LLL)
        39 NIND(LLL)=FMV(LLL)*RNDP*3.141593*0.25*0.1A*0.033
        T1(1) = 0.
        PIND(1)=PATM
        CIND(1) = 2ATM
        WINDG(1) = 0.
        WINDP(1) = 0.
        NIND(1) = 0.
      READ (5,1030) NIJW,(IW(1),I1,1.A),(JW(1),I1,1.A)
      1030 FORMAT (11C/5110/6110)

```

```

MAIN0400
MAIN0410
MAIN0420
MAIN0430
MAIN0440
MAIN0450
MAIN0460
MAIN0470
MAIN0480
MAIN0490
MAIN0500
MAIN0510
MAIN0520
MAIN0530
MAIN0540
MAIN0550
MAIN0560
MAIN0570

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

KK = -1
KKO = -1
IM = II + IP - 1
IT = II + 2
IS = II + 1
IA = IM - 2
IB = IM - 1
JA = JM - 2
JB = JM - 1
READ (5,11,2) RMAX,ZMAX,ZREF
1102 FORMAT (3E10.5)
WRITE (6,2,01) BYAX,ZMAX,ZREF
2001 FORMAT (2H,5X,5HRMAX,1PE14,5,5X,5HZREF,5E14,5)
CALL U-ERR (JM,RVAX,2,2,0,0,RR,J0)
IMPI = MAXO(1,IP)
CALL UNEQR (IMPI,ZMAX,2,ZREF,ZPN,JD)
DO 10 I = 1, I1
  Z(I) = ZPN(I1) - ZPN(I1 + 1)
DO 12 I = 1, IS, IM
  Z(I) = ZPN(I1) + ZPN(I1 + 1)
DO 14 J = 1, JB
  R(J+1) = 0.5 * (R(J) + R(J+1))
  R(I) = R(2)
DO 16 I = 1, I1 + 1 + Z(I)
  Z(I) = 1.5 * (Z(I) + 1) + Z(I)
DO 18 I = 1, I1 + 1
  DELZ(I) = Z(I) - Z(I - 1)
DO 20 DELZ(I) = Z(I) - Z(I - 1)
DO 22 DELZ(I) = Z(I) - R(J - 1)
DO 24 J = 1, JB
  DELZ(I) = R(J) - R(J - 1)
  DELZ(I) = 3.142 * (R(J) - R(J - 1)) * 2
  AZ(I) = 3.142 * (R(J) - R(J - 1)) * 2
DO 26 J = 1, JB
  DO 28 J = 1, JB
  AR(I) = 5.28 * R(J) * DELZ(I)
  AR(I) = 0.203 * R(J) * DELZ(I + 1)

```

MAIN0580
 MAIN0590
 MAIN0600
 MAIN0610
 MAIN0620
 MAIN0630
 MAIN0640
 MAIN0650
 MAIN0660
 MAIN0670
 MAIN0680
 MAIN0690
 MAIN0700
 MAIN0710
 MAIN0720
 MAIN0730
 MAIN0740
 MAIN0750
 MAIN0760
 MAIN0770
 MAIN0780
 MAIN0790
 MAIN0800
 MAIN0810
 MAIN0820
 MAIN0830
 MAIN0840
 MAIN0850
 MAIN0860
 MAIN0870
 MAIN0880
 MAIN0890
 MAIN0900
 MAIN0910
 MAIN0920
 MAIN0930
 MAIN0940
 MAIN0950
 MAIN0960

```

26 AR(I,J) = 0.2*3*R(J)*DELZ(I)
DO 28 J=2,14
  DO 28 J=2,14
    V(I,J) = A/(J)*DELZ(I)
  VZ(I,J) = A/(J)*DELZ(I+1)
  VR(I,J) = A/(J)*DELZ(I)
  WRITE (6,202) I,IM,JM,K,KM,ST,KKST
2002 FORMAT (2I,26X15,NOZZLE BLAST EFFECTS WITH PARTICULATE EJECTION//
13X37,42-P435E/2-3 AXIAL SYMMETRY FLOW MODEL//
245X44) 3.16/45X44JM 3.16/45X44KM 3.16/45X44KKM 3.16/
3 45X44KKST 3.16/ 45X44KKST 3.16 // 1X)
  WRITE (6,2104) RS,DATM,DATY,FJ,RHOP,CIAP,VFLMAX,PAV,FL,ER
2104 FORMAT (14I,
19X33,NOZZLE RADIUS,RS
22X33,ATMOSPHERIC PRESSURE,PAV
32X33,ATMOSPHERIC DENSITY,DATM
42X33,MECHANICAL HEAT EQUIV.,FJ
52X33,PARTICULATE DENSITY,RHOP
MAIN0970
MAIN0980
MAIN0990
MAIN1000
MAIN1010
MAIN1020
MAIN1030
MAIN1040
MAIN1050
MAIN1060
MAIN1070
MAIN1080
MAIN1090
MAIN1100
MAIN1110
MAIN1120
MAIN1130
MAIN1140

```


TWO DIMENSIONAL GAS PARTICLE FLOW

```

620X30MPARTICLE DIAMETER,DIAP      ,E10.4,2X12H(CM)
720X30MAYX, ALLOWABLE VFL,VFLMAX    ,E10.4,
820X30MPARTICLE PRESSURE FACTOR,PAV ,E10.4,2X12H(DY/SQ-CM)
920X30MPARTIFICIAL VISC. FACTOR,FL  ,E10.4,
A 20X.30HERFOR LIMIT. ER          ,E10.4, ///1X)
      WRITE (6,2J36)
2006 FORMAT (1H,3X10H-3, TYPE,M,4X28HRELATIVE ERROR FACTOR,REF(M),10X2
18HABSOLUTE ERROR FACTOR,AEF(M)///1X)
      DO 2008 J=1,7
2008 WRITE (6,2J10) M,REF(M),AEF(M)
2010 FORMAT (18,F22.2,E4.2)
      WRITE (6,2J30) (1,IN(I),JW(I),I=1,N1JW)
2030 FORMAT (1H,19X,1H,18X,2H1W,8X,2HJW) (1H,10X,3J10)
      WRITE (6,2J12)
2012 FORMAT (1H,1,27X25-RADIAL POSITION DATA (CM)///3X31HNODE NUMBER,J
10DE RADIAL POS(J),6X5HRR(J),5X,HDELRR(J)///1X)
      DO 2014 J=1,JM
2014 WRITE (6,2J16) J,RR(J),DELRR(J),AZ(J),AZD(J)
2016 FORMAT (11,F18.1,F17.2,F13.2,F13.6)
      WRITE (6,2J18)
2018 FORMAT (1H,1,27X24-AXIAL POSITION DATA (CM)///3X31HNODE NUMBER,I
10E POSITION DATA (CM),5X5HZZ(I),5X,HDELZZ(I)///1X)
      DO 2020 I=1,IM
2020 WRITE (6,2J22) I,ZZ(I),DELZZ(I),DELZZ(I)
2022 FORMAT (11,F18.1,F18.2,F13.2,F13.2)
      WRITE (6,2J24)
2024 FORMAT (1H,1,30X17HNOZZLE INPUT DATA,5X1H,8X5,7I(M),13X7HUP,ND(M),
11X7HIND(M),11X8HWINDG(M),10X,8HWINDP(M),10X,4HIND(M)///1X)
      DO 2026 J=1,LS
2026 WRITE (6,2J28) M,TI(M),PINQ(M),CIND(M),WINDG(M),WINDP(M),NIND(M)
2028 FORMAT (1H,15,1P18.5,E18.5)
C INITIALIZE PHYSICAL VARIABLES AND F(I,J,M) = COMPUTE ERROR LIMITS FORM
DO 50 J=2,JA
DO 50 J=2,JA
IF (J.EQ.2.AND. I.LT.15) GO TO 50
N(I,J) = 0.
UP(I,J) = 0.
WP(I,J) = 0.
C(I,J) = DATM

```

/MAIN1150
 /MAIN1160
 /MAIN1170
 /MAIN1180
 /MAIN1190
 /MAIN1200
 /MAIN1210
 /MAIN1220
 /MAIN1230
 /MAIN1240
 /MAIN1250
 /MAIN1260
 /MAIN1270
 /MAIN1280
 /MAIN1290
 /MAIN1300
 /MAIN1310
 /MAIN1320
 /MAIN1330
 /MAIN1340
 /MAIN1350
 /MAIN1360
 /MAIN1370
 /MAIN1380
 /MAIN1390
 /MAIN1400
 /MAIN1410
 /MAIN1420
 /MAIN1430
 /MAIN1440
 /MAIN1450
 /MAIN1460
 /MAIN1470
 /MAIN1480
 /MAIN1490
 /MAIN1500
 /MAIN1510
 /MAIN1520
 /MAIN1530

MAIN1540
 MAIN1550
 MAIN1560
 MAIN1570
 MAIN1580
 MAIN1590
 MAIN1600
 MAIN1610
 MAIN1620
 MAIN1630
 MAIN1640
 MAIN1650
 MAIN1660
 MAIN1670
 MAIN1680
 MAIN1690
 MAIN1700
 MAIN1710

```

    UG(I,J) = 2.
    HG(I,J) = 0.
    E(I,J) = 2.5*PATY/FJ
    F(I,J,1) = N(I,J)
    F(I,J,2) = DP(I,J)
    F(I,J,3) = HP(I,J)
    F(I,J,4) = C(I,J)
    F(I,J,5) = 3.
    F(I,J,6) = 0.
    F(I,J,7) = E(I,J)
    SO CONTINUE Y(-)
    C INITIALIZE Y(-)
    L = 0
    DO 60 I=2,IA
    DO 60 J=2,JA
    IF (J.EQ.2.AND. I.LT. IS) GO TO 60
    DO 62 M=1,7
    L = L+1
  
```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

RE(L) = REE(M)
AE(L) = REE(M)*AEF(M)
62 Y(L) = F(I,J,M)
60 CONTINUE
IRK = L
Y = 0.
DT = .0001
EXTERNAL DERIV,CNTRL
REWIND 6
REWIND 9
REWIND 10
IF (KST-2) 34,30,34
30 DO 31 16=1,10000
   READ 16 (Y,K,T,D,T,(Y(I),I=1,IRK)
   READ 10 (I) 41
   IF (KK*KKSI) 31,32,32
31 CONTINUE
32 CONTINUE
DO 41 LL=1,10000
   READ 18 (R) K41
   IF (KK41*KK41) 41,42,42
41 CONTINUE
42 CONTINUE
KK=KK+1
34 CONTINUE
CALL RK2 (JERIV,CNTRL,Y,D,Y,AE,RE,T,D,T,IRK,2.0E6)
REWIND 8
REWIND 9
REWIND 10
STOP
END

```

MAIN1720
 MAIN1730
 MAIN1740
 MAIN1750
 MAIN1760
 MAIN1770
 MAIN1780
 MAIN1790
 MAIN1800
 MAIN1810
 MAIN1820
 MAIN1830
 MAIN1840
 MAIN1850
 MAIN1860
 MAIN1870
 MAIN1880
 MAIN1890
 MAIN1900
 MAIN1910
 MAIN1920
 MAIN1930
 MAIN1940
 MAIN1950
 MAIN1960
 MAIN1970
 MAIN1980
 MAIN1990
 MAIN2000
 MAIN2010
 MAIN2020

TWO DIMENSIONAL GAS PARTICLE FLOW

SUBROUTINE DERIV(Y,DY,T)
CELL AND DEFINITION OF ASSOCIATED VARIABLES

(I,J+1)*

F(I,J,2)
F(I,J,5)
GR(I,J,4)
GR(I,J,7)
U

DR(I,J)

C,N,E,P
F(I,J,1)
F(I,J,4)
F(I,J,7)
GZ(I,J,3)
GZ(I,J,6)
GR(I,J,2)
GR(I,J,5)

(I,J) *

F(I,J,3)
F(I,J,6)
GZ(I,J,1)
GZ(I,J,4)
GZ(I,J,7)
DZ(I,J)

(I+1,J)

BARREL AND DISTRIBUTION OF NOSES

DERI0010
DERI0020
DERI0030
DERI0040
DERI0050
DERI0060
DERI0070
DERI0080
DERI0090
DERI0100
DERI0110
DERI0120
DERI0130
DERI0140
DERI0150
DERI0160
DERI0170
DERI0180
DERI0190
DERI0200
DERI0210
DERI0220
DERI0230
DERI0240
DERI0250
DERI0260
DERI0270
DERI0280
DERI0290
DERI0300
DERI0310
DERI0320
DERI0330
DERI0340
DERI0350
DERI0360
DERI0370
DERI0380
DERI0390

A grid of 10x10 dots. A vertical dashed line is drawn between the 8th and 9th columns. The top row is labeled 'R' and the rightmost column is labeled 'IBL'.

[illegible]

DER10970
 DER10980
 DER10990
 DER11000
 DER11010
 DER11020
 DER11030
 DER11040
 DER11050
 DER11060
 DER11070
 DER11080
 DER11090
 DER11100
 DER11110
 DER11120
 DER11130
 DER11140

```

C  CONVERT F(I,J,M) FROM Y(L)
  L=0
  DO 1 I=2,1A
  DO 1 J=2,J4
  IF(J.EG.2.AND.I.LT.IS) GO TO 1
  DO 3 M=1,7
  L=L+1
  3 F(I,J,M)=Y(L)
  1 CONTINUE
C  CONVERT PHYSICAL VARIABLES FROM F(I,J,M) EXCEPT CR*UG AND CZ*WG
  DO 10 I=2,1A
  DO 10 J=2,JA
  IF(J.EG.2.AND.I.LT.IS) GO TO 15
  N(I,J)=F(I,J,1)
  UP(I,J)=F(I,J,2)
  WP(I,J)=F(I,J,3)
  C(I,J)=F(I,J,4)
  E(I,J)=F(I,J,7)
  15
  
```

TWO DIMENSIONAL GAS PARTICLE FLOW

DERI1150
DERI1160
DERI1170
DERI1180
DERI1190
DERI1200
DERI1210
DERI1220
DERI1230
DERI1240
DERI1250
DERI1260
DERI1270
DERI1280
DERI1290
DERI1300
DERI1310
DERI1320
DERI1330
DERI1340
DERI1350
DERI1360
DERI1370
DERI1380
DERI1390
DERI1400
DERI1410
DERI1420
DERI1430
DERI1440
DERI1450
DERI1460
DERI1470
DERI1480
DERI1490
DERI1500
DERI1510
DERI1520
DERI1530

```

10 CONTINUE
C BOUNDARY VALUES FOR C(I,J)
  DO 12 J=3,JA
    C(1B,2)=C(1A,2)
  C(1B,J)=C(1A,J)
  C(1,J)=C(2,J)
  DO 14 I=1,IB
    C(1,1)=C(1,2)
  C(1,I)=C(1,I+1)
  DO 16 J=1,JB
    C(1,J)=C(1,JA)
  DO 18 I=2,II
    C(1,2)=C(1,3)
  C EVALUATE C7 AND CR
  C CONVERT UG AND WC FROM F(I,J,M)
    DO 24 I=2,IA
      DO 24 J=2,JA
        IF(J.EQ.2)D=1,LT,IS) GO TO 24
        CZ(I,J)=.5*(C(I+1,J)+C(I,J))
        CR(I,J)=.5*(C(I,3)+C(I,J))
        UG(I,J)=F(I,J,6)/CZ(I,J)
        WC(I,J)=F(I,J,6)/CZ(I,J)
      24 CONTINUE
C SET BOUNDARY VALUES FOR PHYSICAL VARIABLES
    DO 30 J=3,JA
      E(1,J)=E(2,J)
      N(1,J)=N(2,J)
      UP(1,J)=UP(2,J)
      UG(1,J)=UG(2,J)
      WP(1,J)=WP(2,J)
      WC(1,J)=WC(2,J)
    DO 32 J=2,JA
      E(1B,J)=E(1A,J)
      N(1B,J)=N(1A,J)
      WP(1B,J)=WP(1A,J)
      WC(1B,J)=WC(1A,J)
      UP(1B,J)=UP(1A,J)
      UG(1B,J)=UG(1A,J)
    DO 34 I=1,IA
      E(1,JH)=E(1,JA)

```


DER11540
 DER11550
 DER11560
 DER11570
 DER11580
 DER11590
 DER11600
 DER11610
 DER11620
 DER11630
 DER11640
 DER11650
 DER11660
 DER11670
 DER11680
 DER11690
 DER11700
 DER11710

N(1,JB)=N(1,JA)
 UP(1,JB)=UP(1,JA)
 UG(1,JB)=UG(1,JA)
 WP(1,JB)=WP(1,JA)
 WG(1,JB)=WG(1,JA)
 DO 36 I=2,11
 E(1,2)=E(1,3)
 N(1,2)=N(1,3)
 WP(1,2)=WP(1,3)
 WG(1,2)=WG(1,3)
 UP(1,2)=0.
 UG(1,2)=0.
 DO 36 I=15,18
 E(1,1)=E(1,2)
 N(1,1)=N(1,2)
 WP(1,1)=WP(1,2)
 WG(1,1)=WG(1,2)
 UG(1,1)=0.

34

36

TWO DIMENSIONAL GAS PARTICLE FLOW

```

38 UP(1,1)=0.
C COMPUTE INPUT VALUES AT NOZZLE CELL
CALL NZLN=(YI,PIN,CIND,WINDG,WINDP,NIND,T,PIN,CIN,WING,WNP,
2 NIN,LD)
VFLN=VIN*VOLP
VFLN=AMIN1(VFLN,.9999)
VFLN=AMAX1(VFLN,.0)
EIN=PIN*(1.0-VFLN)/(0.4*FJ*CIN)
EIN=CIN*EIN+(WING**2)/(2.0*FJ)
EIN=CIN*EIN+VARIABLES FOR NOZZLE CELL
C COMPUTE C=(IS,2)/C(I,2)
E(I,2)=C(I,2)*2*WING**2+UG(I,2)**2)/FJ
2 -0.25*(UG(I,2)**2+WING**2+UG(I,2)**2)/FJ
VFLN(I,2)=VOLP
VFLN=AMIN1(VFLN,.9999)
VFLN=AMAX1(VFLN,.0)
PD(I,2)=0.
VFR(1.0-VFLN)/(1.0-VFLNMAX)
VFR=AMAX1(VFR,1.0E-10)
IF (VFLN*GE. VFLNMAX) PD(I,2)=PA*V(1.0/(VFR*VFR)+2.0*VFR-3.0)
D(I,2)=.4*FJ*(I,2)*C(I,2)/(1.0-VFLN)
RHOG=C(I,2)*(1.0-VFLN)
DELA=WING*UG(I,2)
DELW=AMAX1(DELW,0.0)
DELW=VFR*PD(I,2)
DELW=AMAX1(DELW,0.0)
DELW(I,2)=DELW**2*WING**2*DELW*(SS*DELW)
DELU=UG(I,2)
DELU=AMAX1(DELU,0.0)
DELU(I,2)=DELU**2*WING**2*DELU*(SS*DELU)
DELU=AMAX1(DELU,0.0)
DELU(I,2)=DELU**2*WING**2*DELU*(SS*DELU)
CPR(I,2)=.5*(N(I,2)+N(I,2))
NZ(I,2)=.5*(N(I,2)+N(I,2))
NR(I,2)=.25*(I,2)*C(I,2)*C(I,2)*C(I,2)
CD(I,2)=.25*(UP(I,2)+UP(I,2))
WPR(I,2)=.25*(UP(I,2)+UP(I,2))
UPZ(I,2)=.5*(UG(I,2)+UG(I,2))
WGC(I,2)=.5*(UG(I,2)+UG(I,2))

```

DER11720
 DER11730
 DER11740
 DER11750
 DER11760
 DER11770
 DER11780
 DER11790
 DER11800
 DER11810
 DER11820
 DER11830
 DER11840
 DER11850
 DER11860
 DER11870
 DER11880
 DER11890
 DER11900
 DER11910
 DER11920
 DER11930
 DER11940
 DER11950
 DER11960
 DER11970
 DER11980
 DER11990
 DER12000
 DER12010
 DER12020
 DER12030
 DER12040
 DER12050
 DER12060
 DER12070
 DER12080
 DER12090
 DER12100

```

WGN(1S,2) = .5*(WG(1S,2)+WING)
UGN(1S,2) = .5*UG(1S,2)
UGD(1S,2) = .5*(JG(1S,2)+UG(1T,2))
ADEV = C(1S,2)/(1.-VFL)
DUD = UG(1S,2)*U=(1S,2)
DWD = WG(1S,2)*W=(1S,2)
VFS=DUD*DUD+DWD*DWD
DFP = -APF*ADEN*VFS
ANG=ATAN(DUD/DWD)
DZ(1S,2) = DFP*COS(ANG)
DR(1S,2) = DFP*SIN(ANG)
LXP(1S,2) = 1
KUP(1S,2) = 1
LWG(1S,2) = 1
KUG(1S,2) = 1
IF (WP(1S,2) .GT. 0) LWP(1S,2) = 0
IF (UP(1S,2) .GT. 0) KUP(1S,2) = 0
IF (WG(1S,2) .GT. 0) LWG(1S,2) = 0

```

```

DER12110
DER12120
DER12130
DER12140
DER12150
DER12160
DER12170
DER12180
DER12190
DER12200
DER12210
DER12220
DER12230
DER12240
DER12250
DER12260
DER12270
DER12280

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

      IF (UG(IS,2) .GT. 0) KUG(IS,2) = 0
      C INTERIOR REGION CALCULATIONS FOR COMPUTED VARIABLES
      DO 40 I=2,IA
      DO 40 J=2,JA
      IF(J.E3.AND.I.LT.IT) GO TO 45
      EI(I,J)=E(I,J)/C(I,J)
      2 -O.25*(WG(I,J)**2+WG(I-I,J)**2+UG(I,J)**2+UG(I-J,I)**2)/FJ
      VFL=NI(I,J)*VCLP
      VFL=MINI(VFL,9999)
      VFL=MAXI(VFL,0)
      PD(I,J)=C(VFLMAX) PD(I,J)=PAV
      IF(VFL.GE.0) J=EL(I,J)*C(I,J)/(1.-VFL)
      RHOG = G(I,J)/(1.-VFL)
      DELW = WG(I-I,J)*WG(I,J)
      DELW = MAXI(DELW,0)
      GZ(I,J) = EL*C(I,J)*(SS*DELW)*DELW
      DELW=XP(I-I,J)*P(I,J)
      DELW=MAXI(DELW,0.0)
      GPZ(I,J)=F*MIN(I,J)*DELW*(SS*DELW)
      DELU = UG(I,J-I)*UG(I,J)
      DELU = MAXI(DELU,0)
      GR(I,J)=L*C(I,J)*(SS*DELU)*DELU
      DELUP=XP(I-I,J)*P(I,J)
      DELUP=MAXI(DELUP,0.0)
      GPR(I,J)=F*MIN(I,J)*DELUP*(SS*DELUP)
      NZ(I,J)=.5*(N(I,J)+N(I-I,J))
      NR(I,J)=.5*(N(I,J)+N(I-J,I))
      CD(I,J)=.25*(C(I,J)+C(I-I,J)*C(I-J,I))
      WPR(I,J)=.25*(P(I,J)+P(I-I,J)*P(I-J,I))
      UPZ(I,J)=.25*(UP(I,J)+UP(I-I,J)*UP(I-J,I))
      WGD(I,J)=.25*(WG(I,J)+WG(I-I,J)*WG(I-J,I))
      WGN(I,J)=.25*(WG(I,J)+WG(I-I,J))
      UGN(I,J)=.25*(UG(I,J)+UG(I-I,J))
      UGD(I,J)=.25*(UG(I,J)+UG(I-I,J))
      ADEVG(I,J)/(1.-VFL)
      DUG(I,J)=UP(I,J)
      DWG(I,J)=WP(I,J)
      VFS=HUG(I,J)+WD*CD

```

DERI2290
DERI2300
DERI2310
DERI2320
DERI2330
DERI2340
DERI2350
DERI2360
DERI2370
DERI2380
DERI2390
DERI2400
DERI2410
DERI2420
DERI2430
DERI2440
DERI2450
DERI2460
DERI2470
DERI2480
DERI2490
DERI2500
DERI2510
DERI2520
DERI2530
DERI2540
DERI2550
DERI2560
DERI2570
DERI2580
DERI2590
DERI2600
DERI2610
DERI2620
DERI2630
DERI2640
DERI2650
DERI2660
DERI2670

DER12680
DER12690
DER12700
DER12710
DER12720
DER12730
DER12740
DER12750
DER12760
DER12770
DER12780
DER12790
DER12800
DER12810
DER12820
DER12830
DER12840
DER12850

```

DPP = APPADEN*VFS
ANG=ATAN(DJC/D*O)
DZ(I,J)=DF*%COS(ANG)
DR(I,J)=DF*%SIN(ANG)
LWP(I,J)=1
KUP(I,J)=1
LWG(I,J)=1
KUG(I,J)=1
IF(HP(I,J)*GT.O) LWP(I,J)=0
IF(LUP(I,J)*GT.O) KUP(I,J)=0
IF(LG(I,J)*GT.O) LWG(I,J)=0
IF(LUG(I,J)*GT.O) KUG(I,J)=0
40 CONTINUE
C SET BOUNDARY VALUES FOR COMPUTED VARIABLES
DO 50 J=1,JA
P(I,J)=P(2,J)
QZ(I,J) = QZ(2,J)
CD(I,J)=CD(2,J)

```

TWO DIMENSIONAL GAS PARTICLE FLOW

DERI2860
DERI2870
DERI2880
DERI2890
DERI2900
DERI2910
DERI2920
DERI2930
DERI2940
DERI2950
DERI2960
DERI2970
DERI2980
DERI2990
DERI3000
DERI3010
DERI3020
DERI3030
DERI3040
DERI3050
DERI3060
DERI3070
DERI3080
DERI3090
DERI3100
DERI3110
DERI3120
DERI3130
DERI3140
DERI3150
DERI3160
DERI3170
DERI3180
DERI3190
DERI3200
DERI3210
DERI3220
DERI3230
DERI3240

DZ(1,J)=DZ(2,J)
LWP(1,J)=LWP(2,J)
LWG(1,J)=LWG(2,J)
UGD(1,J)=UGD(2,J)
50 WGD(1,J)=WGD(2,J)
DO 52 J=2,JA
P(1B,J)=P(1A,J)
QZ(1B,J)=QZ(1A,J)
PD(1B,J)=PD(1A,J)
WGN(1B,J)=WGN(1A,J)
52 UGN(1B,J)=UGN(1A,J)
DO 54 I=2,IA
P(1,JH)=P(1,JA)
QR(1,J5)=QR(1,JA)
UGN(1,J8)=UGN(1,JA)
54 PD(1,J8)=PD(1,JA)
DO 56 I=2,II
P(1,2)=P(1,3)
P(1,1)=P(1,2)
GR(1,2)=GR(1,3)
CD(1,2)=CD(1,3)
DR(1,2)=DR(1,3)
WGD(1,2)=WGD(1,3)
KUP(1,2)=KUP(1,3)
KUG(1,2)=KUG(1,3)
56 UGD(1,2)=UGD(1,3)
DO 58 I=1,II
P(1,1)=P(1,2)
GR(1,1)=GR(1,2)
CD(1,1)=CD(1,2)
DR(1,1)=DR(1,2)
WGD(1,1)=WGD(1,2)
KUP(1,1)=KUP(1,2)
KUG(1,1)=KUG(1,2)
58 UGD(1,1)=UGD(1,2)
P(1M-1,1)=P(1M-1,2)
CALCULATE GAS MOMENTUM FLUXES
DO 300 I=1,IM
DO 300 J=1,JM

C

```

IM1=MAXO(I-1,1)
WGB=0.5*(WG(IM1,J)+WG(I,J))
CALL LOFU(WGB,I)
IM1PL=MINO(I-1+L,IM)
IM1PK=MAXO(IM1PL,I)
GZW(I,J)=AZ(I,J)*C(I,J)*(WG(IM1PL,J)**2)
IP1=MINO(I+1,IM)
UGB=0.5*(UG(I,J)+UG(IP1,J))
CALL LOFU(UGB,K)
JPK=MINO(J+1,JM)
JP1=MINO(J-1,JM)
CB=(C(I,J)+C(IP1,J)+C(I,J)+C(IP1,J))/4.0
GRW(I,J)=A*G(I,J)*CB*UGB*WG(I,JPK)
JM1=MAXO(J-1,1)
UGB=0.5*(UG(I,JM1)+UG(I,J))
CALL LOFU(UGB,K)
JM1PK=MINO(JM1+1,JM)
JM1PK=MAXO(JM1PK,1)

```

```

DERI3250
DERI3260
DERI3270
DERI3280
DERI3290
DERI3300
DERI3310
DERI3320
DERI3330
DERI3340
DERI3350
DERI3360
DERI3370
DERI3380
DERI3390
DERI3400
DERI3410
DERI3420

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

GRU(I,J)=A2N(I,J)*C(I,J)*(UG(I,JM2PK)**2)
VGR=0.5*(WG(I,J)+WG(I,JPI))
CALL LOFU('GB,L')
IPL=MING(IPL,IPI)
300 GZU(I,J)=A2Z(J)*CB*WGB*UG(IPL,J)
C COMPUTE DF(I,S,2,M) AT NOZZLE CELL
C
LP = LWP(I,S,2)
KP = KUP(I,S,2)
C
DF(I,S,2,1) = (AZ(2)*(WINP*V(N-WP(I,S,2)*N(I,S+LP,2))
1      -A(I,S,2)*UP(I,S,2)*N(I,S,2+KP))/V(I,S,2)
C
TERM1 = -U2(I,S,2)/DELZ(IS)
IF (UP(I,S,2) .LT. 0.) TERM1 = (UP(I,S,2)-UP(I,T,2))/DELZ(IT)
C
DF(I,S,2,2) = WPR(I,S,2)*TERM1-UP(I,S,2)*(UP(I,S,2+KP)-UP(I,S,1+K**)) /
1  DELRR(2+KP)-DR(I,S,2)/WM-IPD(I,S,3)-PD(I,S,2))/(NR(I,S,2)*WM*DELRR(3))
2  DELRR(I,S,3)-QPR(I,S,2))/(WM*NR(I,S,2)*DELRR(3))
C
TERM1 = (WINP-WP(I,S,2))/DELZZ(IS)
IF (WP(I,S,2) .LT. 0.) TERM1 = (WP(I,S,2)-WP(I,T,2))/DELZZ(IT)
TERM2 = 0.
IF (UPZ(I,S,2) .LT. 0.) TERM2 = (WP(I,S,3)-WP(I,S,2))/DELRR(3)
C
DF(I,S,2,3) = WP(I,S,2)*TERM1-UP7(I,S,2)*TERM2-0Z(I,S,2)/WM
1-(PD(I,T,2)-PD(I,S,2))/(NZ(I,S,2)*WM*DELZ(IT))
2 -(QPI(I,T,2)-QPI(I,S,2))/(NZ(I,S,2)*WM*DELZ(IT))
C
LP = LWG(I,S,2)
KP = KUG(I,S,2)
C
CF(I,S,2,4) = (AZ(2)*(WING*CI(N-WG(I,S,2)*C(I,S+LP,2))-
1      A(I,S,2)*UG(I,S,2)*C(I,S,2+KP))/V(I,S,2)
C
DF(I,S,2,5) = (-GZU(I,S,2)+GRU(I,S,2)*GRU(I,S,3)
2-AR(I,S,2)*(P(I,S,3)+QR(I,S,3)-P(I,S,2)+GR(I,S,2)))/VR(I,S,2)
3+NR(I,S,2)*QZ(I,S,2)
C

```


DERI3820
DERI3830
DERI3840
DERI3850
DERI3860
DERI3870
DERI3880
DERI3890
DERI3900
DERI3910
DERI3920
DERI3930
DERI3940
DERI3950
DERI3960
DERI3970
DERI3980
DERI3990

```

WB=0.5*(WING+WG(IS,2))
IF (WB) 302,301,301
301 WBB=WING
GO TO 303
302 WBB=WG(IS,2)
303 GZW1=AZ(2)*C(IS,2)*(WBB**2)
    GF(IS,2,6)=GZW1*GZW(IS+1,2)*GAW(IS,2)
    2 -AZ(2)*(P(IT,2)+QZ(IT,2)-P(IS,2)-GZ(IS,2))/VZ(IS,2)
    3 +NZ(IS,2)*DZ(IS,2)
C
    GF(IS,2,7) = ((AZ(2)*(WING*(EIN*FJ+PIN))-WG(IS,2)*E(IS+LP,2)*FJ+
    1P(IS+LP,2)*QZ(IS+LP,2)))-AR(IS,2)*UG(IS,2)*E(IS,2)*KP)*FY+
    2*(IS,2)*KP)+3R(IS,2+KP))/V(1,2)+.5*N(IS,2)*DZ(IS,2)*WF(IS,2)+
    3R(IS,2)*U2(IS,2))/FJ
C
C CALCULATE DF VALUES AT INTERIOR NODES
C
DO 200 I=2,14

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

DO 200 J=2,JA
IF(J.EG.2.AND.I.L.T.IT) GO TO 250
LP=LWP(I,J)
LN=LWP(I-1,J)
KP=KUP(I,J)
KV=KUP(I,J-1)
LS=1
KS=1
IF(LWR(I,J).GT.0.) LS=0
IF(LPZ(I,J).GT.0.) KS=0
C
DF(I,J,1)=(AZ(I,J)*(WP(I-1,J)*N(I-1+LN,J)-WP(I,J)*N(I+LP,J))
1-AR(I,J)*UP(I,J)*N(I,J+KP)+AR(I,J-1)*UP(I,J-1)*N(I,J-1+KN))/V(I,J)
C
DF(I,J,2)=AR(I,J)*(UP(I-1+LS,J)-UP(I+LS,J))/DELZ(I+LS)
1-UP(I,J)*(UP(I,J+KP)-UP(I,J-1+KP))/DELRR(I+KP)
2-AR(I,J)/WM*(PD(I,J+1)-PD(I,J))/NR(I,J)*WM*DELR(I,J+1)
3-(GR(I,J+1)-GR(I,J))/(WM*VR(I,J)*DELR(I,J+1))
C
DF(I,J,3)=WP(I,J)*(WP(I-1+LP,J)-WP(I+LP,J))/DELZZ(I+LP)
1-UPZ(I,J)*(WP(I,J+KS)-WP(I,J-1+KS))/DELR(I+KS)
2-UPZ(I,J)/WM*(PD(I,J+1)-PD(I,J))/NZ(I,J)*WM*DELZ(I+1)
3-(GZ(I+1,J)-GZ(I,J))/(NZ(I,J)*WM*DELZ(I+1))
C
LP=LWG(I,J)
LN=LWG(I-1,J)
KP=KUG(I,J)
KV=KUG(I,J-1)
C
DF(I,J,4)=(AZ(I,J)*(WG(I-1,J)*C(I-1+LN,J)-WG(I,J)*C(I+LP,J))
1-AR(I,J)*UC(I,J)*C(I,J+KP)+AR(I,J-1)*UC(I,J-1)*C(I,J-1+KN))/V(I,J)
C
DF(I,J,5)=(GRU(I,J)-GRU(I,J+1)+GZU(I-1,J)-GZU(I,J)
2-AR(I,J)*(P(I,J+1)-P(I,J-1)-P(I,J)-GR(I,J))/VR(I,J)
3+NR(I,J)*DR(I,J)
C
DF(I,J,6)=(GZW(I,J)-GZW(I,J+1)+GRW(I,J-1)-GRW(I,J)
2-AZ(I,J)*(P(I+1,J)+GZ(I+1,J)-P(I,J)-GZ(I,J))/VZ(I,J)
3+IZ(I,J)*JZ(I,J)
C

```

```

DERI4000
DERI4010
DERI4020
DERI4030
DERI4040
DERI4050
DERI4060
DERI4070
DERI4080
DERI4090
DERI4100
DERI4110
DERI4120
DERI4130
DERI4140
DERI4150
DERI4160
DERI4170
DERI4180
DERI4190
DERI4200
DERI4210
DERI4220
DERI4230
DERI4240
DERI4250
DERI4260
DERI4270
DERI4280
DERI4290
DERI4300
DERI4310
DERI4320
DERI4330
DERI4340
DERI4350
DERI4360
DERI4370
DERI4380

```

DER14390
 DER14400
 DER14410
 DER14420
 DER14430
 DER14440
 DER14450
 DER14460
 DER14470
 DER14480
 DER14490
 DER14500
 DER14510
 DER14520
 DER14530
 DER14540
 DER14550
 DER14560
 DER14570

```

C
  DF(I,J,Z) = ((AZ(J)*(WG(I-1,J)*(E(I-1,J)*FJ*P(I-1,LP,J)) +
  19Z(I-1,LP,J)) - WG(I,J)*(E(I,LP,J)*FJ*P(I,LP,J)) + A(I,J-1)*
  24R(I,J)*UG(I,J)*(E(I,J+KP)*FJ*P(I,J+KP)) + A(I,J-1)*
  3UG(I,J-1)*(E(I,J=1+KN)*FJ*P(I,J-1+KN)) + V(I,J)) +
  4.5*N(I,J)*CZ(I,J)*WP(I,J)*D(I-1,J)*WP(I,J)*UP(I,J) +
  5DR(I,J-1)*P(I,J-1))/FJ
  200 CONTINUE
  C CONVERT DY(L) FROM DF(I,J,M)
  L=0
  DO 2 I=2,11
  DO 2 J=2,11
  IF(J-ER*2+ND+1,LT,IS) GO TO 2
  DO 4 M=1,7
  L=L+1
  4 DY(L)=DF(I,J,M)
  2 CONTINUE
  RETURN
  END
  
```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE CNTRL(Y,DY,DT,T,NTRY)
PARAMETER ID=25,JD=15,LD=400,NRKO=2625
DIMENSION Y(NRKO),DY(NRKO)
DIMENSION CP(ID,JD)
COMMON /DC/ C1,C2,ING,WIND,NIN,
2 GRU(ID,JD),GZU(ID,JD),GRW(ID,JD),GZW(ID,JD)
COMMON /AL-/ F(ID,JD,7),DF(ID,JD,7),I1,IS,IA,IB,IM,JA,JB,JM,IT,
1FJ,VOLP,MV,APF,VFLMAX,PAV,FLRS,KW,KK,KKQ,KM,PIN,IRK,RWOP,
2 T1(LD),PIV(LD),CING(LD),WINDG(LD),NIND(LD),
3Z(ID),ZZ(ID),DELZ(ID),R(JD),RR(JD),DELR(JD),DELR(JD),
4AZ(JD),AZC(JD),AR(ID,JD),ARV(ID,JD),ARD(ID,JD),VZ(ID,JD),VZ(ID,JD),
5VR(ID,JD),C(ID,JD),CZ(ID,JD),CR(ID,JD),CD(ID,JD),WC(ID,JD),
6XCN(ID,JD),XGQ(ID,JD),UG(IN,JD),UGN(ID,JD),UGD(ID,JD),WP(ID,JD),
7WPR(ID,JD),UP(ID,JD),UPZ(ID,JD),N(ID,JD),NZ(ID,JD),NR(ID,JD),
8E(ID,JD),E1(ID,JD),P(ID,JD),PR(ID,JD),PO(ID,JD),DR(ID,JD),
9CZ(ID,JD),WP(ID,JD),KUP(ID,JD),LWC(ID,JD),KUG(ID,JD),GZ(ID,JD),
A WINDP(LD)
COMMON/MC/VIJW,IW(8),JW(8),PW(8)
REAL N,NIND,NR,NZ
DATA PB/0.3/.VPROJ/0.0/.ZPROJ/0.0/
KK = KK+1
KKQ=KKQ+1
IF (KKQ-KK) 1,2,2
1 NTRY = 1
2 GO TO 3
3 CONTINUE
WRITE (6,109) KK,KKQ,DT,T,PIN
109 FORMAT (1H,10X,3HKK=,16,10X,4HKKQ=,16,10X,3HDT=,1PE14.6,
2 5X,2HAT=,E14.6,5X,4HPIN=,E14.6)
DO 6 I=1,NIJW
IWI=IW(I)
JW=JW(I)
PL=PIV(I,JW)+0.5*(IWI,JW)*(WGN(IWI,JW)**2+UGN(IWI,JW)**2)
2 +0.5*(WGN(IWI,JW)*WP(IWI,JW)**2+UP(IWI,JW)**2)
6 PW(I)=PL*2.54*2.54/(980.616*153.59)
WRITE (6,300) (I,PW(I),I=1,NIJW)
300 FORMAT (1H,16(3X,3HPW,1,1,2,1)=,1PE11.4))
IF ((KK/5)-5-KK) 8,7,8

```

CNTR0400
CNTR0410
CNTR0420
CNTR0430
CNTR0440
CNTR0450
CNTR0460
CNTR0470
CNTR0480
CNTR0490
CNTR0500
CNTR0510
CNTR0520
CNTR0530
CNTR0540
CNTR0550
CNTR0560
CNTR0570

```

7 CONTINUE
WRITE (8) K, T, (PW(I), I=1, NIJW), PB, VPROJ, ZPROJ, Y(4), Y(5)
8 CONTINUE
IF ((KX/KW)*X-K) 5,4,5
4 CONTINUE
WRITE (9) K, T, DT, (Y(I), I=1, IRK)
DO 9 I=1, I1
DO 9 J=1, IJ
9 CP(I, J)=N(I, J)*WY
WRITE (10) K, (K(I, J), J=1, IJ), (Z(I), I=1, IM),
2 (D(I, J), J=1, IJ), (C(I, J), J=1, JM), I=1, IM)
WRITE (6, 320) PIN, CIN, WING, WINP, NIN
320 FORMAT (14I, 2X, 4HPIN=1PE11.5, 2X, 4HCIN=E11.5, 2X, 5HWING=,
2 E11.5, 2X, 2HWINP=E11.5, 2X, 4HNIN=E11.5)
CALL OUTPUT (IH0, P, ID, JD, IM, JM, 10, 10HP, FIELD)
CALL OUTPUT (IH0, W, ID, JD, IM, JM, 10, 10HWG, FIELD)
CALL OUTPUT (IH0, JG, ID, JD, IM, JM, 10, 10HUG, FIELD)
CALL OUTPUT (IH0, WP, ID, JD, IM, JM, 10, 10HWP, FIELD)

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

CALL OUTPT (IH0,UP ,ID,JD,IM,JM,10,10HUP FIELD )
CALL OUTPT (IH0,C ,ID,JD,IM,JM,10,10HC FIELD )
CALL OUTPT (IH0,N ,ID,JD,IM,JM,10,10HN FIELD )
CALL OUTPT (IH0,EI ,ID,JD,IM,JM,10,10HEI FIELD )
5 CONTINUE
RETURN
END

```

CNTR0580
 CNTR0590
 CNTR0600
 CNTR0610
 CNTR0620
 CNTR0630
 CNTR0640

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE LOFU (U,L)
IF (U) 2,1,1
1 L=0
RETURN
2 L=1
RETURN
END

```

LOFU0010
 LOFU0020
 LOFU0030
 LOFU0040
 LOFU0050
 LOFU0060
 LOFU0070

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE UNEGR(IM, RM, IR, RR, R, ID)
  DIMENSION R(ID)
  FIR=FLOAT(IR)
  FIM=FLOAT(IM)
  R=1.0
  DO 1 K=1,5
    EX=EXP(-B*(FIM+FIR-2.0))+(1.0-EXP(-2.0*B*(FIR-1.0)))*RM/RR
    R=ALOG(EX)/(FIM-FIR)
    WRITE (6,1) K,B,IM,IR,RR
  101 FORMAT (1H3,3X,24K=,15.3X,2HB=,1PE14.6,3X,3HM=,15.3X,
    2 3HR=,15.3X,3HM=,E14.6,3X,3HR=,E14.6)
  1 CONTINUE
  DO 2 K=6,25
    F1=RM*SINH(S*(FIR-1.0))
    F2=RR*SINH(B*(FIR-1.0))
    D1=RM*(FIR-1.0)*COSH(B*(FIR-1.0))-RR*(FIM-1.0)*COSH(B*(FIM-1.0))
    D2=F1*(FIR-1.0)*2-F2*(FIM-1.0)*2
    D3=SGLNLOG(1.0/D1)*DBLE(D2)/DBLE(D2)*DBLE(D1)/
    2 DBLE(D2)
    R=ATN(D3/D2)
    WRITE (6,1) K,B,IM,IR,RR,1PE14.6,3X,2HB=,E14.6)
  102 FORMAT (1H3,3X,24K=,15.3X,2HB=,1PE14.6,3X,3HM=,15.3X,
    2 3HR=,15.3X,3HM=,E14.6,3X,3HR=,E14.6)
  3 CONTINUE
  3 A=RR/SINH(S*(FIR-1.0))
  4 RQ,1=A*SINH(B*(FIR-1.0))
  RETURN
END

```

UNE00010
 UNE00020
 UNE00030
 UNE00040
 UNE00050
 UNE00060
 UNE00070
 UNE00080
 UNE00090
 UNE00100
 UNE00110
 UNE00120
 UNE00130
 UNE00140
 UNE00150
 UNE00160
 UNE00170
 UNE00180
 UNE00190
 UNE00200
 UNE00210
 UNE00220
 UNE00230
 UNE00240
 UNE00250
 UNE00260
 UNE00270
 UNE00280
 UNE00290
 UNE00300

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE NZLINP (T1,PIND,CIND,WINDG,WINDP,NIND,T,PIN,CIN,WING,
2 WINP,NIN,LD)
REAL WINDP,NIN
DIMENSION T1(LD),PIND(LD),CIND(LD),WINDG(LD),WINDP(LD),NIND(LD),
DATA LLL/1,
GO TO (1,2),LLL
1 T1=T1(1)
T2=T1(2)
I=1
LLL=2
2 IF (T-T1) 7,3,3
3 IF (T-T2) 10,10,11
11 KS=1+1
DO 4 K=KS,-D
J=K
IF (T1(K)-T) 4,5,4
4 CONTINUE
5 CONTINUE
I=J
T1=T1(I)
T2=T1(I+1)
GO TO 10
6 I=J-1
T1=T1(I)
T2=T1(I+1)
GO TO 10
7 ME=1-1
DO 8 M=1,ME
N=1-M
IF (T1(N)-T) 9,9,8
8 CONTINUE
9 T1=T1(N)
T2=T1(N+1)
I=N
10 IF (T-T1)/AMAX1(T2-T1),I,DE-11)
TF2=1,0-TF
PIN =TF2*PIND (I)+TF*PIND (I+1)
CIN =TF2*CIND (I)+TF*CIND (I+1)
WING=TF2*WINDG(I)+TF*WINDG(I+1)

```

NZL10010
NZL10020
NZL10030
NZL10040
NZL10050
NZL10060
NZL10070
NZL10080
NZL10090
NZL10100
NZL10110
NZL10120
NZL10130
NZL10140
NZL10150
NZL10160
NZL10170
NZL10180
NZL10190
NZL10200
NZL10210
NZL10220
NZL10230
NZL10240
NZL10250
NZL10260
NZL10270
NZL10280
NZL10290
NZL10300
NZL10310
NZL10320
NZL10330
NZL10340
NZL10350
NZL10360
NZL10370
NZL10380
NZL10390

NZL10400
NZL10410
NZL10420
NZL10430

WINP=TF2*WINP(I)+TF*WINDP(I+1)
NIN =TF2*VIND(I)+TF*VIND(I+1)
RETURN
END

ARK2	0010
ARK2	0020
ARK2	0030
ARK2	0040
ARK2	0050
ARK2	0060
ARK2	0070
ARK2	0080
ARK2	0090
ARK2	0100
ARK2	0110
ARK2	0120
ARK2	0130
ARK2	0140
ARK2	0150
ARK2	0160
ARK2	0170
ARK2	0180
ARK2	0190
ARK2	0200
ARK2	0210
ARK2	0220
ARK2	0230
ARK2	0240
ARK2	0250
ARK2	0260
ARK2	0270
ARK2	0280
ARK2	0290
ARK2	0300
ARK2	0310
ARK2	0320
ARK2	0330
ARK2	0340
ARK2	0350
ARK2	0360
ARK2	0370
ARK2	0380
ARK2	0390

UUU UUU

```

      RETURN
12  EOC=ABS(E/C)
      EOCM=AMAX1(EOC,EOCM)
      IF (EOC-EOCM) 13,13,901
901  EOCM=EOC
      LSV=1
13  CONTINUE
      IF (EOCM-1.0) 17,17,14
14  T=TS
      DO 15 I=1,N
          Y(I)=YST(I)
15  DY(I)=DYST(I)
      CALL IJM (LSV,EOCM)
      DO 16 J=1,10
          EOCM=EOCM/10.0
          DT=DT/THRI0
          IF (EOCM-0.3) 6,6,16
16  CONTINUE

```

```

RK2 0400
RK2 0410
RK2 0420
RK2 0430
RK2 0440
RK2 0450
RK2 0460
RK2 0470
RK2 0480
RK2 0490
RK2 0500
RK2 0510
RK2 0520
RK2 0530
RK2 0540
RK2 0550
RK2 0560
RK2 0570

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

GO TO 6
17 CALL CNTRL (Y,DY,DT,T,NTRY)
GO TO (21,18,19,4),NTRY
18 RETURN
19 TEST
DO 20 I=1,N
Y(I)=YST(I)
20 CV(I)=CVST(I)
GO TO 6
21 IF (ECCM-0.3) 25,25,22
22 DT=DT/THR12
CALL IJ1 (-SV ,ECCM)
GO TO 4
25 IF (ECCM-0.03) 26,4,4
26 DT=DT/THR12
IF (ABS(DT)-ABS(DTM)) 4,4,24
24 DT=ABS(DTM)*DT/ABS(DT)
GO TO 4
END

```

```

RK2 0580
RK2 0590
RK2 0600
RK2 0610
RK2 0620
RK2 0630
RK2 0640
RK2 0650
RK2 0660
RK2 0670
RK2 0680
RK2 0690
RK2 0700
RK2 0710
RK2 0720
RK2 0730
RK2 0740
RK2 0750
RK2 0760

```

TWO DIMENSIONAL GAS PARTICLE FLOW

```

SUBROUTINE IJM (LSV,EOCM)
PARAMETER ID=25,JD=15,LD=400,NRKD=2625
COMMON /ALL/ F(ID,JD,7),DF(ID,JD,7),I1,IS,IA,IB,IM,JA,JB,JM,IT,
1FJ,VOLP,MY,APF,VELMAX,PAV,FL,RC,KW,KK,KKO,KM,PIN,IRK,RHOP,
2T(LD),PIV(LD),CIND(LD),WINDG(LD),NINO(LD),
37(ID),ZZ(I),DELZ(ID),DELZZ(ID),R(JD),RR(JD),DELR(JD),DELR(JD),
4AZ(JD),AZD(JD),AR(ID,JD),ARN(ID,JD),ARD(ID,JD),CO(ID,JD),WG(ID,JD),
5VR(ID,JD),CZ(ID,JD),CA(ID,JD),UGN(ID,JD),UGD(ID,JD),VP(ID,JD),
6WGN(ID,JD),WGD(ID,JD),UPZ(ID,JD),N(ID,JD),NZ(ID,JD),NR(ID,JD),
7WPR(ID,JD),WPR(ID,JD),UPZ(ID,JD),N(ID,JD),NZ(ID,JD),NR(ID,JD),
8E(ID,JD),E1(ID,JD),P(ID,JD),AR(ID,JD),PD(ID,JD),DR(ID,JD),
9OZ(ID,JD),WP(ID,JD),KUP(ID,JD),LWG(ID,JD),KUG(ID,JD),GZ(ID,JD),
A,WINDP(LD)
L=U
DO 2 I=2,IA
ISV=I
DO 2 J=2,JA
JSV=J
IF (J,ER,2,AND,1,LT,IS) GO TO 2
DO 1 N=1,7
MSV=M
L=L+1
IF (L,LSV) 1,3,1
1 CONTINUE
2 CONTINUE
3 CONTINUE
101 WRITE (3,101) EOCM,LSV,ISV,JSV,MSV
101 FORMAT (1H,10X,5HEOCM=,1PE12,5,10X,2HL=,16,10X,2HJ=,16,10X,
2 2HJ=,16,10X,2HM=,16)
RETURN
END

```

TWO DIMENSIONAL GAS PARTICLE FLOW

OUTP0010
OUTP0020
OUTP0030
OUTP0040
OUTP0050
OUTP0060
OUTP0070
OUTP0080
OUTP0090
OUTP0100
OUTP0110
OUTP0120
OUTP0130
OUTP0140
OUTP0150
OUTP0160
OUTP0170
OUTP0180
OUTP0190
OUTP0200
OUTP0210
OUTP0220
OUTP0230
OUTP0240
OUTP0250

```

SUBROUTINE OUTPT (IPC,F,JD,IM,JM,NL,LABEL)
  DIMENSION E(1D,JJ),LABEL(22),LAB2(20)
  DATA LBW/64
  GO TO 200
  ENTRY OUTPT7 (IPC,G,K3,JD,IM,JM,NL,LABEL)
  DIMENSION G(1D,JJ,7)
  DO 201 I=1,IM
  DO 201 J=1,JM
    F(I,J)=G(I,J,K3)
  201 CONTINUE
  JMM=MIND(J,12)
  NW=1+(NL-1)/6
  NST=10-(NW+1)/2
  DO 1 I=1,2J
    1 LAB2(I)=LW+
    DO 2 I=1,NW
      2 NST+I-1
    2 LAB2(K)=LAB2(I)
  WRITE (6,101) IPC,LAB2(1),I,1,20),(J,J=1,JMM)
  101 FORMAT (A1,20A6, // 1H ,2X,1H,2X,2HJ,12,11,10)
  DO 3 I=1,IM
    3 WRITE (6,102) I,(F(I,J),J=1,JMM)
  102 FORMAT (1H ,13,1PE10,3,11E10,3)
  RETURN
  END

```